Magellan Terminals Holdings, L.P.
Corpus Christi Terminal
GHG Permit Application
Response to EPA Questions
March 19, 2014

1. Please provide a detailed description of the distillation process as it pertains to the proposed condensate splitter. This should include a list of all the potential hydrocarbon streams and all the distillates produced and indicate which of the four heaters is capable of processing which hydrocarbon streams and the resulting products from the distillation.

Response: A revised process description is attached. The process will consist of two identical trains, each with two process heaters. Each train will be capable of processing the same hydrocarbon streams and producing the same products. The proposed hydrocarbon feed streams included crude oil and natural gas "condensate" which is a variable composition mixture consisting primarily of ethane and longer chain alkanes. Products from the process include light and heavy naphtha, jet fuel, distillate, resid, and propane/butane/LPG.

One of the process heaters is the Fractionator Heater which will pre-heat a bottoms stream from the pre-fractionator prior to entering the fractionator. The second process heater is a hot oil heater, which does not receive or directly process a hydrocarbon stream. The hot oil heater provides heat in the form of heated oil, much like a boiler would provide process heat in the form of steam, where required throughout the process. The hot oil system is a closed system in which the "used" hot oil is returned from the process to the hot oil heater for reheating and reuse.

2. Please provide a simplified process flow with a representation of all the GHG emission sources and associated EPNs.

Response: A revised process flow diagram is attached. All GHG emissions sources have been identified with a green G next to each block on the diagram where GHGs are emitted.

3. Please provide the total annual operating time and maximum firing rates for the four proposed heaters and two vapor combustors along with their maximum potential emissions.

Response: The four process heaters will be permitted to operate continuously (8,760 hours/year). Each Hot Oil Heater (H-1B and H-2B) has a maximum firing rate of 108 MMBtu/hr and an annual average firing rate of 98 MMBtu/hr. Each Fractionator Heater (H-1A and H-2A) has a maximum firing rate of 116 MMBtu/hr and an annual average firing rate of 105 MMBtu/hr. All rates are HHV. Each of the two marine vapor combustion units will have a maximum firing rate of 146 MMBtu/hr, based on the current design, and will be authorized to operate 8,760 hour/year. This firing rate will be confirmed, and the GHG emission rates will be calculated and included in the revised GHG permit application.

4. Please provide information on the thermal efficiency for the four proposed heaters, and information on control/monitoring systems to ensure combustion efficiency is maximized and to ensure heaters will maintain at the proposed thermal efficiency level.

Response: The design thermal efficiency of each of the four heaters is 91%. Magellan will monitor exhaust temperature and O_2 content, and adjust the air/fuel using fans and a bypass damper on the air preheat exchanger to maintain heater efficiency to the maximum extent practical during actual operation.

5. Please provide detail information on additional ancillary equipment (i.e., emergency generator, fire water pump engine, etc.) and their impact on the efficiency of the unit and overall environmental impacts.

Response: There will be two 617 hp diesel-fired firewater pump engines, one 500 kW diesel-fired emergency generator, and one 100 kW diesel-fired emergency generator. Each engine will be permitted to operate no more than 100 hours per year for testing purposes. Any additional operation will be for emergency purposes only. Two 16 MMBtu/hr gas fired Tank Heaters, one new and one existing, will also be used at the facility. An additional vapor combustion unit (VCU) used to control emissions from tank maintenance activities has been added to the project. These emission points and their GHG emissions will be included in the revised GHG permit application.

6. As mentioned in Section 6.1.1, "Incondensable material produced by the splitter process may also be used as heater fuel; therefore, reducing purchased natural gas usage". Please provided information on the composition of this incondensable material and the quantity of such material which will be used as a fuel supply.

Response: The non-condensable streams used as fuel in the heaters will contribute an estimated 25 MMBtu/hr, 12-month average, of the total heat input to the four process heaters. This represents approximately 6% of the combined firing capacity of the heaters. The composition of this material, shown in an attached table, is similar to natural gas and thus will not significantly impact the total GHG emission rate from the heaters. However, for completeness, the contribution to the GHG emissions from this material will be quantified and included in the updated heater emissions representations in the revised GHG permit application.

7. The permit application does not provide any compliance monitoring for the new condensate splitter. A monitoring (i.e., CEM), recordkeeping, and reporting strategy to ensure enforceability of the BACT requirements pursuant to 40CFR Section 52.21 (n) should be proposed.

Response: The four process heaters, two tank heaters, and the vapor combustor will result in over 99% of the GHG emissions from the project. Magellan will continuously monitor the fuel flow to each of these combustion units and calculate GHG emissions from each based on fuel flow rates and EPA default emission factors for natural gas. The vent gas flow rate to the vapor combustor will also be monitored, and the vent streams will be sampled and analyzed for composition at least monthly. The composition of the streams will be used to calculate a CO2 emission factor that will be applied to the flow rate to calculate CO2 emissions from the vapor combustor. Emissions from the emergency engines will be calculated from EPA approved factors and record of the actual operating hours of each engine. Records of all monitoring data and calculations will be maintained at the site for 5 years. All remaining emission sources have an insignificant contribution to total GHG emissions and thus will not be monitored. Emissions from these remaining sources will be assumed to be equal to the represented rates in the permit application.

8. Please provide a copy of the completed TCEQ Form PI-I General Application for Air Preconstruction Permit and Amendment, if any.

Response: A copy of the completed TCEQ Form PI-1 is enclosed.

9. Please provide detail information on the Carbon Capture and Sequestration review for this specific facility.

Response: The revised GHG permit application will include a cost analysis for a Carbon Capture and Sequestration system that demonstrates that this control option is not cost effective.

10. Please provide information identifying each emission point will be constructed under which phase of construction.

Response: As stated in the response to Item No. 1, two identical process trains will be installed. Train 1 will be installed in Phase 1, and Train 2 will be installed in Phase 2. All facilities that support both trains will be installed in Phase 1. The attached table indicates which emission points are included in each of the two phases.

11. As mentioned in Section 6.1.4, "The CO_2 streams included in this application are similar in nature to the gas-fired industrial boiler...." Please provide site-specific flue gas stream information (i.e., pressure, the quantity and concentration of CO_2 that is in the flue gas stream, etc.)

Response: The four large process heaters will be designed to operate with 15% excess air, and the small tank heaters will be operated with 20% excess air. At these excess air levels, the flue gas is about 8% CO_2 by volume. These rates will be confirmed, and supporting documentation will be included in the revised GHG permit application.

12. Under the Good Combustion Practices and Periodic Heater Tune-ups discussion in Section 6.1.4, please provide information on how will the data be recorded and stored, and information on the monitoring and recordkeeping requirements.

Response: Magellan will maintain records of all inspections and tune-ups on site for 5 years. The description of the operations that constitute part of the Good Combustion Practices does not result in any recordable data for which records are to be maintained.

13. The global warming potentials (GWP) have been revised. The final rule published on November 29, 2013 in the Federal Register will be effective for all permits issued on or after January 1, 2014. The methane value was increased from 21 to 25 (times more potent than CO_2), the N_2O value was decreased from 310 to 298 and the SF_6 value decreased from 23,900 to 22,800. Please provide updated emission tables using the new GWPs.

Response: The updated emissions calculations in the revised GHG permit application will utilize the above revised GWPs.

Section 4
Process Description

The Magellan condensate splitter facility to be installed in the MTH Corpus Christi Terminal will process 100,000 bbls/day of a hydrocarbon condensate material (including both condensate and crude oil) to obtain products suitable for commercial use or as feedstock for further refining. The facility will consist of two trains processing 50,000 bbls/day each of condensate, with Phase 1 being the initial 50,000 bbls/day installation and Phase 2 an identical train to be installed in the future. The process described in the following paragraphs utilizes conventional distillation technology for the specified range of condensate feed.

The hydrocarbon condensate is fed from storage tanks (EPNs T135-T138) to the prefractionator column. The feed to this prefractionator column is preheated by cross heat exchange with hot streams from the main fractionator to reduce overall heat input to the unit from fired heating. In the prefractionator column the lightest fraction of the condensate is distilled from the overhead at a pressure that will permit complete condensation. Any incondensable material that may be produced will be used as fuel gas in the heaters (EPNs H-1A, H-1B, H-2A, and H-2B). Free water that may be present in the feed will be flashed in the pre-fractionation column and produced from the overhead accumulator. Overhead liquid from the prefractionator column is cooled with an air cooler, recovered from the overhead accumulator, and sent to two additional fractionation columns to further refine the stream. The bottoms stream from the pre-fractionation column is pumped into a downstream fired heater and into the main fractionation column. Heat is supplied to the prefractionator by means of the column feed preheat and a hot oil system heated by a hot oil heater (EPNs H-1B and H-2B).

The liquid overhead stream from the pre-fractionator column is pumped to a depropanizer column. The column overhead vapor is condensed with an air cooler. The propane product is recovered from an overhead accumulator where it is sent to pressurized storage tanks (FINs T170-T179). Heat is supplied to the depropanizer column using the hot oil system.

The bottoms stream from the depropanizer column is pressured to a debutanizer column. The overhead vapor is condensed with an air cooler. The butane product is recovered from an overhead accumulator where it is sent to pressurized storage tanks (FINs T170-T179). Heat is supplied to the depropanizer column using the hot oil system. The debutanizer bottoms product,

light naphtha, is cooled with an air cooler, further cooled by cross exchange with the prefractionator feed, and sent to storage (EPNs T159-T162).

The main fractionation column separates the bottoms from the pre-fractionation column into four products. These products include heavy naphtha, jet fuel, diesel, and residual liquid (resid). The net overhead product, heavy naphtha, is cooled with an air cooler and pumped to storage (EPNs T163-T168). The cooling is accomplished by cross exchange with the prefractionator feed in order to pre-heat the feed followed by final cooling. The jet and diesel are recovered from the column as side streams. The jet and diesel are then fed to the top trays of individual stripping columns. Light ends are stripped from the product draw in the jet side column by introducing heat to the bottom of the stripper column. Heat is supplied to this column by the fractionators heaters (EPNs H-1A and H-1B). Natural gas is used as stripping vapor for the diesel side stream stripper. Stripping gas is necessary because the vapor generated by reboiling diesel would result in higher temperatures that could lead to coking. The stripped side draw vapors are returned to the main fractionation column from the overhead of each stripper column and the stripped side draw products are used to preheat the feed to the process before final cooling and transfer to storage (EPNs T43-T46, T154-T157, and T-120-T123).

The fractionator bottoms product, resid, is then cross exchanged with feed to the pre-fractionator column, further cooled, and then sent to storage (EPNs T124-T127). This product is the heaviest fraction of the condensate. Lighter material is removed in the lower stripping section of the column. Normally steam is used as a stripping medium. However, since steam is not being used in this plant, natural gas will be used as the stripping medium. The stripping gas ends up in the column off gas. The fractionator column will be operated at the lowest practical pressure to minimize temperatures and improve separation. Both a liquid distillate product and a non-condensable gas stream saturated with heavier components will be produced from the overhead vapor along with column reflux. The off-gas will be compressed and sent to fuel gas.

In addition to the main process equipment described above, the condensate splitter requires certain support systems. An existing tank heater (EPN H-3) and a new tank heater (EPN H-4) will be used as needed to provide heat to storage tanks and dock lines. The tank heaters, which use oil as a heat transfer medium, are only anticipated to be needed during the winter months. A flare (EPN FL-1) is provided for use in emergency overpressure situations to dispose of excess process vapors. The flare also controls routine process streams and vapors from

specific MSS activities. This flare utilizes a continuous pilot to ensure that unexpected release events result in safe disposal. Fuel gas to the plant is supplied by natural gas pipeline. A new fire water pump (EPN FWP1), a backup firewater pump (EPN FWP2), and two new emergency backup generators (EPNs EMGEN1 and EMGEN2) are also included with this project. Two new diesel fuel tanks (EPNs FWPTK and EMGENTK) will store fuel for the emergency combustion units.

Existing Port of Corpus Christi docks and Magellan marine vapor combustor controls (EPNs LOADFUG and VCU1/VCU2) will be utilized to transfer products offsite. Piping modifications will be made to each dock. LPG (propane/butane) product will be transferred under pressure to tank trucks at a new loading rack (EPN LPGTRUCK). All of the products may be transferred to local refineries and terminals via existing pipelines.

This application also includes maintenance, startup, and shutdown (MSS) activities. A vapor combustion unit (EPN MSSVCU) will be installed at the facility to control vapors generated during certain MSS activities including storage tank roof landings, process vessel and piping maintenance, and pressurized tank maintenance activities. Vacuum trucks (EPN VRTRUCK) and frac tanks (EPN FRTANK) may be used to collect and store liquids generated during MSS activities. Product samples will be collected (EPN SAMPLE) and tested onsite using a bench scale lab. Leftover sample liquid will be stored in a tank (EPN SAMPTK).

Magellan is also planning a potential wastewater treatment system for the splitter process that may consist of a desalter, a CPI gravity place separator, an Induced Gas Floatation (IGF) stage, and a nut shell filter. In addition one oil-water separator may be added to the facility. This system is still in the planning phase.

A simplified process flow diagram is included as Figure 4-1.

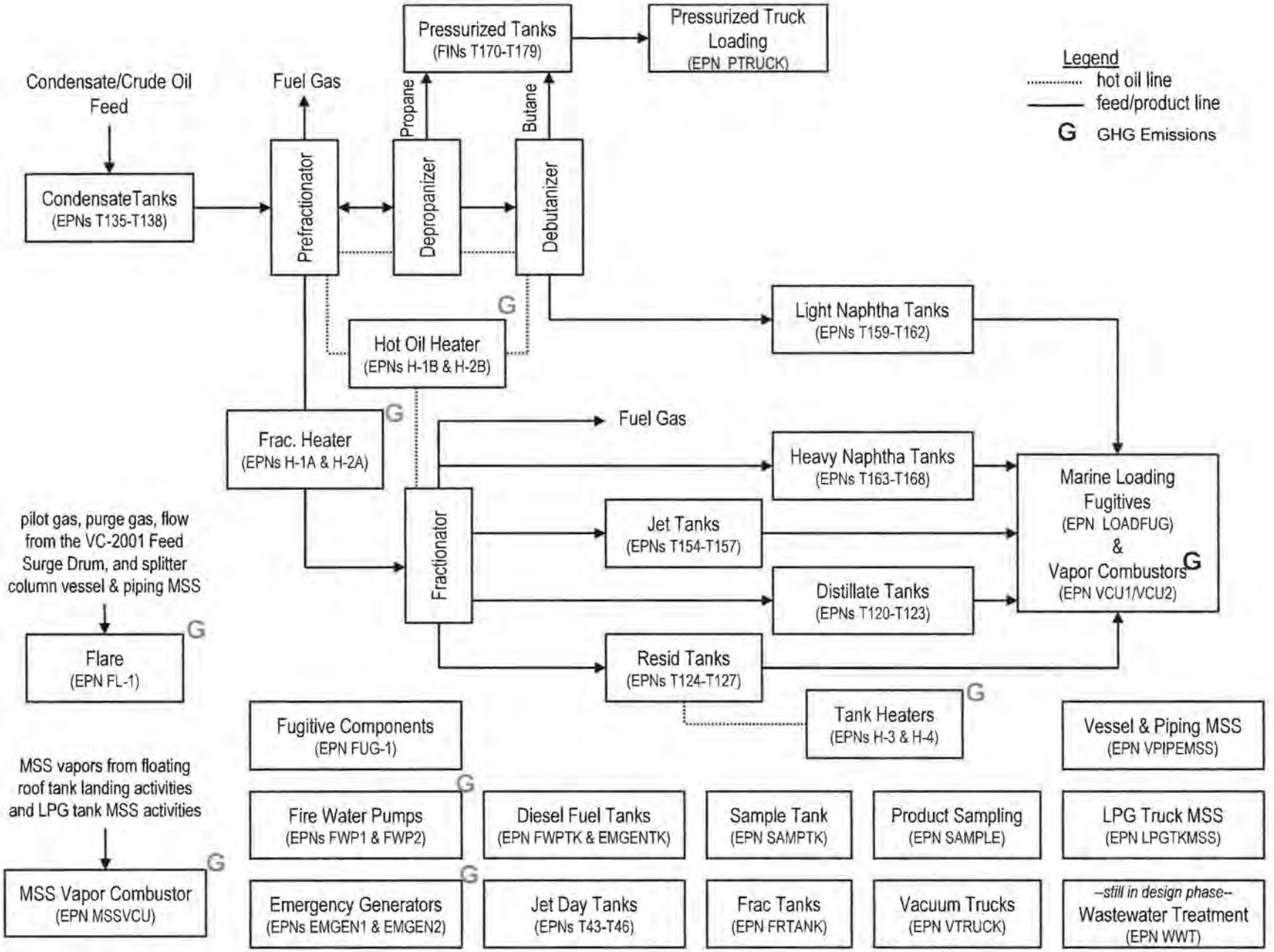

Figure 4-1 ◆ Magellan Processing L.P. ◆ Condensate Splitter Project ◆ Corpus Christi, Texas

Magellan Terminals Condensate Splitter Project - GHG EPNs

EPN	Description	Status	Project Phase
H-1A	Fractionator Heater	New	1
H-2A	Fractionator Heater	New	2
H-1B	Hot Oil Heater	New	1
H-2B	Hot Oil Heater	New	2
H-3	Tank Heater	Existing	NA
H-4	Tank Heater	New	1
VCU-1	Vapor Combustor	Existing	NA
VCU-2	Vapor Combustor	Existing	NA
MSSVCU	Vapor Combustor	New	1
FL-1	Flare	New	1
FUG1	Natural Gas Fugitives	New	1
FWP1	Fire Water Pump Engine	New	1
FWP2	Fire Water Pump Engine	New	1
EMGEN1	Emergency Generator Engine	New	1
EMGEN2	Emergency Generator Engine	New	1

Typical Composition of Incondensible Material Fired in Heaters

Constituent	Volume %
Methane	87.65%
Ethane	8.29%
Isobutane	0.11%
n-Butane	2.27%
Isopentane	1.68%

Texas Commission on Environmental Quality
Form PI-1 General Application for
Air Preconstruction Permit and Amendment

Important Note: The agency requires that a Core Data Form be submitted on all incoming applications unless a Regulated Entity and Customer Reference Number have been issued and no core data information has changed. For more information regarding the Core Data Form, call (512) 239-5175 or go to www.tceq.texas.gov/permitting/central_registry/guidance.html.

I. Applicant Information		
A. Company or Other Legal Name: Magellan Processing L.P.		
Texas Secretary of State Charter/Registration Number (if applicable):		
B. Company Official Contact Name: Ms. Melanie Little		
Title: Vice President of Operations		
Mailing Address: One Williams Center, MD 27		
City: Tulsa	State: OK	ZIP Code: 74172
Telephone No.: 918-574-7306	Fax No.:	E-mail Address: melanie.little@magellanlp.com
C. Technical Contact Name: Ms. Shahana Banoo		
Title: Air Specialist, Sr.		
Company Name: Magellan Terminals Holdings, L.P.		
Mailing Address: One Williams Center, MD 27		
City: Tulsa	State: OK	ZIP Code: 74172
Telephone No.: 918-574-7767	Fax No.: 918-574-7760	E-mail Address: shahana.banoo@magellanlp.com
D. Site Name: Corpus Christi Terminal		
E. Area Name/Type of Facility: Condensate Splitter		■ Permanent ☐ Portable
F. Principal Company Product or Business: Natural Gas Liquids		
Principal Standard Industrial Classification Code (SIC): 1321		
Principal North American Industry Classification System (NAICS): 211112		
G. Projected Start of Construction Date: November 2014		
Projected Start of Operation Date: January 2016		
H. Facility and Site Location Information (If no street address, provide clear driving directions to the site in writing.):		
Street Address: 1802 Poth Ln		
City/Town: Corpus Christi	County: Nueces	ZIP Code: 78407
Latitude (nearest second): 27* 48' 29.34"	Longitude (nearest second): 97* 26' 12.25"	

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I.	**Applicant Information (continued)**	
I.	Account Identification Number (leave blank if new site or facility):	
J.	Core Data Form.	
Is the Core Data Form (Form 10400) attached? If No, provide customer reference number and regulated entity number (complete K and L).		■ YES ☐ NO
K.	Customer Reference Number (CN): TBD	
L.	Regulated Entity Number (RN): TBD	
II.	**General Information**	
A.	Is confidential information submitted with this application? If Yes, mark each confidential page confidential in large red letters at the bottom of each page.	☐ YES ■ NO
B.	Is this application in response to an investigation, notice of violation, or enforcement action? If Yes, attach a copy of any correspondence from the agency and provide the RN in section I.L. above.	☐ YES ■ NO
C.	Number of New Jobs: 80	
D.	Provide the name of the State Senator and State Representative and district numbers for this facility site:	
State Senator: Juan 'Chuy' Hinojosa		District No.: 20
State Representative: Abel Herrero		District No.: 34
III.	**Type of Permit Action Requested**	
A.	Mark the appropriate box indicating what type of action is requested.	
■ Initial ☐ Amendment ☐ Revision (30 TAC 116.116(e) ☐ Change of Location ☐ Relocation		
B.	Permit Number (if existing):	
C.	Permit Type: Mark the appropriate box indicating what type of permit is requested. *(check all that apply, skip for change of location)*	
■ Construction ☐ Flexible ☐ Multiple Plant ☐ Nonattainment ☐ Plant-Wide Applicability Limit		
■ Prevention of Significant Deterioration ☐ Hazardous Air Pollutant Major Source		
☐ Other:		
D.	Is a permit renewal application being submitted in conjunction with this amendment in accordance with 30 TAC 116.315(c).	☐ YES ■ NO

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III.	**Type of Permit Action Requested *(continued)***		
E.	Is this application for a change of location of previously permitted facilities? If Yes, complete III.E.1 - III.E.4.0		☐ YES ■ NO
1.	Current Location of Facility (If no street address, provide clear driving directions to the site in writing.):		
Street Address:			
City:	County:	ZIP Code:	
2.	Proposed Location of Facility (If no street address, provide clear driving directions to the site in writing.):		
Street Address:			
City:	County:	ZIP Code:	
3.	Will the proposed facility, site, and plot plan meet all current technical requirements of the permit special conditions? If "NO", attach detailed information.		☐ YES ☐ NO
4.	Is the site where the facility is moving considered a major source of criteria pollutants or HAPs?		☐ YES ☐ NO
F.	Consolidation into this Permit: List any standard permits, exemptions or permits by rule to be consolidated into this permit including those for planned maintenance, startup, and shutdown.		
List:			
G.	Are you permitting planned maintenance, startup, and shutdown emissions? If Yes, attach information on any changes to emissions under this application as specified in VII and VIII.		■ YES ☐ NO
H.	Federal Operating Permit Requirements (30 TAC Chapter 122 Applicability) Is this facility located at a site required to obtain a federal operating permit? If Yes, list all associated permit number(s), attach pages as needed).		☐ YES ☐ NO ■ To be determined
Associated Permit No (s.):			

1. Identify the requirements of 30 TAC Chapter 122 that will be triggered if this application is approved.

☐ FOP Significant Revision ☐ FOP Minor ☐ Application for an FOP Revision
☐ Operational Flexibility/Off-Permit Notification ☐ Streamlined Revision for GOP
■ To be Determined ☐ None

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III.	**Type of Permit Action Requested *(continued)***	
H.	Federal Operating Permit Requirements (30 TAC Chapter 122 Applicability) *(continued)*	
2.	Identify the type(s) of FOP(s) issued and/or FOP application(s) submitted/pending for the site. ***(check all that apply)***	
☐ GOP Issued	☐ GOP application/revision application submitted or under APD review	
☐ SOP Issued	☐ SOP application/revision application submitted or under APD review	
IV.	**Public Notice Applicability**	
A.	Is this a new permit application or a change of location application?	■ YES ☐ NO
B.	Is this application for a concrete batch plant? If Yes, complete V.C.1 – V.C.2.	☐ YES ■ NO
C.	Is this an application for a major modification of a PSD, nonattainment, FCAA 112(g) permit, or exceedance of a PAL permit?	☐ YES ■ NO
D.	Is this application for a PSD or major modification of a PSD located within 100 kilometers or less of an affected state or Class I Area?	☐ YES ■ NO
If Yes, list the affected state(s) and/or Class I Area(s).		
List:		
E.	Is this a state permit amendment application? If Yes, complete IV.E.1. – IV.E.3.	
1.	Is there any change in character of emissions in this application?	☐ YES ☐ NO
2.	Is there a new air contaminant in this application?	☐ YES ☐ NO
3.	Do the facilities handle, load, unload, dry, manufacture, or process grain, seed, legumes, or vegetables fibers (agricultural facilities)?	☐ YES ☐ NO
F.	List the total annual emission increases associated with the application ***(List all that apply and attach additional sheets as needed):***	
Volatile Organic Compounds (VOC): 268.14		
Sulfur Dioxide (SO_2): 28.86		
Carbon Monoxide (CO): 96.13		
Nitrogen Oxides (NOx): 33.73		
Particulate Matter (PM): 9.07		
PM 10 microns or less (PM10): 9.07		
PM 2.5 microns or less (PM2.5): 9.07		
Lead (Pb):		
Hazardous Air Pollutants (HAPs): 9.00 (total HAPs)		
Other speciated air contaminants not listed above: H2S 0.36; NH3 8.00		

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V. Public Notice Information *(complete if applicable)*		
A. Public Notice Contact Name: Ms. Shahana Banoo		
Title: Air Specialist, Sr.		
Mailing Address: One Williams Center, MD 27		
City: Tulsa	State: OK	ZIP Code: 74172
B. Name of the Public Place: Corpus Christi Central Library		
Physical Address *(No P.O. Boxes)*: 805 Comanche St		
City: Corpus Christi	County: Nueces	ZIP Code: 78412
The public place has granted authorization to place the application for public viewing and copying.		■ YES ☐ NO
The public place has internet access available for the public.		■ YES ☐ NO
C. Concrete Batch Plants, PSD, and Nonattainment Permits		
1. County Judge Information (For Concrete Batch Plants and PSD and/or Nonattainment Permits) for this facility site.		
The Honorable: Loyd Neal		
Mailing Address: 901 Leopard Street, Room 303		
City: Corpus Christi	State: TX	ZIP Code: 78401
2. Is the facility located in a municipality or an extraterritorial jurisdiction of a municipality? ***(For Concrete Batch Plants)***		☐ YES ☐ NO
Presiding Officers Name(s):		
Title:		
Mailing Address:		
City:	State:	ZIP Code:
3. Provide the name, mailing address of the chief executive and Indian Governing Body; and identify the Federal Land Manager(s) for the location where the facility is or will be located.		
Chief Executive: Mayor Nelda Martinez		
Mailing Address: 1201 Leopard St.		
City: Corpus Christi	State: TX	ZIP Code: 78401
Name of the Indian Governing Body:		
Mailing Address:		
City:	State:	ZIP Code:

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V.	**Public Notice Information *(complete if applicable) (continued)***	
C.	Concrete Batch Plants, PSD, and Nonattainment Permits	
3.	Provide the name, mailing address of the chief executive and Indian Governing Body; and identify the Federal Land Manager(s) for the location where the facility is or will be located. *(continued)*	
Name of the Federal Land Manager(s):		
D.	Bilingual Notice	
Is a bilingual program required by the Texas Education Code in the School District?		■ YES ☐ NO
Are the children who attend either the elementary school or the middle school closest to your facility eligible to be enrolled in a bilingual program provided by the district?		■ YES ☐ NO
If Yes, list which languages are required by the bilingual program?	Spanish	
VI.	**Small Business Classification *(Required)***	
A.	Does this company (including parent companies and subsidiary companies) have fewer than 100 employees or less than $6 million in annual gross receipts?	☐ YES ■ NO
B.	Is the site a major stationary source for federal air quality permitting?	■ YES ☐ NO
C.	Are the site emissions of any regulated air pollutant greater than or equal to 50 tpy?	■ YES ☐ NO
D.	Are the site emissions of all regulated air pollutants combined less than 75 tpy?	☐ YES ■ NO
VII.	**Technical Information**	
A.	The following information must be submitted with your Form PI-1 ***(this is just a checklist to make sure you have included everything)***	
1.	■ Current Area Map	
2.	■ Plot Plan	
3.	☐ Existing Authorizations	
4.	■ Process Flow Diagram	
5.	■ Process Description	
6.	■ Maximum Emissions Data and Calculations	
7.	■ Air Permit Application Tables	
a.	■ Table 1(a) (Form 10153) entitled, Emission Point Summary	
b.	■ Table 2 (Form 10155) entitled, Material Balance	
c.	■ Other equipment, process or control device tables	
B.	Are any schools located within 3,000 feet of this facility?	■ YES ☐ NO

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VII.	**Technical Information**			
C.	Maximum Operating Schedule:			
Hour(s): 24	Day(s): 7	Week(s): 52	Year(s):	
Seasonal Operation? If Yes, please describe in the space provide below.				☐ YES ■ NO
D.	Have the planned MSS emissions been previously submitted as part of an emissions inventory?			☐ YES ■ NO
Provide a list of each planned MSS facility or related activity and indicate which years the MSS activities have been included in the emissions inventories. Attach pages as needed.				
E.	Does this application involve any air contaminants for which a disaster review is required?			☐ YES ■ NO
F.	Does this application include a pollutant of concern on the Air Pollutant Watch List (APWL)?			☐ YES ■ NO
VIII.	**State Regulatory Requirements** **Applicants must demonstrate compliance with all applicable state regulations to obtain a permit or amendment.** *The application must contain detailed attachments addressing applicability or non applicability; identify state regulations; show how requirements are met; and include compliance demonstrations.*			
A.	Will the emissions from the proposed facility protect public health and welfare, and comply with all rules and regulations of the TCEQ?			■ YES ☐ NO
B.	Will emissions of significant air contaminants from the facility be measured?			■ YES ☐ NO
C.	Is the Best Available Control Technology (BACT) demonstration attached?			■ YES ☐ NO
D.	Will the proposed facilities achieve the performance represented in the permit application as demonstrated through recordkeeping, monitoring, stack testing, or other applicable methods?			■ YES ☐ NO
IX.	**Federal Regulatory Requirements** **Applicants must demonstrate compliance with all applicable federal regulations to obtain a permit or amendment.** *The application must contain detailed attachments addressing applicability or non applicability; identify federal regulation subparts; show how requirements are met; and include compliance demonstrations.*			
A.	Does Title 40 Code of Federal Regulations Part 60, (40 CFR Part 60) New Source Performance Standard (NSPS) apply to a facility in this application?			■ YES ☐ NO
B.	Does 40 CFR Part 61, National Emissions Standard for Hazardous Air Pollutants (NESHAP) apply to a facility in this application?			☐ YES ■ NO

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IX.	**Federal Regulatory Requirements** **Applicants must demonstrate compliance with all applicable federal regulations to obtain a permit or amendment.** *The application must contain detailed attachments addressing applicability or non applicability; identify federal regulation subparts; show how requirements are met; and include compliance demonstrations.*	
C.	Does 40 CFR Part 63, Maximum Achievable Control Technology (MACT) standard apply to a facility in this application?	■ YES ☐ NO
D.	Do nonattainment permitting requirements apply to this application?	☐ YES ■ NO
E.	Do prevention of significant deterioration permitting requirements apply to this application?	■ YES ☐ NO
F.	Do Hazardous Air Pollutant Major Source [FCAA 112(g)] requirements apply to this application?	☐ YES ■ NO
G.	Is a Plant-wide Applicability Limit permit being requested?	☐ YES ■ NO
X.	**Professional Engineer (P.E.) Seal**	
Is the estimated capital cost of the project greater than $2 million dollars?		■ YES ☐ NO
If Yes, submit the application under the seal of a Texas licensed P.E.		
XI.	**Permit Fee Information**	
Check, Money Order, Transaction Number ,ePay Voucher Number:	Fee Amount: $ 75,000	
Paid online?	Check No. 3140144441	☐ YES ■ NO
Company name on check: Magellan Terminals Holdings, L.P.		
Is a copy of the check or money order attached to the original submittal of this application?		■ YES ☐ NO ☐ N/A
Is a Table 30 (Form 10196) entitled, Estimated Capital Cost and Fee Verification, attached?		■ YES ☐ NO ☐ N/A

Texas Commission on Environmental Quality
Form PI-1 General Application for
Air Preconstruction Permit and Amendment

XII. Delinquent Fees and Penalties
This form will not be processed until all delinquent fees and/or penalties owed to the TCEQ or the Office of the Attorney General on behalf of the TCEQ is paid in accordance with the Delinquent Fee and Penalty Protocol. For more information regarding Delinquent Fees and Penalties, go to the TCEQ Web site at: www.tceq.texas.gov/agency/delin/index.html.
XIII. Signature
The signature below confirms that I have knowledge of the facts included in this application and that these facts are true and correct to the best of my knowledge and belief. I further state that to the best of my knowledge and belief, the project for which application is made will not in any way violate any provision of the Texas Water Code (TWC), Chapter 7, Texas Clean Air Act (TCAA), as amended, or any of the air quality rules and regulations of the Texas Commission on Environmental Quality or any local governmental ordinance or resolution enacted pursuant to the TCAA I further state that I understand my signature indicates that this application meets all applicable nonattainment, prevention of significant deterioration, or major source of hazardous air pollutant permitting requirements. The signature further signifies awareness that intentionally or knowingly making or causing to be made false material statements or representations in the application is a criminal offense subject to criminal penalties.
Name: Melanie Little
Signature: Melanie Little *Original Signature Required*
Date: 3/14/2014