

US EPA ARCHIVE DOCUMENT



# **Steam Hydrogasification Research Overview**

*2010 Pacific Southwest Organic Residuals Symposium*

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*Center for Environmental Research and Technology,*

*University of California, Riverside*



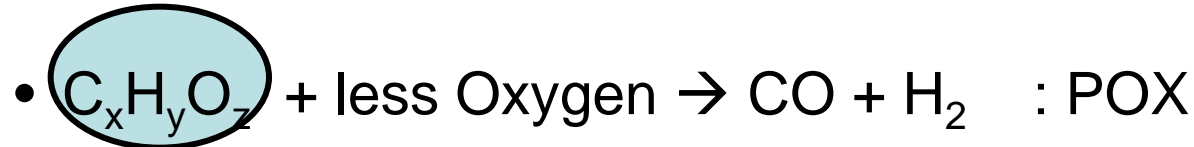
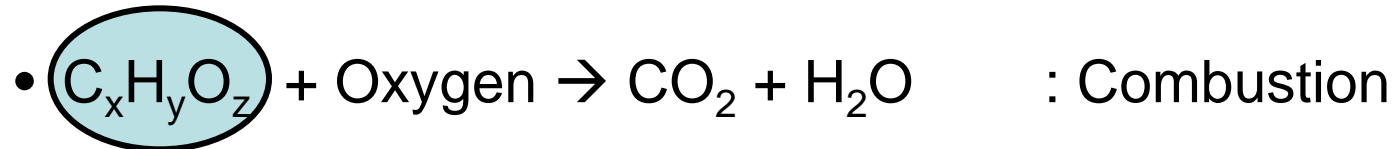
## **Content**

- 1. Background of Gasification and GTL*
- 2. Introduction to the Steam Hydrogasification Reaction*
- 3. Applications/ Projects for Steam Hydrogasification Reaction*



## What is Gasification Process ?

- A thermo-chemical process converts any carbon-containing material into a synthesis gas, usually via partial oxidation (POX) reaction.

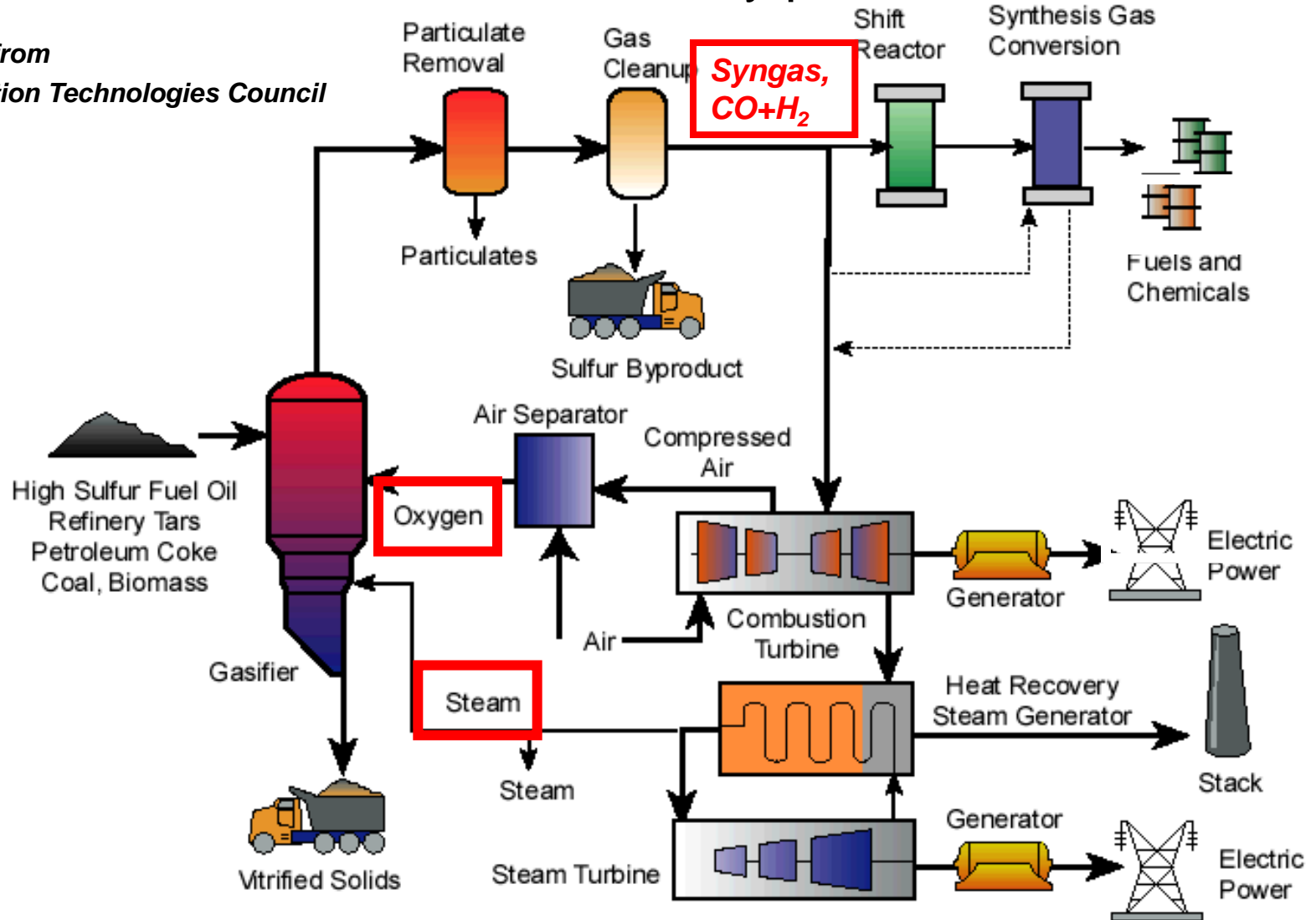


- The synthesis gas can be used as a fuel to generate electricity (IGCC) or used as a feedstock for synthetic fuel or chemicals (GTL Process)



# Typical Gasification Technology with Fuel or Electricity production

•Quoted from Gasification Technologies Council





## Hydrogasification Process



- Gasification in Hydrogen Environment
- Used for SNG production from coal and biomass since 1930s.
- Internal hydrogen supply thru water gas reaction of the char or steam methane reforming of the product gas
- Requires high pressure (~100atm) or catalyst.  
→Lack of commercial success or interest.



## Steam Hydrogasification Process (SHR)

- The most unique feature of SHR is the introduction of water to reaction scheme



*Others : CO, CO<sub>2</sub>, C<sub>2</sub> +*

- Effect of steam on the hydrogasification of carbon had not been studied extensively
- Our initial research found that addition of water
  - Increased the reaction rate
  - High efficiency at lower temperature
  - High efficiency at lower pressure



## Advantages of Steam Hydrogasification Process (SHR)

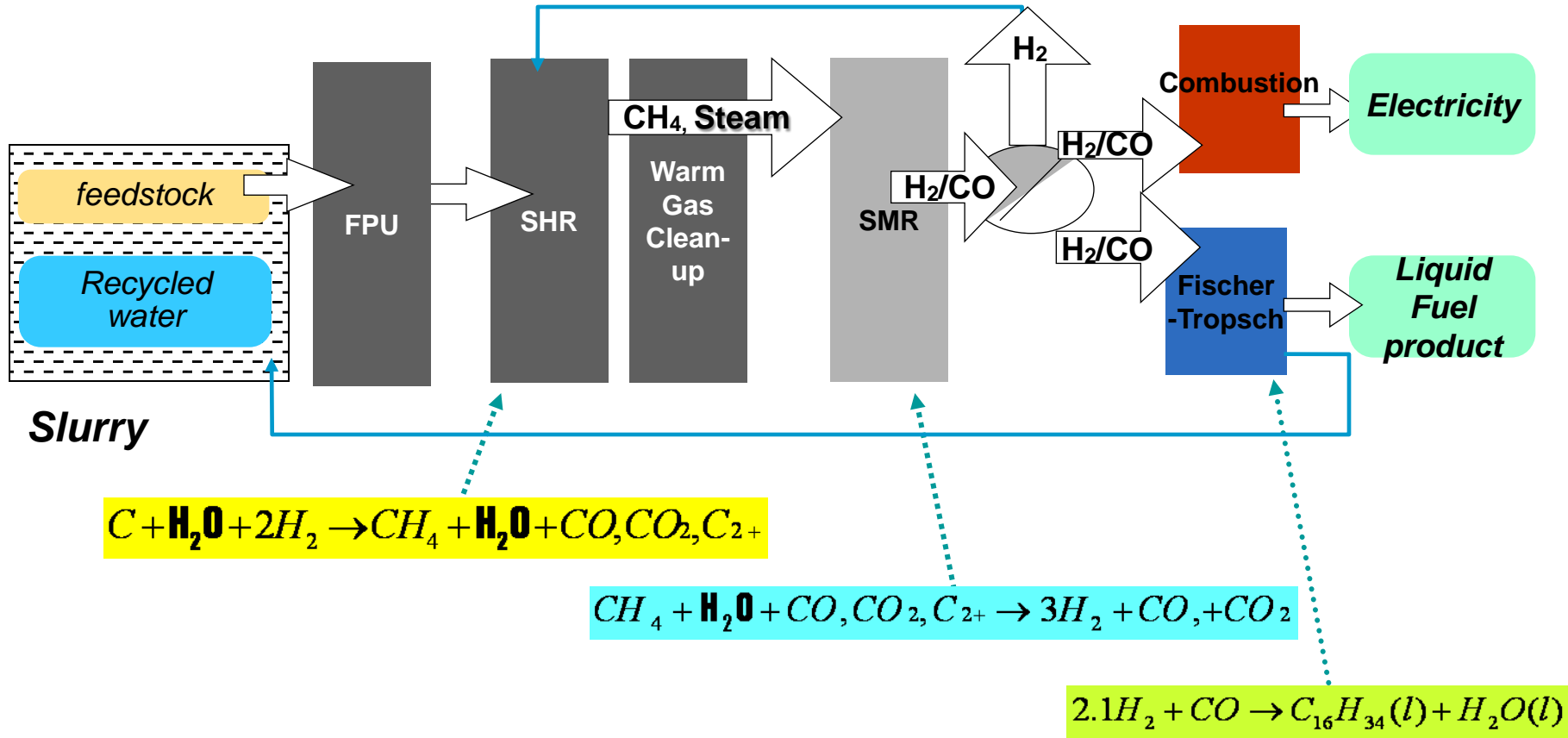


- **Process can handle wet feedstock w/o drying.**
  - Utilize a high pressure slurry pump to reduce costs
- **No expensive oxygen plant required**
  - Process is suitable for smaller scale, distributed facilities (ideal for biomass/waste, coal/biomass feedstock)
- **Can control slurry feed for desired synthesis gas product distribution**
  - Carbon, Water, Hydrogen input ratio
  - Does not require the Water-Gas Shift Process





## CE-CERT Process



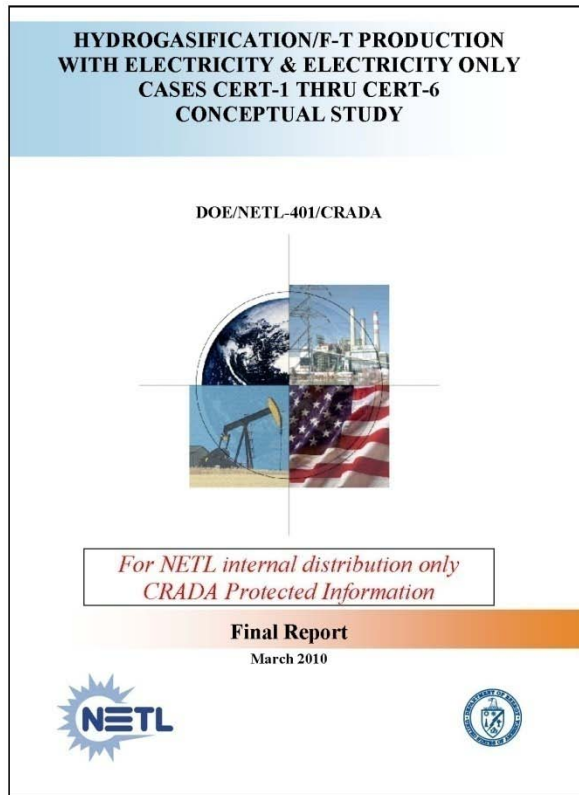
SHR – Steam Hydrogasification Reactor, SMR – Steam Methane Reformer



## Process Reviewed by DOE/NETL

- Since 2007, For the Independent Review of the Process
- Verify the flow-sheet for the several different cases
- Estimate TPC (Total Project Cost) and perform economic analysis

*Their conclusion is that the CE-CERT process has 12 % higher efficiency with 18 % lower capital cost than the most up-to-date conventional mainstream gasification technologies.*





## Laboratory Bench Scale SHR, 1lb/ hour



# PDU scale Fluidized Bed Reactor

## 10 lb/ hr

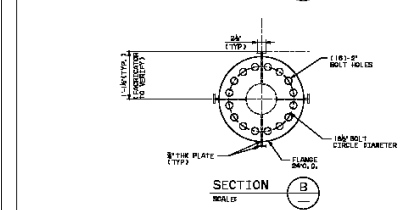
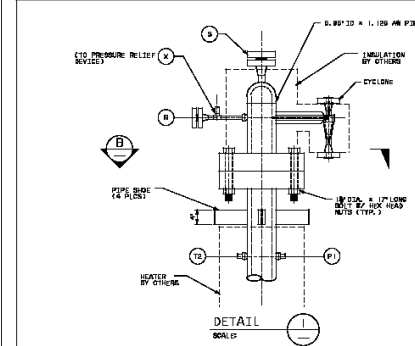
**Funded by PIER project from California Energy Commission (CEC)**

**(Demonstration of Syngas Production from Biosolid-Biomass)**

**Period Oct. 09 – Sep.11**

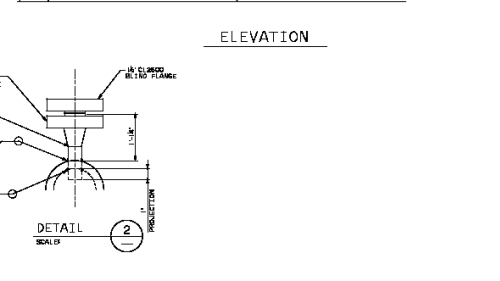
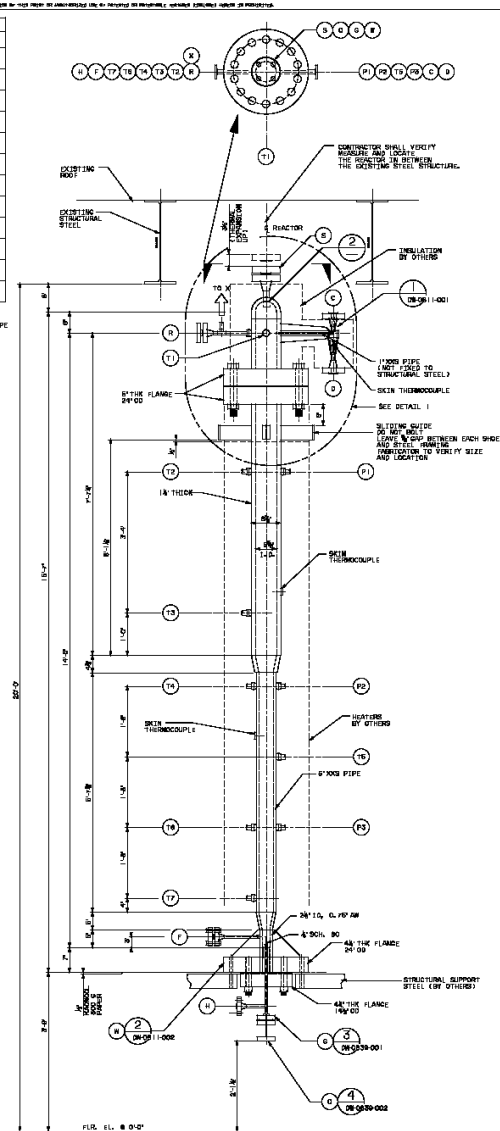
4/6/8 " OD x 22' height  
 iHT800, 150 psi/825C  
 ~20 sec gas residence  
 Time @ 1ft/sec v

NOZZLE TAG	DESCRIPTION	MATERIAL	REMARKS
B	SAND FEED	316 SS BOYD LARGENOR 112	1/4" SCH 40 PIPE, 1/2" BORE, 1/4" DIA. PIPES AND NUTS AND WELDS
T1-T7	THERMOCOUPLE CONNECTION	316 SS BOYD LARGENOR 112	BY FABRICATOR
P1-P3	PRESSURE CONNECTION	316 SS BOYD LARGENOR 112	BY FABRICATOR
H	FLUIDIZING GAS CONNECTION	316 SS BOYD LARGENOR 112	1/4" SCH 40 PIPE, 1/2" BORE, 1/4" DIA. PIPES AND NUTS
R	RODING PORT	316 SS BOYD LARGENOR 112	1/4" SCH 40 PIPE, 1/2" BORE, 1/4" DIA. PIPES AND NUTS
F	ALTERNATE FEED PORT	316 SS BOYD LARGENOR 112	1/4" SCH 40 PIPE, 1/2" BORE, 1/4" DIA. PIPES AND NUTS
D	INJECTOR FEED OR NOZZLE	316 SS BOYD LARGENOR 112	SEE DIMENSION 1001 FOR DETAIL
S	SILVER FEED NOZZLE	316 SS BOYD LARGENOR 112	SEE DIMENSION 1001 FOR DETAIL
M	BIOMASS NOZZLE	316 SS BOYD LARGENOR 112	SEE DIMENSION 1001 FOR DETAIL
X	10 PSI PRESSURE RELIEF DEVICE	316 SS BOYD LARGENOR 112	SEE DIMENSION 1001 FOR DETAIL
C	CYCLONE GAS OUTLET	316 SS BOYD LARGENOR 112	SEE DIMENSION 1001 FOR DETAIL
D	CYCLONE SOLIDS DISCHARGE	316 SS BOYD LARGENOR 112	SEE DIMENSION 1001 FOR DETAIL

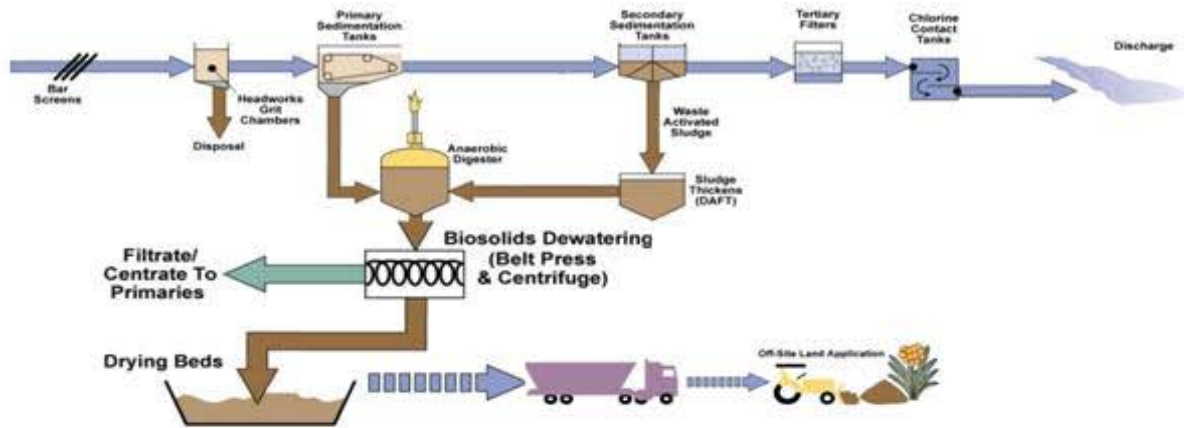


- NOTES
- FOR DESIGN BASIS REFER TO DOC. NO. (A71418 000 JSD 041 001) REV 0 OR EQUIVALENT.
  - ALL MATERIAL TO BE BOYD (LARGENOR 112)
  - USE 1/400 WR FILLER METAL FOR ALL WELDS.
  - ALL CONTINUOUS WELDS TO BE GASE TIGHT. ALL WELDS TO BE FULL PENETRATION (LWD).
  - VESSEL WELDS TO BE 100% RADIOGRAPHED.
  - BOYD FLEXITAL OR EQUIVALENT WITH CERAMIC FILLER TO BE USED AT ALL FLANGE CONNECTIONS.
  - PERMANENT FOR PERMANENT TAG NOZZLES, THERMOCOUPLES, AND THE ALTERNATE FEED NOZZLE TO BE CALLED BY FABRICATOR. REMOVE TAG NOZZLES TO BE CALLED BY FABRICATOR. THE PRESSURE TAG NOZZLES AND THE THERMOCOUPLES, AT WELDS ONLY, ARE TO BE CALLED BY FABRICATOR TO BE CALLED BY FABRICATOR.
  - VESSEL HYDROTEST TO BE PERFORMED AT 440 PSI IN THE SHOP.
  - LEAK SENSITIVE PNEUMATIC TEST AT 70 PSI TO BE PERFORMED AT SHOP FOR THE REACTOR AFTER HYDROTEST.
  - RELIEF LIGHTER IS TO BE ABOVE EACH NOZZLE AND STUFF GATE WITH WINDUP WOOL.
  - PRESSURE RELIEF DEVICE TO BE VENTED TO SAFE LOCATION (BY OTHERS).
  - SHELL TEMPERATURE NOT TO EXCEED BOOTY BY SKIN TEMPERATURE THERMOCOUPLE REQUIREMENT.

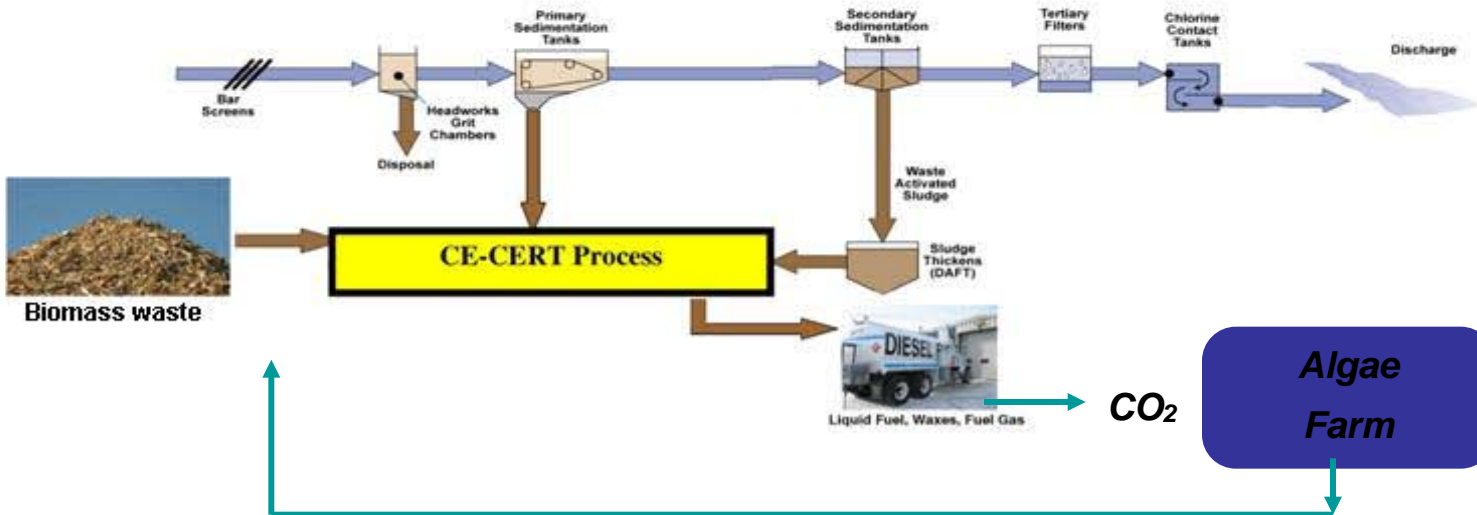
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## 1. Current Process for the Municipal Waste Water Treatment

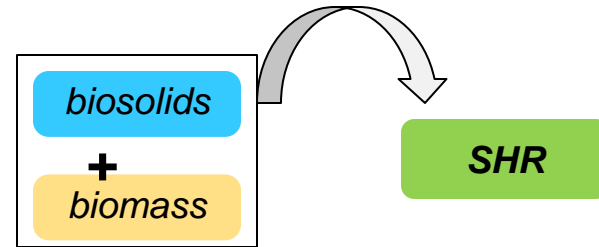
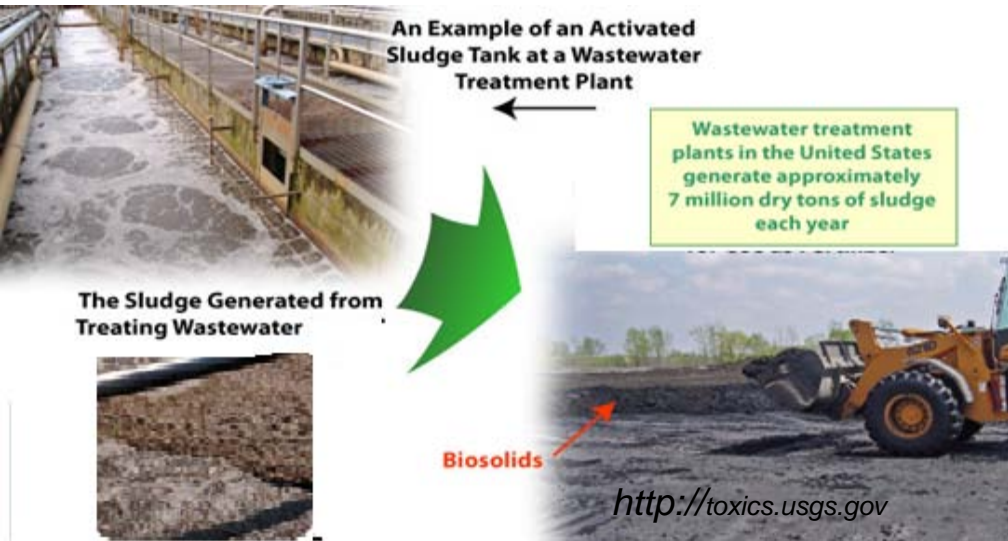


## 2. Suggested Process with Hydrogasification (CE-CERT process)





# Co-mingling of biomass and biosolids



Biosolids samples (DAFT, Dissolved Air Flootation Thickener after the secondary sedimentation treatment) are from Riverside Regional Water Quality Control Treatment Plant

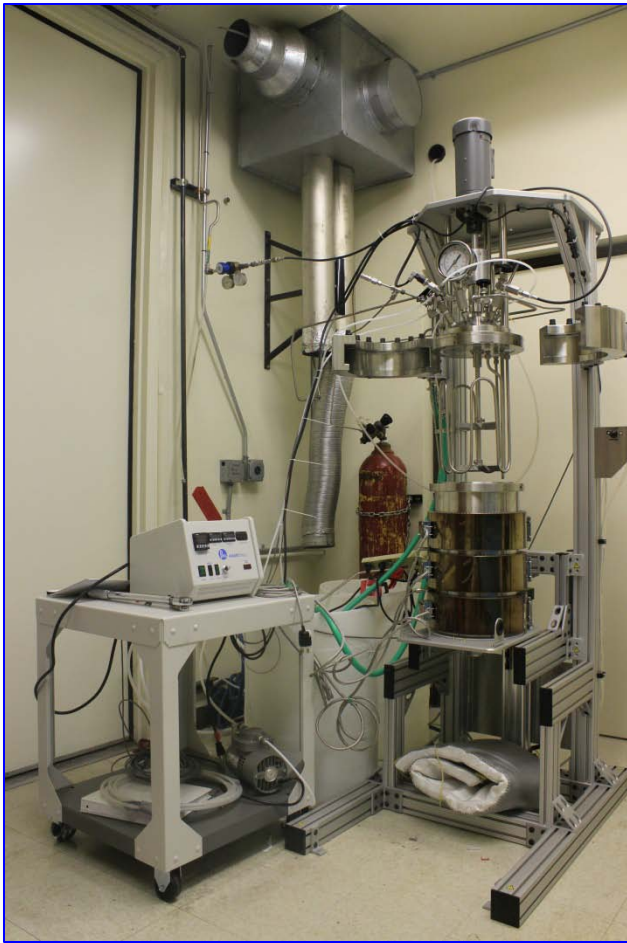
**Table1 Proximate and Ultimate Analysis of biomass(pinewood) and biosolids**

Analysis	Compound	pinewood	Biosolids
Proximate (wt%)	Moisture	5.65	92.9
	Volatile matter	81.52	4.9
	Fixed carbon	12.58	0.6
	Ash	0.25	1.6
Ultimate (dry basis (wt%))	C	47.56	40.8
	H	6.31	6.22
	N	0.05	7.47
	O	45.81	23.14
	Balance*	0.27	22.37

Balance includes other elements eg, S, Cl, metals



# Feedstock Pretreatment Unit (FPU) by Hydrothermal Reaction to produce Pumpable Slurry



*Before*

CE-CERT/UCR



*After*

CE-CERT/UCR





**Initial studies**

Figure 3 Carbon conversion of SHR in lab scale batch reactor at 700°C

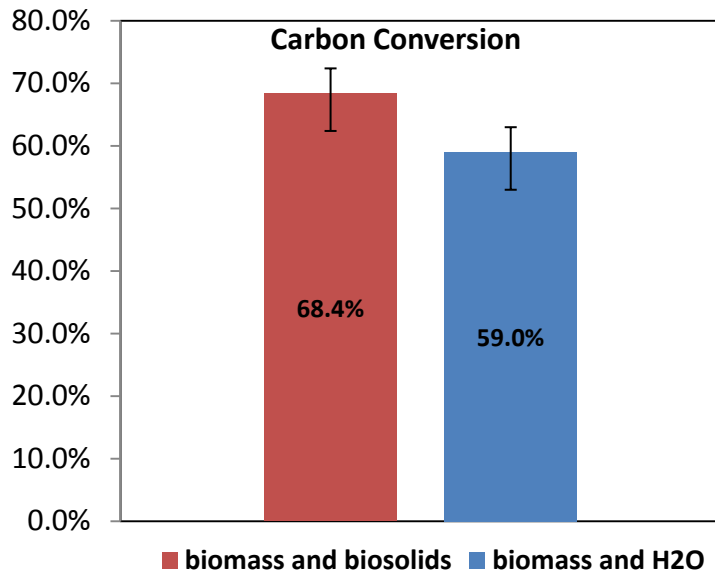


Table3. Metal elements in biosolids (DAFT)

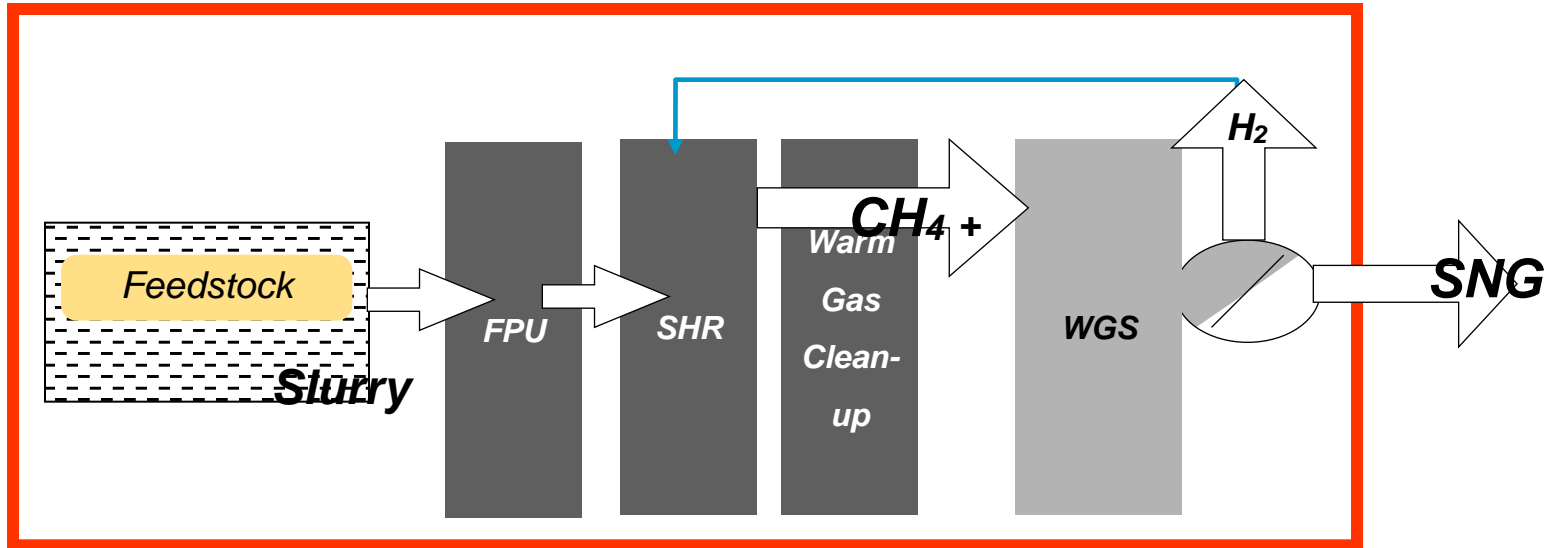
Metal Element	Concentration Mass (ppm)
Iron (Fe)	14770
Calcium (Ca)	11440
Aluminum (Al)	3200
Magnesium (Mg)	1620
Potassium (K)	1620
Titanium (Ti)	1010
Sodium (Na)	690
Zinc (Zn)	400
Copper (Cu)	360
Manganese(Mn)	178
Strontium (Si)	100
Bismuth(Bi)	16
Nickel(Ni)	9

*It has been speculated that the enhanced conversion efficiency may be the result of a catalytic action in the SHR caused by the metal species in the biosolids.*





# Alternative Process for the SNG Production



- DOE SBIR Research
  - High ash, moisture Lignite feedstock
- AQMD Clean Fuel Program
  - Co-mingled Biomass+ Biosolid



## **IP & Publications**

### **1. Patents**

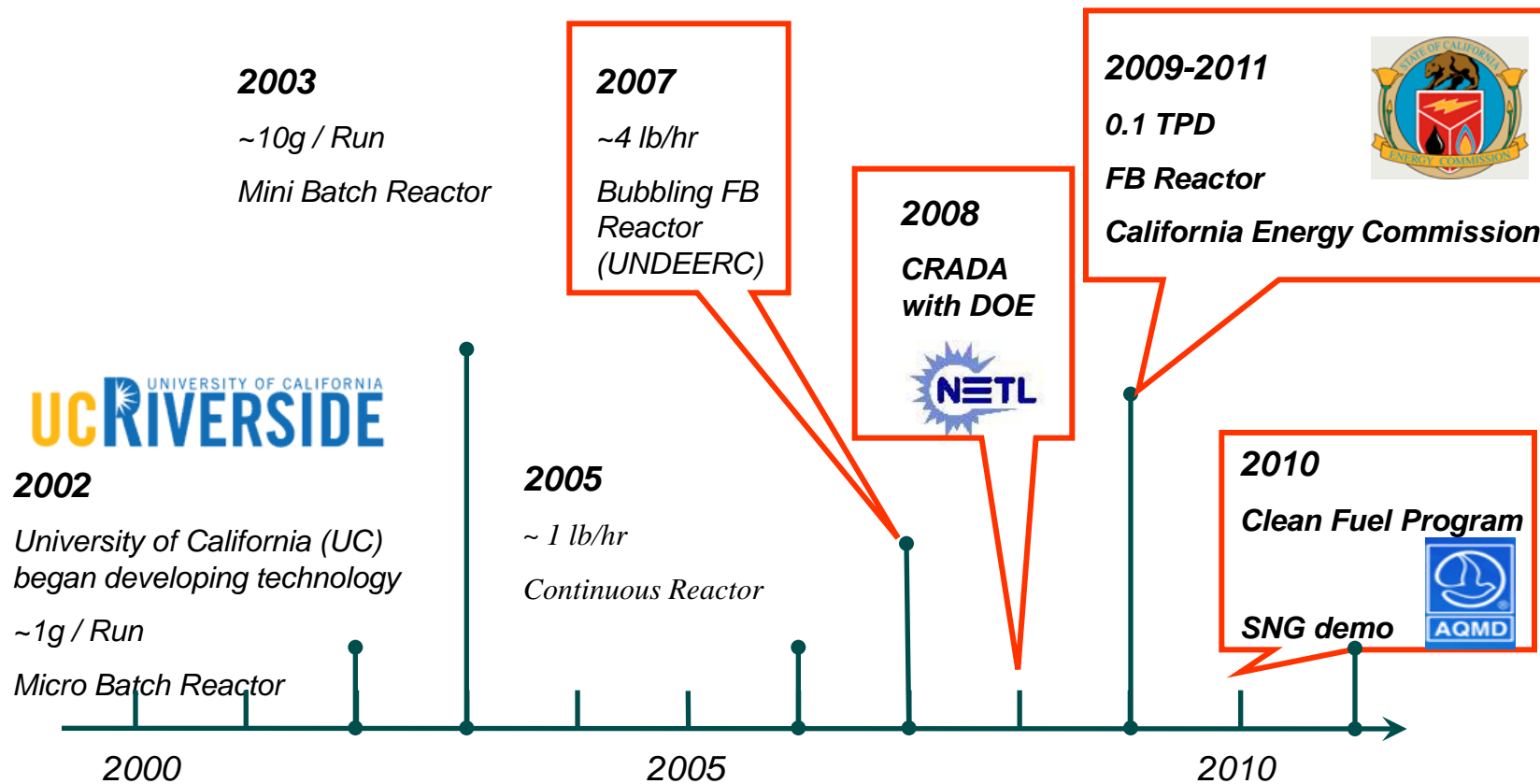
- Total 13 application since year 2002
- 4 Patents awarded
- In Year 2009, 1 new process patent applications

### **2. Publications**

- Total 6 Pier Reviewed Paper Published
- In Year 2009, 1 Published, 3 in preparation.
- 4 Conference Presentations

### **3. Students/ Staff**

- 2MS and 1 PhD in 2009
- 9 PhD Applicants.
- 2 Full Time Engineers
- 2 Visiting Scholars



**2002**

University of California (UC) began developing technology

~1g / Run

Micro Batch Reactor

2000

**2005**

~ 1 lb/hr

Continuous Reactor

2005

**2007**

~4 lb/hr

Bubbling FB Reactor  
(UNDEERC)

**2008**

CRADA with DOE



**2009-2011**

0.1 TPD

FB Reactor

California Energy Commission



**2010**

Clean Fuel Program

SNG demo



2010



# Thank you, Question?

[cspark@cert.ucr.edu](mailto:cspark@cert.ucr.edu)





# Major Plant Parameters

	<b>CTL w/ CE-CERT Process (CERT-2)</b>	<b>CTL w/ Conventional Entrained type Gasifier</b>
Input	4000 TPD CTL Plant	3707 TPD CTL Plant
Out	107 MW electricity 7143 BPD (2.8 BPD/Metric Ton of Coal)	10.3 MW electricity 7143 BPD
HHV $\eta$	53.4%	47.6%
TPC/ TCR	\$1,026 MM/\$1,512 MM (Jan. 2008 \$)	\$1215 MM/\$1,764 MM
IRR*	17% (@ \$38/T) 20% (@ \$18/T)	7% (@ \$38/T) 12% (@ \$18/T)

*\*By Power Systems Financial Model prepared for NETL by Nexant, Inc*

15%, interest rate, \$2.69 /gallon of diesel, 4% IRR for CERT-1