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Environmental and Sustainable Technology Evaluation - Biomass Co-firing in Industrial Boilers – Minnesota Power's Rapids Energy Center

Prepared by:



Southern Research Institute Under Subcontract to ERG



For:

U.S. Environmental Protection Agency Office of Research and Development – Environmental Technology Verification Program

EPA REVIEW NOTICE

This report has been peer and administratively reviewed by the U.S. Environmental Protection Agency, and approved for publication. Mention of trade names or commercial products does not constitute endorsement or recommendation for use.

U.S. Environmental Protection Agency

THE ENVIRONMENTAL TECHNOLOGY VERIFICATION PROGRAM

Environmental and Sustainable Technology Evaluation (ESTE)





ESTE Joint Verification Statement

TECHNOLOGY TYPE:	Biomass Co-firing
APPLICATION:	Industrial Boilers
TECHNOLOGY NAME:	Wood Waste Co-firing With Coal
COMPANY:	Minnesota Power, Rapids Energy Center
ADDRESS:	Grand Rapids, Minnesota

The U.S. Environmental Protection Agency (EPA) has created the Environmental Technology Verification (ETV) program to facilitate the deployment of innovative or improved environmental technologies through performance verification and dissemination of information. The goal of the ETV program is to further environmental protection by accelerating the acceptance and use of improved and cost-effective technologies. ETV seeks to achieve this goal by providing high-quality, peer-reviewed data on technology performance to those involved in the purchase, design, distribution, financing, permitting, and use of environmental technologies. This verification was conducted under the Environmental and Sustainable Technology Evaluation (ESTE) program, a component of ETV that was designed to address agency priorities for technology verification.

The goal of the ESTE program is to further environmental protection by substantially accelerating the acceptance and use of improved and innovative environmental technologies. The ESTE program was developed in in response to the belief that there are many viable environmental technologies that are not being used for the lack of credible third-party performance data. With performance data developed under this program, technology buyers, financiers, and permitters in the United States and abroad will be better equipped to make informed decisions regarding environmental technology purchase and use.

This ESTE project involved evaluation of co-firing common woody biomass in industrial, commercial or institutional coal-fired boilers. For this project ERG was the responsible contractor and Southern Research Institute (Southern) performed the work under subcontract. Client offices within the EPA, those with an explicit interest in this project and its results, include: Office of Air and Radiation (OAR), Combined Heat and Power (CHP) Partnership, Office of Air Quality Planning and Standards (OAQPS), Combustion Group, Office of Solid Waste (OSW), Municipal and Industrial Solid Waste Division, and ORD's Sustainable Technology Division. Letters of support have been received from the U.S. Department of Agriculture Forest Service and the Council of Industrial Boiler Owners.

TECHNOLOGY DESCRIPTION

Minnesota Power's Rapids Energy Center (REC) hosted this testing. REC provides power and heat for the neighboring Blandin Paper Mill in Grand Rapids, Minnesota. The facility has two identical Foster Wheeler Spreader Stoker Boilers installed in 1980 (Boilers 5 and 6). This verification was conducted on Boiler 5. Each boiler has a steaming capacity of approximately 175,000 lb/hour. The boilers can be fired with western subbituminous coal supplied by Decker Coal Company, located in the northwest section of the Powder River Basin, wood waste, railroad ties, on-site generated waste oils and solvents, and other paper wastes. Particulate emissions from each boiler are controlled by a Zurn multiclone dust collector and cold side electrostatic precipitator (ESP).

Waste wood and bark from the neighboring Blandin Paper mill, as well as waste wood from other local facilities, was co-fired with coal during this verification. The fuels (woody biomass and coal) are conveyed to the boiler separately and mixed on the stoker. Proximate analyses of the woody biomass used for this testing is as follows (wet weight basis):

Component	<u>% by Weight</u>
Moisture	46.5
Ash	1.28
Fixed carbon	27.3

The average heating value of the woody biomass was 4,645 Btu/lb.

Under normal operations, each boiler generates approximately 175,000 lb/h steam which is used to power a 15 MW steam turbine and provide process steam to the Blandin mill. The boilers typically cofire woody waste, primarily bark, at a nominal coal:biomass fuel ratio of 15:85 percent. The woody biomass waste is of sufficient supply nearly all year long with the exception of spring months. During periods of reduced wood waste supply the facility increases the amount of coal used to fuel the boilers.

VERIFICATION DESCRIPTION

This project was designed to evaluate changes in boiler performance due to co-firing woody biomass with coal. Boiler operational performance with regard to efficiency, emissions, and fly ash characteristics were evaluated while combusting 100 percent coal and then reevaluated while co-firing biomass with coal. The verification also addressed sustainability issues associated with biomass co-firing at this site.

The testing was limited to two operating points on Boiler 5:

- firing coal only at a typical nominal load
- firing a coal:biomass "co-firing" mixture of approximately 7:93 percent by weight at the same operating load

Under each condition, testing was conducted in triplicate with each test run approximately three hours in duration. In addition to the emissions evaluation, this verification addressed changes in fly ash composition. Fly ash can serve as a portland cement production component, structural fill, road materials, soil stabilization, and other beneficial uses. An important property that limits the use of fly ash is carbon content. Presence of metals in the ash, particularly mercury (Hg), can also limit fly ash use, such as in

cement manufacturing. Biomass co-firing could impact fly ash composition and properties, so this verification included evaluation of changes in fly ash carbon burnout (loss on ignition), minerals, and metals content.

During testing, the verification parameters listed below were evaluated. This list was developed based on project objectives cited by the client organizations and input from the Biomass Co-firing Stakeholder Group (BCSG).

Verification Parameters:

- Changes in emissions due to biomass co-firing including:
- Nitrogen oxides (NO_X)
- Sulfur dioxide (SO₂)
- Carbon monoxide (CO)
- Carbon dioxide (CO₂)
- Total particulates (TPM) (including condensable particulates)
- Primary metals: arsenic (As), selenium (Se), zinc (Zn), and Hg
- Secondary metals: barium (Ba), beryllium (Be), cadmium (Cd), chromium (Cr), copper (Cu), manganese (Mn), nickel (Ni), and silver (Ag)
- Hydrogen chloride (HCl) and hydrogen fluoride (HF)
- Boiler efficiency
- Changes in fly ash characteristics including:
- Carbon, hydrogen, and nitrogen (CHN), and SiO₂, Al₂O₃, and Fe₂O₃ content
- Primary metals: As, Se, Zn, and Hg
- Secondary metals: Ba, Be, Cd, Cr, Cu, Mn, Ni, and Ag
- fly ash fusion temperature

- Resource Conservation Recovery Act (RCRA) metals and Toxic Characteristic Leaching Procedure (TCLP).

• Sustainability indicators including CO₂ emissions associated with sourcing and transportation of biomass and ash disposal under baseline (no biomass co-firing) and test case (with biomass co-firing) conditions.

Rationale for the experimental design, determination of verification parameters, detailed testing procedures, test log forms, and QA/QC procedures can be found in Test and Quality Assurance Plan titled *Test and Quality Assurance Plan – Environmental and Sustainable Technology Evaluation Biomass Co-firing in Industrial Boilers.*

Quality Assurance (QA) oversight of the verification testing was provided following specifications in the ETV Quality Management Plan (QMP). Southern's QA Manager conducted a technical systems audit and an audit of data quality on a representative portion of the data generated during this verification and a review of this report. Data review and validation was conducted at three levels including the field team leader (for data generated by subcontractors), the project manager, and the QA manager. Through these activities, the QA manager has concluded that the data meet the data quality objectives that are specified in the Test and Quality Assurance Plan.

VERIFICATION OF PERFORMANCE

Boiler Efficiency

Test ID	Fuel	Heat Input (MMBtu/hr)	Heat Output (MMBtu/hr)	Efficiency (%)
Baseline 1		296.6	220.4	74.3
Baseline 2	100 % Coal	304.1	225.8	74.2
Baseline 3		295.7	221.3	74.9
Cofire 1	Blended Fuel (8	368.4	227.9	61.8
Cofire 2	Coal; 92 Woody biomass)	363.7	219.9	60.5
Cofire 3		357.8	220.1	61.5
Baseline Average		298.8	222.5	74.5 ± 0.3
Cofire Average		363.3	222.6	61.3 ± 0.7
Absolute Difference		64.5	0.1	-13.2
% Difference		21.8%	0.00%	-17.7%
Statistically Signi	ficant Change?	na	na	Yes

Table S-1. Boiler Efficiency

The average efficiencies during baseline (coal only) and co-firing tests were 74.5 ± 0.3 and 61.3 ± 0.7 percent respectively. This results in a statistically significant decrease of 17.7 percent efficiency when firing the blended fuel. The mass of woody fuel needed to provide an equal amount of heat is much greater. During baseline testing, an average 31,600 lb/h coal was consumed. During co-firing, fuel feed rates for coal and woody biomass averaged approximately 6,470 and 75,200 lb/h, respectively.

Emissions Performance

Test ID	Fuel	SO ₂	CO ₂	NOx	со
Baseline 1		0.489	167	0.533	0.229
Baseline 2	100 % Coal	0.485	160	0.540	0.210
Baseline 3		0.448	153	0.509	0.251
Cofire 1	Discolari	0.0013	131	0.188	0.680
Cofire 2	Blended Fuel	0.0014	127	0.193	0.337
Cofire 3	1 401	0.0012	134	0.201	0.649
Baseline Averages		0.474 ± 0.02	160 ± 7	0.527 ± 0.01	0.230 ± 0.02
Cofire Averages		0.0013 ± 0.0001	131 ± 4	0.194 ± 0.007	0.555 ± 0.2
% Difference		-99.7%	-18.3	-63.2%	142%
Statistically Significant C	Change?	Yes	Yes	Yes	Yes

Table S-2.	Gaseous	Pollutants	(Ib/MMBtu)

As expected SO₂ emissions were essentially eliminated using this high blend of woody biomass. NO_X emissions were also greatly reduced when co-firing (less fuel-bound nitrogen and lower thermal NO_X formation due to higher fuel moisture content, both shown in Table 3-1), and there was a statistically significant change in CO₂ emissions and a large increase in CO emissions. In similar testing at a different

facility, wood pellets were co-fired with coal at a much lower rate (about 15 percent) and at a much lower moisture content (about 7 percent). During that testing NO_X emissions were slightly increased and CO and CO_2 emissions were not significantly impacted. The two tests serve as a useful comparison between relatively dry and very moist woody fuels, and how this can impact emissions.

A large reduction in condensable particulates was evident while co-firing the woody fuel. Although there was not a significant change in emissions of filterable particulates, the total particulate emission rate was reduced by 81 percent due to the large decrease in condensable particulates.

Test ID	Fuel	Total Particulate	Filterable PM	Condensable PM
Baseline 1		0.0295	0.0044	0.0251
Baseline 2	100 % Coal	0.0277	0.0042	0.0236
Baseline 3		0.0379	0.0049	0.0262
Cofire 1		0.0088	0.0055	0.0050
Cofire 2	Blended Fuel	0.0029	0.0031	0.0030
Cofire 3		0.0062	0.0026	0.0021
Baseline Averages		0.0317 ± 0.005	0.0045 ± 0.0004	0.0249 ± 0.0013
Cofire Averages		0.0060 ± 0.003	0.0037 ± 0.002	0.0034 ± 0.0015
Absolute Difference		-0.0257	-0.0008	-0.0216
% Difference		-81.2%	-17.1%	-86.5%
Statistically Significa	ant Change?	Yes	No	Yes

Table S-3. Particulate Emissions (Ib/MMBtu)

Metals emissions were extremely low during all test periods. Changes in metals emissions on a percentage basis were large and quite variable across the elements analyzed, including the list of eight secondary metals. For the four primary metals shown, the reductions in mercury and selenium were statistically significant.

Emissions of HCl and HF were considerably lower during co-firing due the reduced levels of chlorine and fluorine in the fuel, showing decreases of approximately 62 and 77 percent, respectively. The reductions for both are statistically significant using the t-test.

Fly Ash Characteristics

Changes in ash characteristics were significant. Minerals content was much lower in the cofired fuel ash. Loss on ignition was significantly higher, indicating that the woody biomass is more difficult to fully combust. Changes in carbon content or fusion temperatures of the ash were not statistically significant. Quantitative flyash results are voluminous and not presented here, but can be viewed in the main body of the report in Tables 3-7 through 3-9.

Biomass co-firing during this verification did not impact the quality of the ash with regard to fly ash TCLP metals (40 CFR 261.24). Metals content was well below the TCLP requirements for all tests as shown in Table 3-8. Ash results did not meet the Class F Requirements (C 618-05) for use in concrete for either the baseline or co-fired fuels.

Sustainability Issues

- The REC receives woody biomass based fuel from the neighboring Blandin Mill and a wide variety of commercial suppliers throughout the northern plains region. During the first 6 months of 2007, the facility received a total of approximately 173,000 tons of woody biomass based fuel. Of that, approximately 83,000 tons came from the Blandin Mill, and the remaining 90,000 tons were purchased from commercial providers.
- Fuel and emissions associated with transportation of woody biomass to the Blandin Mill are not considered in this analysis since the woody biomass is transported to the facility whether used as fuel or not. Collected data show that approximately 33,000 gallons of diesel fuel was used to transport woody biomass based fuels from commercial suppliers to the REC (equating to an estimated 0.37 gallons per ton of woody biomass delivered). Based on an Energy Information Administration emission factor of 19.564 lbs CO₂/gallon, CO₂ emissions per ton of woody biomass based fuel transported to the facility are:

7.2 lbs CO_2 / ton woody biomass (0.37 gal fuel /ton pellets * 19.564 lbs CO_2 /gal). 648 tons CO_2 annually (7.2 lb/ton * 180,000 tons woody biomass delivered annually).

- Based on data generated during this testing, the CO₂ emission rates while firing straight coal and blended fuel (at a blending rate of approximately 92 percent woody biomass by mass) were 160 and 165 lb/MMBtu, respectively. However, combustion of wood-based fuel, which is composed of biogenic carbon, emits no appreciable CO₂ emissions under international greenhouse gas accounting methods developed by the IPCC and adopted by the ICFPA [6]. By analyzing the heat content of the coal and the woody biomass, the total boiler heat input for the test periods, and boiler efficiency, it was determined that approximately 90 percent of the heat generated during co-firing test periods is attributable to the wood-based fuel. It is therefore estimated that the CO₂ emissions offset during this testing is approximately 90 percent, or 148 lb/MMBtu at this co-firing blend. REC Boiler 5 typically operates around 220 MMBtu/hr heat generating rate. Assuming an availability and utilization rate of 75 percent for Boiler 5 at this heat rate, this would equate to estimated annual CO₂ emission reductions of approximately 107,000 tons per year.
- The mass of woody fuel needed to provide an equal amount of heat is much greater. During baseline testing, an average 31,600 lb/h coal was consumed. During co-firing, fuel feed rates for coal and woody biomass averaged approximately 6,470 and 75,200 lb/h, respectively.
- Biomass co-firing during this verification did not impact the quality of the ash with regard to fly ash TCLP metals (40 CFR 261.24). Metals content was well below the TCLP requirements for all tests. Ash results did not meet the Class F Requirements (C 618-05) for use in concrete for either the baseline or co-fired fuels. As such, biomass co-firing did not impact either sustainability issue since the quality of the ash with regard to fly ash TCLP metals and Class F Requirements was unchanged.

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Details on the verification test design, measurement test procedures, and Quality Assurance/Quality Control (QA/QC) procedures can be found in the Test Plan titled *Test and Quality Assurance Plan – Environmental and Sustainable Technology Evaluation Biomass Co-firing in Industrial Boilers*. (Southern 2006). Detailed results of the verification are presented in the Final Report titled *Environmental and Sustainable Technology Evaluation Biolers – Minnesota Power's Rapids Energy Center* (Southern 2007). Both can be downloaded from Southern's web-site (<u>www.sri-rtp.com</u>) or the ETV Program web-site (<u>www.epa.gov/etv</u>).

Signed by: Sally Gutierrez – April 28, 2008

Sally Gutierrez Director National Risk Management Research Laboratory Office of Research and Development Tim Hansen – April 3, 2008

Tim Hansen Program Director Southern Research Institute

Notice: This verification was based on an evaluation of technology performance under specific, predetermined criteria and the appropriate quality assurance procedures. The EPA and Southern Research Institute make no expressed or implied warranties as to the performance of the technology and do not certify that a technology will always operate at the levels verified. The end user is solely responsible for complying with any and all applicable Federal, State, and Local requirements. Mention of commercial product names does not imply endorsement or recommendation.

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Southern Research Institute

Environmental and Sustainable Technology Evaluation

Biomass Co-firing in Industrial Boilers

Minnesota Power's Rapids Energy Center

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Acronyms and Abbreviations

Ag As Ba Be BCSG Btu Btu/h	silver arsenic barium beryllium Biomass Co-firing Stakeholder Group British thermal unit British thermal unit per hour	OAR OSW ppmvd psig REC Se SO ₂ T	Office of Air and Radiation Office of Solid Waste parts per million by volume, dry pounds per square inch, gauge Rapids Energy Center selenium sulfur dioxide tons (English)
Cd CEMS	cadmium continuous emissions monitoring system	TCLP	Toxic Characteristic Leaching Procedure.
CHN CHP CO CO ₂	carbon, hydrogen, and nitrogen combined heat and power carbon monoxide carbon dioxide chromium	TPM TQAP Zn °F	total particulate matter test and quality assurance plan zinc degrees Fahrenheit
Cr Cu DQO EPA-ORD	copper data quality objective Environmental Protection		
	Agency Office of Research and Development		
ESP ESTE	electrostatic precipitator Environmental and Sustainable Technology Evaluation		
ETV	Environmental Technology Verification		
gr/dscf	grains per dry standard cubic foot		
HCl HF Hg ICI	hydrogen chloride hydrogen fluoride mercury industrial-commercial-		
kW	institutional kilowatt		
lb/h lb/lb-mol	pounds per hour pounds per pound-mole		
MMBtu/h	million British thermal units per hour		
Mn MQO MW	manganese measurement quality objective megawatt		
Ni NO	nickel		
$NO_X O_2$	nitrogen oxides oxygen		
QA/QC	quality assurance / quality control		
OAQPS	Office of Air Quality Planning and Standards		

ACKNOWLEDGMENTS

Southern Research Institute wishes to thank the ETV-ESTE program management, especially Theresa Harten, David Kirchgessner, and Robert Wright for supporting this verification and reviewing and providing input on the testing strategy and this Verification Report. Thanks are also extended to the Rapids Energy Center for hosting the test, especially Compliance Superintendent Doug Tolrud, Plant Engineer Jim Uzelak, Lead Station Operator Gordon Ranta, and Instrument and Lab Specialist Nick Wooner. Their input supporting the verification and assistance with coordinating field activities was invaluable to the project's success.

1.0 INTRODUCTION

1.1 BACKGROUND

The U.S. Environmental Protection Agency's Office of Research and Development (EPA-ORD) operates the Environmental and Sustainable Technology Evaluation (ESTE) program to facilitate the deployment of innovative technologies through performance verification and information dissemination. In part, the ESTE program is intended to increase the relevance of Environmental Technology Verification (ETV) Program projects to the U.S. EPA program and regional offices.

The goal of the ESTE program is to further environmental protection by substantially accelerating the acceptance and use of improved and innovative environmental technologies. The ESTE program was developed in response to the belief that there are many viable environmental technologies that are not being used for the lack of credible third-party performance data. With performance data developed under this program, technology buyers, financiers, and permitters in the United States and abroad will be better equipped to make informed decisions regarding environmental technology purchase and use.

The ESTE program involves a three step process. The first step is a technology category selection process conducted by ORD. The second step involves selection of the project team and gathering of project collaborators and stakeholders. Collaborators can include technology developers, vendors, owners, and users and support the project through funding, cost sharing, and technical support. Stakeholders can include representatives of regulatory agencies, trade organizations relevant to the technology, and other associated technical experts. The project team relies on stakeholder input to improve the relevance, defensibility, and usefulness of project outcomes. Both collaborators and stakeholders are critical to development of the project test and quality assurance plan (TQAP), the end result of step two. Step three includes the execution of the verification and quality assurance and review process for the final reports.

This ESTE project involved evaluation of co-firing common woody biomass in industrial, commercial or institutional coal-fired boilers. For this project ERG was the responsible contractor and Southern Research Institute (Southern) performed the work under subcontract. Client offices within the EPA, those with an explicit interest in this project and its results, include: Office of Air and Radiation (OAR), Combined Heat and Power (CHP) Partnership, Office of Air Quality Planning and Standards (OAQPS), Combustion Group, Office of Solid Waste (OSW), Municipal and Industrial Solid Waste Division, and ORD's Sustainable Technology Division. Letters of support have been received from the U.S. Department of Agriculture Forest Service and the Council of Industrial Boiler Owners.

With increasing concern about global warming and fossil fuel energy supplies, there continues to be an increasing interest in biomass as a renewable and sustainable energy source. Many studies and research projects regarding the efficacy and environmental impacts of biomass co-firing have been conducted on large utility boilers, but less data is available regarding biomass co-firing in industrial size boilers. As such, OAQPS has emphasized an interest in biomass co-firing in industrial-commercial-institutional (ICI) boilers in the 100 to 1000 million British thermal units per hour (MMBtu/h) range. The reason for this emphasis is to provide support for development of a new area-source "Maximum Achievable Control Technology" standard.

The focus for this project was to evaluate performance and emission reductions for ICI boilers as a result of biomass co-firing. The primary objectives of this project were to:

- Evaluate changes in boiler emissions due to biomass co-firing
- Evaluate boiler efficiency with biomass co-firing
- Examine any impact on the value and suitability of fly ash for beneficial uses (carbon and metals content)
- Evaluate sustainability indicators including emissions from sourcing and transportation of biomass and disposal of fly ash

This document is one of two Technology Evaluation Reports for this ESTE project. This report presents results of the testing conducted on Unit 5 at Minnesota Power's Rapids Energy Center (REC) in Grand Rapids, Minnesota. This report includes the following components:

- Brief description of the verification approach and parameters (§ 2.0)
- Description of the test location (§ 2.1)
- Brief description of sampling and analytical procedures (§ 2.2)
- Test results (§ 3.0)
- Data quality (§ 4.0)

This report has been reviewed by representatives of ORD, OAQPS, OSW, the EPA QA team, and the project stakeholders and collaborators. It documents test operations and verification results. It is available in electronic format from Internet sites maintained by Southern (<u>www.sri-rtp.com</u>) and ETV program (<u>www.epa.gov/etv</u>).

2.0 VERIFICATION APPROACH

This project was designed to evaluate changes in boiler performance due to co-firing woody biomass with coal. Boiler operational performance with regard to efficiency, emissions, and fly ash characteristics were evaluated while combusting 100 percent coal and then reevaluated while co-firing biomass with coal. The verification also addressed sustainability issues associated with biomass co-firing at this site.

The testing was limited to two operating points on Unit 5 at REC:

- firing coal only at a typical nominal load
- firing a coal:biomass "co-firing" mixture of approximately 8:92 percent by weight at the same operating load

In addition to the emissions evaluation, this verification addressed changes in fly ash composition. Fly ash can serve as a portland cement production component, structural fill, road materials, soil stabilization, and other beneficial uses. An important property that limits the use of fly ash is carbon content. Presence of metals in the ash, particularly mercury (Hg), can also limit fly ash use, such as in cement manufacturing. Biomass co-firing could impact fly ash composition and properties, so this verification included evaluation of changes in fly ash carbon burnout (loss on ignition), minerals, and metals content.

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- Secondary metals: barium (Ba), beryllium (Be), cadmium (Cd), chromium (Cr), copper (Cu), manganese (Mn), nickel (Ni), and silver (Ag)
- Hydrogen chloride (HCl) and hydrogen fluoride (HF)
- Boiler efficiency
- Changes in fly ash characteristics including:
- Carbon, hydrogen, and nitrogen (CHN), and SiO₂, Al₂O₃, and Fe₂O₃ content
- Primary metals: As, Se, Zn, and Hg
- Secondary metals: Ba, Be, Cd, Cr, Cu, Mn, Ni, and Ag
- fly ash fusion temperature
- Resource Conservation Recovery Act (RCRA) metals and Toxic Characteristic Leaching Procedure (TCLP).

 Sustainability indicators including CO₂ emissions associated with sourcing and transportation of biomass and ash disposal under baseline (no biomass co-firing) and test case (with biomass cofiring) conditions.

2.1 HOST FACILITY AND TEST BOILER

Testing was conducted on two industrial boilers that are capable of co-firing woody biomass. The two units that hosted tests were Minnesota Power's REC Boiler 5 (MP-5) and the University of Iowa Main Power Plant's Boiler 10 (UI-10). Results of the UI-10 testing are published under separate cover and can be found at www.sri-rtp.com.

Minnesota Power's REC provides power and heat for the neighboring Blandin Paper Mill in Grand Rapids, Minnesota. The facility has two identical Foster Wheeler Spreader Stoker Boilers installed in 1980 (Boilers 5 and 6). This verification was conducted on Boiler 5. Each boiler has a steaming capacity of approximately 175,000 lb/hour. The boilers can be fired with western subbituminous coal supplied by Decker Coal Company, located in the northwest section of the Powder River Basin, wood waste, railroad ties, on-site generated waste oils and solvents, and other paper wastes. Particulate emissions from each boiler are controlled by a Zurn multiclone dust collector and cold side electrostatic precipitator (ESP). Cleaned flue gas from each boiler exhausts to the atmosphere via a common stack which is 205 feet above elevation and has an inner diameter of 9 feet. Figure 2-1 is a schematic of the boilers.

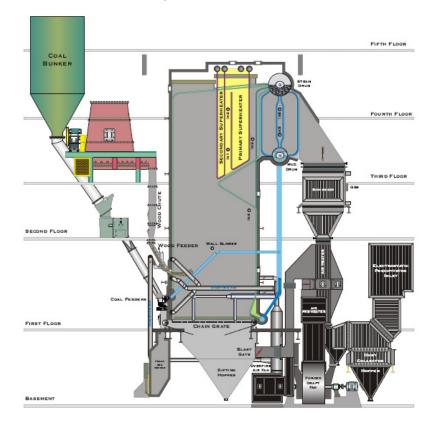


Figure 2-1. Minnesota Power's Foster Wheeler Spreader Stokers

Since both boilers exhaust through a common stack, emission testing for this program was conducted in the ductwork of the selected boiler upstream of the stack. The testing location and ports are shown in Figure 2-2.



Figure 2-2. Emission Testing Ports for MP-5

Under normal operations, each boiler generates approximately 175,000 lb/h steam which is used to power a 15 MW steam turbine and provide process steam to a nearby industrial facility. The boilers typically co-fire woody waste, primarily bark, at a nominal coal:biomass fuel ratio of 15:85 percent. The woody biomass waste is of sufficient supply nearly all year long with the exception of spring months. During periods of reduced wood waste supply the facility increases the amount of coal used to fuel the boilers. More details regarding the fuels used for this test is presented in Section 2.2.2.

Fly ash generated by this boiler is collected from the dust collector and precipitator and distributed to farms for crop use as long as the fuel blend is less than 50 percent coal. In 2003, approximately 7,700 tons of ash was distributed to farms. When coal exceeds 50 percent, the ash is landfilled.

The systems data control system (DCS) includes a PI Historian software package that allows the facility to customize data acquisition, storage, and reporting activities. Each boiler is also equipped with continuous emission monitoring systems (CEMS) that record NO_X , SO_2 , CO, and O_2 concentrations and emission rates. Table 2-1 summarizes the CEMS on each boiler.

Parameter	Instrument Make/Model	Instrument Range	Reporting Units
	Teledyne Monitor Labs		
NO _X	(TML) 41-H-O2	0 – 500 ppm	lb/MMBtu
SO_2	TML 50-H	0 – 1000 ppm	lb/MMBtu
СО	TML 30-M	0 – 5000 ppm	lb/MMBtu
O ₂	TML 41-H-O2	0-25 %	%

Table 2-1.MP-5 CEMS

The facility has a fully equipped control room that continuously monitors boiler operations. Operational parameters that were recorded during this test program include the following:

- Heat input, (Btu/h)
- Steam flow (lb/h)
- Steam pressures (psig) and temperatures (°F)
- Air flows (lb/h) and temperatures (°F)
- Power output (MW)
- SO₂ emissions (lb/MMBtu)
- ESP variables (volts, amperes, fields on line), recorded manually

Data recorded during each test period was averaged over the test period and reported to document boiler operations during the testing, co-firing rates, and boiler efficiency. Key parameters such as heat input and steam flow are summarized in the results section of this report. Dust collector and ESP operational data are summarized in Appendix E.

2.2 FIELD TESTING

Waste wood and bark from the neighboring Blandin Paper mill, as well as waste wood from other local facilities, was co-fired with coal during this verification. The fuels (woody biomass and coal) are conveyed to the boiler separately and mixed on the stoker. Figure 2-3 shows the woody biomass conveyer during verification testing.



Figure 2-3. Rapids Energy Woody biomass Feed

Proximate analyses of the woody biomass used for this testing is as follows (wet weight basis):

<u>Component</u>	<u>% by Weight</u>
Moisture	46.5
Ash	1.28
Fixed carbon	27.3

The average heating value of the woody biomass was 4,645 Btu/lb. These values are the average of three composite samples collected on the day of testing and may not reflect variability in the woody biomass used at REC.

2.2.1 Field Testing Matrix

A set of three replicate tests were conducted while firing coal only on March 28, 2007. The following day, a second set of three tests were conducted while firing primarily woody biomass co-fired with a small amount of coal. Duration of each test run was approximately 120 minutes. Other than changes in fuel composition, all other boiler operations were replicated as closely as possible during test sets. Test and sampling procedures were also consistent between sets of tests. Table 2-2 summarizes the test matrix.

Date	Time	Test ID	Fuel	Heat Input (MMBtu/h)	Steam Flow (Klb/h)
	0940 – 1215	Baseline 1	100 % coal	296.6	153.6
03-28-07	1250 – 1520	Baseline 2		304.1	157.3
	1555 - 1825	Baseline 3		295.7	154.2
	0815 - 1050	Cofire 1	Blended Fuel	293.5	159.2
03-29-07	1228 - 1500	Cofire 2	(8 % Coal; 92	285.2	153.7
03-29-07			% woody		153.9
	1520 - 1750	Cofire 3	biomass)	285.6	

Table 2-2. Rapids Energy Boiler 5 Test Periods

All testing was conducted during stable boiler operations (defined as boiler steam flows varying by less than 5 percent over a 5 minute period). Southern representatives coordinated testing activities with boiler operators to ensure that all testing was conducted at the desired boiler operating set points and the boiler operational data needed to calculate efficiency was properly logged and stored. Southern also supervised all emissions testing activities.

2.3 BOILER PERFORMANCE METHODS AND PROCEDURES

Conventional field testing protocols and reference methods were used to determine boiler efficiency, emissions, and fly ash properties. A brief description of the methods and procedures is provided here. Details regarding the protocols and methods proposed are provided in the document titled: *Test and Quality Assurance Plan – Environmental and Sustainable Technology Evaluation – Biomass Co-firing in Industrial Boilers* [1].

2.3.1 Boiler Efficiency

Boiler efficiency was determined following the Btu method in the B&W Steam manual [2]. The efficiency determinations were also used to estimate boiler heat input during each test period. The facility logs all of the data required for determination of boiler efficiency on a regular basis. Certain parameters such as ambient conditions and flue gas temperatures were independently measured by Southern. Table 2-3 summarizes the boiler operational parameters logged during testing and the source and logging frequency for each.

Operational Parameter	Source of Data	Logging Frequency
Intake air temperature, °F	Southern measurements	Five minute intervals
Flue gas temperature at air heater inlet, °F		
Fuel temperature, °F	Southern measurements	Twice per test run
Moisture in air, lb/lb dry air		
Fuel consumption, lb/h	Facility PI Historian Control	One minute averages
Combustion air temperature, °F	System	
Steam flow, MMBtu/h or lb/h		
Steam pressure, psig		
Steam temperature, °F		
Supply water pressure, psig		
Supply water temperature, °F		
Power generation, kW		
Fuel ultimate analyses, both woody	Analytical laboratory	One composite coal,
biomass and coal		mixed fuel, and fly ash
Fuel heating value, Btu/lb		sample per test (3 total for
Unburned carbon loss, %		each condition)

Table 2-3.	Summary of	of Boiler	Efficiency	Parameters

Fuel feed rates were monitored during the verification testing to confirm fuel blending rates (fuel feed rate is not required for the boiler efficiency calculations via the Btu method). Woody biomass feed rates to the boiler are monitored by the site using a belt scale. Coal firing rates are determined by counting and recording the number of hopper releases over a given period of time, and assigning an assumed mass of coal per release. The coal feed rate data were later determined to be invalid. Therefore, fuel blending rate was derived using the total calculated heat input, the measured woody biomass feed rate, and the measured heating value of the woody biomass and the coal.

2.3.1.1 Fuel Sampling and Analyses

Fuel samples were collected during each test run for ultimate and heating value analysis. A composite of grab samples of coal and biomass were prepared during co-firing test runs and submitted to Wyoming Analytical Laboratories, Inc. in Laramie, Wyoming for the analyses shown in Table 2-4.

Parameter	Method
Ultimate analysis	ASTM D3176
Gross calorific value	ASTM D5865 (coal) ASTM
	E711-87 (biomass)

Table 2-4.	Summary	of Fuel	Analyses
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Grab samples of each fuel (coal and woody biomass separately) were collected from the fuel conveyers immediately above the stoker feed hopper. The grabs contained approximately one lb of fuel and were collected at 30 minute intervals during each test run and combined in a large pail. One mixed composite sample of approximately one lb each fuel was generated for each test run, sealed and submitted for analysis. Collected composite samples were labeled, packed and shipped to Wyoming Analytical along

with completed chain-of-custody documentation for off-site analysis. These samples were submitted to the field team leader for subsequent analysis. The ultimate analysis reported the following fuel constituents as percent by weight (wet):

• carbon

- sulfurnitrogen
- hydrogenoxygen

waterash

The efficiency analysis requires the unburned carbon loss value, or carbon content of fly ash. Fly ash samples were also collected during each test run and submitted for analysis. Prior to each test run, precipitator ash hoppers were cleared of residual ash. Grab samples of ash were then collected from a hopper at 30 minute intervals during each test run and combined in a gallon size metal ash sampling can. Collected ash samples were then sealed in plastic bags, labeled, packed and shipped to Wyoming Analytical along with completed chain-of-custody documentation for off-site analysis. Results of these analyses were used to complete the combustion gas calculations in the Btu method.

2.3.2 Boiler Emissions

Testing was conducted on each boiler to determine emissions of the following atmospheric pollutants:

- nitrogen oxides (NO_x)
- sulfur dioxide (SO₂)
- carbon monoxide (CO)
- carbon dioxide (CO₂)
 primary metals (As,

Hg, Se, Zn)

- secondary metals
- acid gases (HCl, HF)

- particulate matter (filterable and condensable)
- Emission rates for NO_X , SO_2 , and CO were determined continuously using the facility's continuous emissions monitoring system (CEMS). For all other parameters, a total of three replicate test runs were conducted under both the baseline (coal only) and co-firing operating conditions. Each test run was approximately 120 minutes in duration.

Measurements required for emissions tests include:

- fuel heat input, Btu/h (via boiler efficiency, Section 2.3.1)
- pollutant and O₂ concentrations, parts per million (ppm), grains per dry standard cubic foot (gr/dscf), or percent
- flue gas molecular weight, pounds per pound-mole (lb/lb-mol)
- flue gas moisture concentration, percent
- flue gas flow rate, dry standard cubic feet per hour (dscfh)

The average concentrations established as part of each test run are reported in units of ppmvd for NO_X , CO, SO₂, HCl, and HF, and percent for CO₂. Concentrations of total particulate matter are reported as grains per dry standard cubic foot (gr/dscf). The average emission rates for each pollutant are also reported in units of pounds per hour (lb/h), and pounds per million Btu (lb/MMBtu).

All testing was conducted by GE Energy following EPA Reference or Conditional Methods for emissions testing [3]. Table 2-5 summarizes the reference methods used and the fundamental analytical principle for each method.

Parameter or Measurement	U.S. EPA Reference Method	Principle of Detection
CO ₂	3A	Non-dispersive infra-red
TPM	5	Gravimetric
condensable PM	CTM040/202	Gravimetric
Metals	29	Inductively coupled plasma / cold vapor atomic absorption spectroscopy
HCI, HF	26	lon chromatography
Moisture	4	Gravimetric
Flue gas flow rate	2	Pitot traverse

Table 2-5.	Summary of Emission Test Me	ethods and Analytical Equipment
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2.3.3 Fly ash Characteristics

Fly ash samples were collected during the efficiency and emissions testing periods to evaluate the impact of biomass co-firing on ash composition. Fly ash samples were collected from from the ESP collection hoppers during each test run. Hoppers were cleaned out between runs. Collected samples were submitted to Wyoming Analytical along with completed chain-of-custody documentation for determination of the parameters listed below. The laboratory also conducted tests to evaluate ash fusion temperature, and airentraining agents index. Results are compared to the Class F (bituminous and anthracite) or Class C (lignite and sub bituminous) fly ash specifications. Table 2-6 summarizes the analytical methods that were used.

Parameter	Method
CHN	ASTM D5373
minerals	ASTM D4326-04
RCRA metals	SW-846 3052/6010
Metals TCLP	SW-846 1311/6010
Air-entraining agents index	Foam Index Test
Fly ash fusion temperature	ASTM D1857

Table 2-6. Summary of Fly ash Analyses

2.4 SUSTAINABILITY INDICATORS AND ISSUES

Sustainability is an important consideration regarding use of woody biomass as a renewable fuel source. This project evaluated certain sustainability issues for the Rapids Energy facility. The following sustainability related issues were examined:

- Estimated daily and annual woody biomass consumption at the nominal co-firing rate
- Biomass delivery requirements (distance and mode)
- Coal delivery requirements (distance and mode)

Biomass Consumption, Type, and Source

The projected daily and annual biomass consumption rate is useful in determining whether the supply of biomass is sustainable. Biomass consumption rates measured during the testing conducted at each site were used as the basis to estimate daily and annual biomass consumption for each site. The source, type, and compositional analyses of the biomass was documented during testing.

Associated GHG Emissions

By evaluating the average biomass consumption rate during the testing, upstream CO_2 emissions associated with the biomass supply were estimated. The distance between the biomass source and the boiler tested along with CO_2 emission factors for the modes of transportation used to deliver the biomass were used to complete this analysis. Emission factors were determined based on EPA's AP 42 Emission Factors Database [4].

Solid Waste Issues (Ash utilization)

Results of the baseline coal fly ash analyses and the co-fired fuel fly ash analyses were compared to determine if co-firing biomass has a measurable impact on the carbon content of the ash with respect to ASTM standards for cement admixtures. In addition, results of the RCRA metals analyses for the baseline and co-fire ash were compared to evaluate impact on metals content. The metals TCLP analytical results were used to examine if co-firing impacts fly ash characteristics with respect to the TCLP standards cited in 40 CFR 261.24 [5].

3.0 RESULTS

Results of the testing are summarized in the following sections. Field and analytical data generated during the verification are presented in Appendices A through D including detailed emissions testing data, fuel and ash analyses, boiler efficiency calculations, and REC woody biomass delivery records. As expected, the facility was able to operate under both conditions (coal only and co-firing) without difficulties. Due to lack of demand from the host paper mill, all testing was conducted at approximately 88 percent of boiler capacity (approximately 155,000 lb/h steam). Using the total calculated heat input, the measured woody biomass feed rate, and the measured heating value of the woody biomass and the coal, the fuel blending rate was determined to be an average of 8 percent coal and 92 percent woody biomass during co-firing.

As part of the data analysis, results were analyzed to evaluate changes in boiler performance and fly ash characteristics between the two sets of tests. Standard deviations of the replicate measurements conducted under each fueling condition and a statistical analysis (t-test with a 90 percent confidence interval) were used to verify the statistical significance of any observed changes in emissions or efficiency.

3.1 BOILER EFFICIENCY

Table 3-1 summarizes the major fuel characteristics for both coal and blended fuel. Detailed fuel analyses, including results on a dry basis, are presented in Appendix B.

Test ID	Fuel	Moisture (%)	Carbon (%)	Nitrogen (%)	Sulfur (%)	Ash (%)	Heating Value (Btu/Ib)
Baseline 1		23.5	54.2	0.93	0.33	3.95	9,445
Baseline 2	100 % Coal	23.6	54.8	1.12	0.33	3.59	9,491
Baseline 3		23.9	54.4	0.54	0.33	3.98	9,422
Cofire 1	Blended	43.6	29.6	0.30	0.04	1.65	5,025
Cofire 2	Fuel (8	46.0	29.0	0.42	0.05	1.16	4,930
Cofire 3	Coal; 92 woody biomass)	44.7	29.4	0.44	0.04	1.79	5,085
Baseline Averages		23.7	54.5	0.86	0.33	3.84	9,453
Cofire Averages		44.8	29.3	0.39	0.04	1.53	5,014
% Difference		89.2%	-46.2%	-55.2%	-86.9%	-60.1%	-47.0%

 Table 3-1. Fuel Characteristics (as received)

As expected, the moisture content of the blended fuel was much higher than the coal, and carbon, ash and heating values were much lower.

The average efficiencies during baseline (coal only) and co-firing tests were 74.5 ± 0.3 and 61.3 ± 0.7 percent respectively. This results in a statistically significant decrease of 17.7 percent efficiency when

firing the blended fuel. Combustion appeared to occur higher up the boiler with; this was observed by the camera inside the boiler. Table 3-2 summarizes boiler efficiency during the test periods

Test ID	Fuel	Heat Input (MMBtu/hr)	Heat Output (MMBtu/hr)	Efficiency (%)
Baseline 1		296.6	220.4	74.3
Baseline 2	100 % Coal	304.1	225.8	74.2
Baseline 3		295.7	221.3	74.9
Cofire 1	Blended Fuel (8	368.4	227.9	61.8
Cofire 2	Coal; 92 Woody	363.7	219.9	60.5
Cofire 3	biomass)	357.8	220.1	61.5
Baseline Average		298.8	222.5	74.5 ± 0.3
Cofire Average		363.3	222.6	61.3 ± 0.7
Absolute Difference		64.5	0.1	-13.2
% Difference		21.8%	0.00%	-17.7%
Statistically Signi	ficant Change?	na	na	Yes

Table 3	3-2.	Boiler	Efficiency
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The mass of woody fuel needed to provide an equal amount of heat is much greater. During baseline testing, an average 31,600 lb/h coal was consumed. During co-firing, fuel feed rates for coal and woody biomass averaged approximately 6,470 and 75,200 lb/h, respectively.

3.2 BOILER EMISSIONS

Table 3-3 summarizes emission rates for the gaseous pollutants evaluated. As expected SO₂ emissions were essentially eliminated using this high blend of woody biomass. NO_X emissions were also greatly reduced when co-firing (less fuel-bound nitrogen and lower thermal NO_X formation due to higher fuel moisture content, both shown in Table 3-1), and there was a statistically significant change in CO₂ emissions and a large increase in CO emissions. In similar testing at a different facility, wood pellets were co-fired with coal at a much lower rate (about 15 percent) and at a much lower moisture content (about 7 percent). During that testing NO_X emissions were slightly increased and CO and CO₂ emissions were not significantly impacted. The two tests serve as a useful comparison between relatively dry and very moist woody fuels, and how this can impact emissions.

Regarding CO_2 emissions, it should be noted that combustion of wood-based fuel, which is composed of biogenic carbon, emits no appreciable CO_2 emissions under international greenhouse gas accounting methods developed by the Intergovernmental Panel of Climate Change (IPCC) and adopted by the International Council of Forest and Paper Associations (ICFPA). Therefore, the facility realizes a significant annual reduction in CO_2 emissions when co-firing wood (see Section 3.4.1)

Test ID	Fuel	SO ₂	CO ₂	NO _x	СО
Baseline 1		0.489	167	0.533	0.229
Baseline 2	100 % Coal	0.485	160	0.540	0.210
Baseline 3		0.448	153	0.509	0.251
Cofire 1	Blended	0.0013	131	0.188	0.680
Cofire 2	Fuel	0.0014	127	0.193	0.337
Cofire 3	1 dei	0.0012	134	0.201	0.649
Baseline Averages		0.474 ± 0.02	160 ± 7	0.527 ± 0.01	0.230 ± 0.02
Cofire Averages		0.0013 ± 0.0001	131 ± 4	0.194 ± 0.007	0.555 ± 0.2
% Difference		-99.7%	-18.3	-63.2%	142%
Statistically Significant	Change?	Yes	Yes	Yes	Yes

Table 3-4 summarizes results of filterable, condensable, and total particulate emissions.

Test ID	Fuel	Total Particulate	Filterable PM	Condensable PM
Baseline 1		0.0295	0.0044	0.0251
Baseline 2	100 % Coal	0.0277	0.0042	0.0236
Baseline 3		0.0379	0.0049	0.0262
Cofire 1	Blended	0.0088	0.0055	0.0050
Cofire 2	Fuel	0.0029	0.0031	0.0030
Cofire 3		0.0062	0.0026	0.0021
Baseline Averages		0.0317 ± 0.005	0.0045 ± 0.0004	0.0249 ± 0.0013
Cofire Averages		0.0060 ± 0.003	0.0037 ± 0.002	0.0034 ± 0.0015
Absolute Difference		-0.0257	-0.0008	-0.0216
% Difference		-81.2%	-17.1%	-86.5%
Statistically Signification	ant Change?	Yes	No	Yes

 Table 3-4. Particulate Emissions (lb/MMBtu)

A large reduction in condensable particulates was evident while co-firing the woody fuel. Although there was not a significant change in emissions of filterable particulates, the total particulate emission rate was reduced by 81 percent due to the large decrease in condensable particulates. Dust collector and ESP operational data presented in Appendix E indicate that conditions were consistent between the two sets of runs with regard to control device operations.

			1	1	
Test ID	Fuel	Arsenic	Mercury	Selenium	Zinc
Baseline 1	100 %	9.61E-07	2.44E-06	2.04E-06	2.56E-05
Baseline 2	Coal	2.11E-06	2.40E-06	2.13E-06	1.53E-05
Baseline 3	oou	8.12E-07	2.07E-06	2.35E-06	1.45E-05
Cofire 1	Dlandad	4.83E-07	9.39E-07	6.11E-07	1.91E-05
Cofire 2	Blended Fuel	4.67E-07	7.84E-07	8.83E-07	2.51E-05
Cofire 3	i uei	4.89E-07	8.33E-07	9.05E-07	2.20E-05
		1.29E-06 ±	2.30E-06 ±	2.18E-06 ±	1.84E-05 ±
Baseline Averages		7.71E-07	2.01E-07	1.60E-07	6.20E-06
		4.80E-07 ±	8.52E-07 ±	8.00E-07 ±	2.21E-05 ±
Cofire Averages		8.42E-09	9.36E-08	2.10E-07	4.04E-06
Absolute Difference		-8.15E-07	-1.45E-06	-1.38E-06	3.64E-06
% Difference		-62.9%	-63.0%	-63.2%	19.5%
Statistically Significa	nt Change?	No	Yes	Yes	No

Metals emissions (primary metals summarized in Table 3-5) were extremely low during all test periods. Changes in metals emissions on a percentage basis were large and quite variable across the elements analyzed, including the list of eight secondary metals. Absolute differences are shown in the table to demonstrate how low metals emissions were, causing the large changes on a percent difference basis. For the four primary metals shown, the reductions in mercury and selenium were statistically significant.

Acid gas emissions are summarized below. Emissions of HCl and HF were considerably lower during co-firing due the reduced level of chlorine in the fuel. The reductions for both are is statistically significant using the t-test.

Test ID	Fuel	Hydrochloric Acid, HCl	Hydrofluoric Acid, HF
Baseline 1		4.83E-04	2.18E-03
Baseline 3	100 % Coal	6.07E-04	2.25E-03
Baseline 3		5.45E-04	2.07E-03
Cofire 1		3.35E-04	6.08E-04
Cofire 2	Blended Fuel	1.45E-04	3.74E-04
Cofire 3		1.37E-04	5.06E-04
Baseline Averages		5.45E-04 ± 6.21E-05	2.17E-03 ± 9.11E-05
Cofire Averages		2.06E-04 ± 1.12 E-04	4.96E-04 ± 1.17E-04
Absolute Difference		-3.39E-04	-1.67E-03
% Difference		-62.3%	-77.1%
Statistically Signific	ant Change?	Yes	Yes

 Table 3-6. Acid Gas Emissions (lb/MMBtu)

3.3 FLYASH CHARACTERISTICS

Results of the flyash analyses are summarized in Tables 3-7 through 3-9. Changes in ash characteristics were significant. Minerals content was much lower in the cofired fuel ash. Loss on ignition was significantly higher, indicating that the woody biomass is more difficult to fully combust. Changes in carbon content or fusion temperatures of the ash were not statistically significant.

Biomass co-firing during this verification did not impact the quality of the ash with regard to fly ash TCLP metals (40 CFR 261.24). Metals content was well below the TCLP requirements for all tests as shown in Table 3-8. Ash results did not meet the Class F Requirements (C 618-05) for use in concrete for either the baseline or co-fired fuels.

							Ash Fusior	n Temp., ℉
Test ID	Fuel	Carbon, wt %	Silicon Dioxide, % as SiO₂	Aluminum Oxide, % as Al₂O₃	Iron Oxide, % as Fe ₂ O ₃	Loss on Ignition	Reducing Atmosphere: Initial Deformation	Oxidizing Atmosphere: Initial Deformation
Baseline 1	100 %	7.11	14.2	7.99	2.40	12.1	2,332	2,310
Baseline 2	Coal	8.34	12.9	8.48	2.48	11.3	2,188	2,328
Baseline 3	000	9.00	13.8	9.84	2.76	11.1	2,181	2,334
Cofire 1	Dlandad	8.49	7.83	3.81	1.38	16.2	2,402	2,393
Cofire 2	Blended Fuel	10.3	6.21	3.23	1.30	18.3	2,390	2,692
Cofire 3		9.57	6.13	3.01	1.25	17.9	2,388	2,005
Baseline Averages		8.15 ± 0.9	13.6 ± 0.7	8.77 ± 0.9	2.55 ± 0.2	11.5 ± 0.5	2,234 ± 85	2,324 ± 12
Cofire Averages		9.47 ± 0.9	6.72 ± 0.9	3.35 ± 0.4	1.31 ± 0.07	17.5 ± 1.1	2,393 ± 6	2,363 ± 340
% Difference		14.9%	-67.9%	-89.4%	-64.1%	41.0%	6.90%	1.68%
Statistically Significant	t Change?	No	Yes	Yes	Yes	Yes	No	No

Table 3-7. Ash Characteristics

Ξ	
М	Test ID
Ξ	Baseline 1
0	Baseline 2
0	Baseline 3
Ξ	Cofire 1
	Cofire 2
	Cofire 3
п	Baseline Average
	Cofire Averages
	Limit / 40 C
A ARCH	
NS EP	

Table 3-8. Ash TCLP Metals

Test ID	Fuel	Silver, mg/L	Arsenic, mg/L	Barium, mg/L	Cadmium, mg/L	Chromium, mg/L	Mercury, mg/L	Lead, mg/L	Selenium, mg/L
Baseline 1		< 0.001	0.003	0.27	0.001	0.05	< 0.001	0.02	0.10
Baseline 2	100 % Coal	< 0.001	0.008	0.21	0.002	0.06	< 0.001	< 0.001	0.10
Baseline 3		< 0.001	0.016	0.38	0.002	0.079	0.002	< 0.001	0.14
Cofire 1	Dlandad	< 0.001	0.005	0.30	<0.001	0.069	<0.001	0.012	0.094
Cofire 2	Blended Fuel	< 0.001	0.004	0.37	<0.001	0.095	<0.001	0.011	0.091
Cofire 3	i dei	< 0.001	0.003	0.35	<0.001	0.096	<0.001	0.012	0.094
Baseline Averages		< 0.001	0.009	0.29	0.002	0.06	< 0.002	< 0.02	0.11
Cofire Averages		< 0.001	0.004	0.34	< 0.001	0.09	< 0.001	0.01	0.093
Limit / 40 CFR 26	61.24	5.0	5.0	100.0	1.0	5.0	0.2	5.0	1.0

Test ID	Fuel	Silicon Dioxide (SiO2) + Aluminum Oxide (Al2O3) + Iron Oxide (Fe2O3), (%)	Sulfur Trioxide (SO3), (%)	Loss on ignition, (%)
Baseline 1		24.63	14.21	12.13
Baseline 2	100 % Coal	23.82	18.12	11.32
Baseline 3		26.42	19.58	11.12
Cofire 1	Blended	13.02	10.15	16.24
Cofire 2	Fuel	10.74	11.35	18.25
Cofire 3	1 401	10.39	10.27	17.92
Class F Requirements		70.0 (min %)	5.0 (max %)	6.0 (max %)
Baseline Averages		24.96	17.30	11.52
Cofire Averages		11.38	10.59	17.47
Absolute Difference		-13.57	-6.71	5.95
% Difference		-74.7%	-48.1%	41.0%

 Table 3-9. Fly Ash Class F Requirements (C 618-05)

3.4 SUSTAINABILITY ISSUES

Table 3-1 summarized the composition of the site's coal supply and the blended fuel. Regarding use and or disposal of fly ash, biomass co-firing did not impact either sustainability issue since the quality of the ash with regard to fly ash TCLP metals and Class F Requirements was unchanged. The following is a brief GHG sustainability analysis for use of the woody biomass fuel at this site.

3.4.1 GHG Emission Offsets

Energy Used and Associated CO2 Emissions to Harvest, Process, and Shred Wood-Based Fuel

The woody biomass fuel used at REC has a significant level of energy use and associated CO_2 emissions to harvest, process, and shred the timber prior to transportation to the site. However, since the woody biomass used at REC comes from such a wide variety of suppliers, both geographically and organizationally, estimation of this portion of the GHG offset analysis was well beyond the scope of this project, and therefore not considered here.

Transportation Fuel Use

The REC receives woody biomass based fuel from the neighboring Blandin Mill and a wide variety of commercial suppliers throughout the northern plains region. During the first 6 months of 2007, the facility received a total of approximately 173,000 tons of woody biomass based fuel. Of that, approximately 83,000 tons came from the Blandin Mill, and the remaining 90,000 tons were purchased

from commercial providers. Appendix D summarizes the woody biomass deliveries to the REC during this period.

Fuel and emissions associated with transportation of woody biomass to the Blandin Mill are not considered in this analysis since the woody biomass is transported to the facility whether used as fuel or not. The data in Appendix D show that approximately 33,000 gallons of diesel fuel was used to transport woody biomass based fuels from commercial suppliers to the REC (equating to an estimated 0.37 gallons per ton of woody biomass delivered). The analysis assumes trucks using 350 Cummins motors or equivalent were used to transport the fuel at an estimated fuel economy of 6.5 miles per gallon.

CO2 Emissions From Transportation Fuel Use

Based on an Energy Information Administration emission factor of 19.564 lbs CO_2 /gallon, CO_2 emissions per ton of woody biomass based fuel transported to the facility are:

- 7.2 lbs CO_2 / ton woody biomass (0.37 gal fuel /ton pellets * 19.564 lbs CO_2 /gal).
- 648 tons CO₂ annually (7.2 lb/ton * 180,000 tons woody biomass delivered annually).

CO2 Emissions from Combustion of Bituminous Coal Compared to Woody biomass

Based on data generated during this testing, the CO_2 emission rates while firing straight coal and blended fuel (at a blending rate of approximately 92 percent woody biomass by mass) were 160 and 165 lb/MMBtu, respectively. However, combustion of wood-based fuel, which is composed of biogenic carbon, emits no appreciable CO_2 emissions under international greenhouse gas accounting methods developed by the IPCC and adopted by the ICFPA [6]. By analyzing the heat content of the coal and the woody biomass, the total boiler heat input for the test periods, and boiler efficiency, it was determined that approximately 90 percent of the heat generated during co-firing test periods is attributable to the wood-based fuel. It is therefore estimated that the CO_2 emissions offset during this testing is approximately 90 percent, or 148 lb/MMBtu at this co-firing blend.

REC Boiler 5 typically operates around 220 MMBtu/hr heat generating rate. Assuming an availability and utilization rate of 75 percent for Boiler 5 at this heat rate, this would equate to estimated annual CO_2 emission reductions of approximately 107,000 tons per year. CO_2 offsets from use of wood pellets could be even greater had the analysis included emissions associated with coal mining and transportation, but this type of complex analysis was not included in the scope of this study.

4.0 DATA QUALITY ASSESSMENT

4.1 DATA QUALITY OBJECTIVES

Under the ETV program, Southern specifies data quality objectives (DQOs) for each primary verification parameter before testing commences as a statement of data quality. The DQOs for this verification were developed based on input from EPA's ETV QA reviewers, and input from the BCSG. Test results which meet the DQOs provide an acceptable level of data quality for technology users and decision makers.

The DQOs for this verification are qualitative in that the verification produced emissions performance data that satisfy the QC requirements contained in the EPA Reference Methods specified for each pollutant, and the fuel and fly ash analyses meet the quality assurance / quality control (QA/QC) requirements contained in the ASTM Methods being used.

This verification did not include a stated DQO for boiler efficiency determinations because measurement accuracy validation for certain boiler parameters was not possible. Section 4.1.3 provides further discussion.

4.1.1 Emissions Testing QA/QC Checks

Each of the EPA Reference Methods used here for emissions testing contains rigorous and detailed calibrations, performance criteria, and other types of QA/QC checks. For instrumental methods using gas analyzers, these performance criteria include analyzer span, calibration error, sampling system bias, zero drift, response time, interference response, and calibration drift requirements. Methods 5, 29, CTM040, and 202 for determination of particulates and metals also include detailed performance requirements and QA/QC checks. Details regarding each of these checks can be found in the methods and are not repeated here. However, results of certain key QA/QC checks for each method are reported as documentation that the methods were properly executed. Key emissions testing QA/QC checks are summarized in Table 4-1. Where facility CEMS were used, up to date relative accuracy test audit (RATA) certifications and quarterly cylinder gas audits (CGAs) have been procured, reviewed, and filed at Southern to document system accuracy.

The emissions testing completeness goal for this verification was to obtain valid data for 90 percent of the test periods on each boiler tested. This goal was achieved as all data was validated for the test periods.

Parameter	Calibration/QC Check	When Performed/Frequency	Allowable Result	Actual Result
CO ₂ ,	Analyzer calibration	Daily before testing	± 2 % of analyzer	
	error test	D.C. Li	span	All calibrations, system
	System bias checks	Before each test run	\pm 5 % of analyzer	bias checks, and drift tests were within the
	System calibration drift test	After each test run	span ± 3 % of analyzer span	allowable criteria.
NO_X, CO, SO_2, O_2	Relative accuracy test audit	Annually (last RATA April 17, 2006)	\pm 20 percent of reference method	Relative accuracies for NO _X , CO, SO ₂ , and O ₂ CEMS were 11.7, 3.0, 1.0, and 0.2 percent, respectively
TPM, Metals	Percent isokinetic rate	After each test run	90 - 110 % for TPM and metals	
	Analytical balance calibration	Daily before analyses	± 0.0002 g]
	Filter and reagent blanks	Once during testing after first test run	< 10 % of particulate catch for first test run	All criteria were met for the TPM and metals measurement and
	Sampling system leak test	After each test	<0.02 cfm	analytical systems.
	Dry gas meter calibration	Once before and once after testing	± 5 %	
	Sampling nozzle calibration	Once for each nozzle before testing	± 0.01 in.	
Metals	ICP/CVAAS	Spike and recovery of prepared QC standards	± 25% of expected value	All matrix spike and recovery results were within 90 to 110 percent of the standards, including an independent Hg audit sample
HCl,	Sampling system leak	After each test	<0.02 cfm	
HF	test	Once before and once	± 5 %	All criteria were met for the acid gases
	Dry gas meter calibration	after testing	± 3 %	measurement and
	Ion chromatograph	Analysis of prepared QC standards	± 10% of expected value	analytical systems.

4.1.2 Fly ash and Fuel Analyses QA/QC Checks

The laboratory selected for analysis of collected fuel and fly ash samples (Wyoming Analytical Laboratory Services, Inc.) operates under an internal quality assurance protocol, a copy of which is maintained at Southern. Each of the analytical procedures used here include detailed procedures for instrument calibration and sample handling. They also include QA/QC checks in the form of analytical repeatability requirements or matrix spike analyses. All of the QA/QC checks specified in the methods were met during these analyses.

4.1.3 Boiler Efficiency QA/QC Checks

Table 4-2 summarizes the contributing measurements for boiler efficiency determination, measurement quality objectives (MQOs) for each, and the primary method of evaluating the MQOs. Factory calibrations, sensor function checks, and reasonableness checks in the field were used to assess achievement of the MQOs where possible. Some of the MQOs were either not met or impossible to verify, so the overall uncertainty of the boiler efficiency determinations is unclear. In anticipation of this, the test plan did not specify a DQO for boiler efficiency.

InstrumentInstrumentFuel temperature, $^{\circ}F$ NIST-traceable calibrationUpon purchase and every 2 years $\pm 6 \ ^{\circ}F$ Fuel temp $\pm 1 \ ^{\circ}F$ Air temperature, $^{\circ}F$ NIST-traceable calibration $\pm 1 \ ^{\circ}F$ $\pm 1 \ ^{\circ}F$ $\pm 1 \ ^{\circ}F$ Air temperature, $^{\circ}F$ NIST-traceable calibration $\pm 3.5 \ ^{\circ}\%$ $\pm 3.0 \ ^{\circ}\%$ Moisture in air, lb/lbNIST-traceable calibration $\pm 3.5 \ ^{\circ}\%$ $\pm 3.0 \ ^{\circ}\%$ Combustion air temperature, $^{\circ}F$ Cross check with NIST- traceable standardAnnually $\pm 6 \ ^{\circ}F$ Within $5 \ ^{\circ}F$ Steam flow, MMBtu/h or lb/hOrifice calibrationUpon installation $\pm 5 \ ^{\circ}F$ readingCalibration not availableSteam pressure, psig Supply water temperature, $^{\circ}F$ Cross check with NIST- traceable standardAnnually $\pm 5 \ ^{\circ}F$ $\pm 10 \ ^{\circ}F$ Supply water temperature, $^{\circ}F$ Eras pressure, psigCalibration not available $available$ Supply water temperature, $^{\circ}F$ Cross check with boiler efficiency calculationsAnnually $\pm 5 \ ^{\circ}F$ readingInvalidated for coal scales, but not used for determining efficiencyFuel lead rate, lb/hCross check with boiler epeatabilityAnnually $\pm 5 \ ^{\circ}F$ readingInvalidated for coal scales, but not used for determining efficiencyFuel lead rate, lb/hASTM D1945 duplicate sample analysis and repeatability2 samplesWithin D1945Method repeatability limits for each fluel componentFuel heating va	Measurement /	QA/QC Check	When Performed	MQO	Results achieved
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air heater inlet, °FNIST-traceable calibrationAir temperature, °FNIST-traceable calibration± 1 °F± 1 °FMoisture in air, lb/lbNIST-traceable calibration± 3.5 %± 3.0 %Combustion air temperature, °FCross check with NIST- traceable standardAnnually± 6 °FWithin 5°FSteam flow, MMBtu/h or lb/hOrifice calibrationUpon installation± 5 % reading ± 5 % readingCalibration not availableSteam pressure, psigCross check with NIST- traceable standardAnnually± 5 psig± 6 psigSteam temperature, °FCross check with NIST- traceable standardAnnually± 5 psig± 6 psigSteam temperature, °FCross check with NIST- traceable standardAnnually± 5 psig± 10 °FSupply water pressure, psigSupply water traceable standardAnnually± 5 % reading ± 2 % of reference standardCalibrations not availableFuel feed rate, lb/hCross check with boiler efficiency calculationsAnnually± 5 % reading to freference standardInvalidated for coal scales, but not used for determining efficiencyFuel ultimate analyses, both wood and coalASTM D1945 duplicate sample analysis and repeatability2 samplesWithin D1945 repeatability limits for each fuel componentMethod repeatability criteria were met	I	NIST-traceable		±6 °F	
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component	both wood and coal	sample analysis and	-	repeatability limits	repeatability criteria
component		repeatability		for each fuel	were met
		1 2		component	
	Fuel heating value,	ASTM D1945 duplicate	1		1
Btu/lb sample analysis and repeatability limits	6			repeatability limits	
repeatability for each fuel				1 0	
component					

Table 4-2.	Boiler	Efficiency	QA/QC	Checks
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4.1.4 Technical Systems Audit

A technical systems audit was conducted during the week of March 26-30, 2007 at the REC facility in support of this verification. The audit was conducted in accordance with SRI's recently drafted

ETV/ESTE project QA guideline. The audit was conducted remotely by the quality assurance manager, Eric Ringler, with the assistance of project staff member, Sarah Fisher, in the field.

Prior to the audit, the QAM developed an audit check-matrix listing each measurement to be conducted and the audit criteria to be examined. Before leaving for the field, the QAM and field technician went through the check-matrix and audit procedures to ensure good coordination of the audit. The field technician examined the check matrix to verify it was consistent with the TQAP and with expected field conditions. She also determined key test parameters for the audit. According to the project QA guideline, an audit is considered complete if all key measurements are audited and spot checks conducted for the remaining measurements.

During field measurements, the QAM and field technician discussed audit progress and findings on a daily basis by telephone. One deviation from the test plan was noted. Ash samples were collected from the ESP hopper instead of directly from the stack. The impact of this on data quality is unknown, but considered to be minor, since ash composition is an ancillary measurement and not one of the verification parameters. There is some concern about the representativeness of the samples. A corrective action report was completed.

Apart from this, all audit criteria were satisfied for all key and other audited parameters. The audit was very thorough and went well beyond the minimum required for a successful audit. The completed check-matrix and corrective action report is documented at Southern.

5.0 REFERENCES

- [1] Southern Research Institute, *Test and Quality Assurance Plan Environmental and Sustainable Technology Evaluation Biomass Co-firing in Industrial Boilers*, <u>www.sri-rtp.com</u>, Southern Research Institute, Research Triangle Park, NC. October 2006.
- [2] Babcock & Wilcox, *Steam –Its Generation and Use 40th Edition*, The Babcock & Wilcox Company, Barberton, Ohio, 1992.
- [3] Code of Federal Regulations (Title 40 Part 60, Appendix A) *Test Methods (Various)*, <u>http://www.gpoaccess.gov/cfr/index.html</u>, U.S. Environmental Protection Agency, Washington, DC, 2005.
- U.S. EPA, AP-42, Compilation of Air Pollutant Emission Factors, <u>http://www.epa.gov/oms/ap42.htm</u>, U.S. Environmental Protection Agency Office of Transportation and Air Quality, Washington D.C., 2005.
- [5] Code of Federal Regulations (Title 40 Part 261.24) *Identification and Listing of Hazardous Waste – Toxicity Characteristic*, <u>http://www.access.gpo.gov/nara/cfr/waisidx 05/40cfr261 05.html</u>, U.S. Environmental Protection Agency, Washington, DC, 2005.
- [6] The Climate Change Working Group of The International Council of Forest and Paper Associations (ICFPA) *Calculation Tools for Estimating Greenhouse Gas Emissions from Pulp and Paper Mills, Version 1.1,* National Council for Air and Stream Improvement, Inc. (NCASI), Research Triangle Park, NC, July, 2005.

Southern Research Institute/USEPA April 2008

Appendix A Unit 5 Emissions Data

PARTICULATE TEST RESULTS SUMMARY

Company:	Minnesota Power
Plant:	Grand Rapid, MN
Unit:	Boiler 5 Outlet Duct

Test Run Number	1	2	3	Average
Source Condition	Coal	Coal	Coal	
Date	03/28/2007	03/28/2007	03/28/2007	
Start Time	9:44	12:47	15:54	
End Time	12:12	15:14	18:22	
Total Particulate:				
grains/dscf	0.0165	0.0159	0.0225	0.0183
lb/hr	8.741	8.432	11.214	9.462
Filterable PM:				
grains/dscf	0.0025	0.0024	0.0029	0.0026
lb/hr	1.310	1.266	1.461	1.346
Condensible PM (Method 202):				
grains/dscf	0.0141	0.0135	0.0195	0.0157
lb/hr	7.432	7.166	9.753	8.117
Stack Parameters:				
Gas Volumetric Flow Rate, acfm	109,086	109,584	103,502	107,391
Gas Volumetric Flow Rate, dscfm	61,639	61,872	58,209	60,573
Average Gas Temperature, °F	396.1	402.3	399.4	399.3
Average Gas Velocity, ft/sec	41.339	41.528	39.223	40.697
Flue Gas Moisture, percent by volume	7.9	7.3	8.0	7.8
Average Flue Pressure, in. Hg	29.77	29.77	29.77	
Barometric Pressure, in. Hg	29.79	29.79	29.79	
Average %CO2 by volume, dry basis	12.7	12.4	12.3	12.5
Average %O2 by volume, dry basis	7.5	7.3	7.7	7.5
Dry Molecular Wt. of Gas, lb/lb-mole	30.332	30.276	30.276	
Gas Sample Volume, dscf	99.601	96.953	89.041	
Isokinetic Variance	101.9	98.8	96.4	

Rapids Energy Center, Grand Rapids, MN Boiler No. 5 Outlet Duact Average Results Tests 1 through 3 3/28/07

Parameter		centration bs/dscf)	Emi	issions Rate (Ibs/hr)		gr/dscf		gr/acf	ľ	ug/Nm³
Arsenic		1.10E-10		3.89E-04		7.72E-07		4.31E-07		1.766
Barium	<	9.58E-10	<	3.39E-03	<	6.70E-06	<	3.75E-06	<	15.342
Beryllium	<	7.11E-12	<	2.50E-05	<	4.98E-08	<	2.78E-08	V	0.114
Cadmium		1.66E-11		5.83E-05		1.16E-07		6.48E-08		0.266
Chromium	<	1.60E-10	<	5.62E-04	<	1.12E-06	<	6.25E-07	V	2.557
Zinc		1.55E-09		5.51E-03		1.09E-05		6.08E-06		24.908
Copper		3.78E-10		1.35E-03		2.65E-06		1.48E-06		6.061
Lead	<	3.78E-11	<	1.33E-04	<	2.64E-07	<	1.48E-07	V	0.605
Manganese		1.57E-09		5.56E-03		1.10E-05		6.16E-06		25.200
Mercury		1.95E-10		6.89E-04		1.37E-06		7.65E-07		3.131
Nickel	<	3.79E-10	<	1.33E-03	<	2.65E-06	<	1.48E-06	<	6.064
Selenium		1.85E-10		6.50E-04		1.30E-06		7.24E-07		2.966
Silver	<	2.04E-10	<	7.17E-04	<	1.43E-06	<	7.97E-07	<	3.263

METHOD 26 TEST RESUL	TS

Date:	03/28/2007		Condition: Coal	
Project:	Minnisota Power		Data Taken By: MH	
Location:	Outlet Duct		Fuel Factor:	
Source:	Boiler 5			
Test Numbe	r	1	Time: 10:15-11	-15
	arometric(Hg"):	29.790	Carbon Dioxide Content(%):	12.70
	tatic(H ₂ O"):	-0.25	Oxygen Content(%):	7.50
	tack(Hg"):	29.772	Nitrogen Content(%):	79.80
	ne (liters)	6861.22	HF (mg)	0.073
	e (liters)	6981.31	HCI (mg)	0.330
Meter Temp	erature (°F)	79.50		
Meter Volum	ne (dscf)	4.153	HF (ppm):	0.746
Meter Calibr	ation (Y)	1.005	HCI (ppm):	1.850
			HF (lbs/hr):	0.1433
			HCI (lbs/hr):	0.648
	ta Η (ΔΗ)	0.010	HF (lbs/MMBtu):	0.00E+0
Dry Standar	d Flow Rate (dscfm):	61,639	HCI (Ibs/MMBtu):	0.0000
Test Numbe	r:	2	Time: 12:47-13	:47
	arometric(Hg"):	29.790	Carbon Dioxide Content(%):	12.40
	tatic(H ₂ O"):	-0.25	Oxygen Content(%):	7.30
	tack(Hg"):	29.772	Nitrogen Content(%):	80.30
Initial Volum	ne (liters)	6999.74	HF (mg)	0.041
	e (liters)	7119.82	HCI (mg)	0.077
	erature (°F)	73.60		
Meter Volum	ne (dscf)	4.199	HF (ppm):	0.414
Meter Calibr	ation (Y)	1.005	HCI (ppm):	0.427
			HF (lbs/hr):	0.0799
			HCI (lbs/hr):	0.150
Average Del	ta Η (ΔΗ)	0.010	HF (lbs/MMBtu):	0.00E+0
Dry Standar	d Flow Rate (dscfm): *	61,872	HCI (Ibs/MMBtu):	0.0000
Test Numbe	r;	3	Time: 15:54-16	:54
Pressure, Ba	arometric(Hg"):	29.790	Carbon Dioxide Content(%):	12.30
	arometric(Hg"): atic(H ₂ O"):	29.790 -0.25	Carbon Dioxide Content(%): Oxygen Content(%):	12.30 7.70
Pressure, St				
Pressure, St Pressure, St	tatic(H ₂ O"):	-0.25	Oxygen Content(%):	7.70
Pressure, St Pressure, St Initial Volum	tatic(H ₂ O"): tack(Hg"):	-0.25 29.772	Oxygen Content(%): Nitrogen Content(%):	7.70 80.00
Pressure, St Pressure, St Initial Volum Final Volum	tatic(H ₂ O"): tack(Hg"): ne (liters)	-0.25 29.772 7121.170	Oxygen Content(%): Nitrogen Content(%): HF (mg)	7.70 80.00 0.100
Pressure, St Pressure, St Initial Volum Final Volum Meter Tempo	tatic(H ₂ O"): tack(Hg"): ne (liters) e (liters)	-0.25 29.772 7121.170 7241.190	Oxygen Content(%): Nitrogen Content(%): HF (mg)	7.70 80.00 0.100
Pressure, St Pressure, St Initial Volum Final Volum Meter Tempe Meter Volum	tatic(H ₂ O"): tack(Hg"): ne (liters) e (liters) erature (⁰ F)	-0.25 29.772 7121.170 7241.190 77.20	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg)	7.70 80.00 0.100 0.370 1.018
Pressure, St Pressure, St Initial Volum Final Volum Meter Tempe Meter Volum	tatic(H ₂ O"): tack(Hg"): e (liters) e (liters) re tature (°F) ne (dscf)	-0.25 29.772 7121.170 7241.190 77.20 4.169	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HF (ppm):	7.70 80.00 0.100 0.370 1.018
Pressure, St Pressure, St Initial Volum Final Volum Meter Tempe Meter Volum	tatic(H ₂ O"): tack(Hg"): e (liters) e (liters) re tature (°F) ne (dscf)	-0.25 29.772 7121.170 7241.190 77.20 4.169	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCl (mg) HC (ppm): HC (ppm): HF (lbs/hr): HCl (lbs/hr):	7.70 80.00 0.100 0.370 1.018 2.066
Pressure, St Pressure, St Initial Volum Final Volum Meter Tempo Meter Volum Meter Calibr Average Del	tatic(H ₂ O"): tack(Hg"): e (liters) e (liters) e rature (°F) tation (Y) ta H (ΔH)	-0.25 29.772 7121.170 7241.190 77.20 4.169	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HF (ppm): HCI (ppm): HF (lbs/hr): HCI (bs/hr):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683
Pressure, St Pressure, St Initial Volum Final Volum Meter Tempo Meter Volum Meter Calibr Average Del	tatic(H ₂ O"): tack(Hg"): te (liters) e (liters) e (liters) e (liters) erature (°F) tation (Y)	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCl (mg) HC (ppm): HC (ppm): HF (lbs/hr): HCl (lbs/hr):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847
Pressure, St Pressure, St Initial Volum Final Volum Meter Tempo Meter Volum Meter Calibr Average Del	tatic(H ₂ O"): tack(Hg"): e (liters) erature (⁰ F) e (dscf) tation (Y) ta H (ΔH) d Flow Rate (dscfm):	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HF (ppm): HCI (ppm): HF (lbs/hr): HCI (bs/hr):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000
Pressure, St Pressure, St Initial Volume Meter Tempe Meter Volume Meter Calibr Average Del Dry Standare Test Numbe	tatic(H ₂ O"): tack(Hg"): e (liters) erature (⁰ F) e (dscf) tation (Y) ta H (ΔH) d Flow Rate (dscfm):	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HCI (ppm): HCI (ppm): HF (lbs/hr): HCI (lbs/hr): HCI (lbs/MMBtu): HCI (lbs/MMBtu):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000
Pressure, St Pressure, St Pressure, St Initial Volum Final Volum Meter Tempo Meter Volum Meter Calibr Meter C	tatic(H ₂ O"): tack(Hg"): e (liters) erature (°F) e (dscf) ation (Y) tat H (ΔH) d Flow Rate (dscfm): r: arometric(Hg"): tatic(H ₂ O"):	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HCI (ppm): HCI (ppm): HF (lbs/hr): HF (lbs/hr): HCI (lbs/hr): HCI (lbs/hr): HCI (lbs/hMBtu): HCI (lbs/MMBtu):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000 12.30 7.70
Pressure, St Pressure, St Initial Volume Meter Volume Meter Volume Meter Calibr Average Del Dry Standare Pressure, St Pressure, St Pressure, St	tatic(H ₂ O"): tack(Hg"): te (liters) e (liters) re (dscf) ta H (ΔH) d Flow Rate (dscfm): r: arometric(Hg"): tatic(H ₂ O"): tack(Hg"):	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HCI (ppm): HF (lbs/hr): HF (lbs/hr):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000
Pressure, St Pressure, St Initial Volume Keter Tempy Meter Volume Meter Calibr Average Del Dry Standard Test Numbe Pressure, St Pressure, St Pressure, St Pressure, St	tatic(H ₂ O"): tack(Hg"): e (liters) e (liters) retature (°F) ation (Y) tat H (ΔH) d Flow Rate (dscfm): f: arometric(Hg"): tatic(H ₂ O"): tack(Hg"):	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HF (ppm): HCI (ppm): HCI (lbs/hr): HCI (lbs/hr):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000 :02 12.30 7.70 80.00 0.087
Pressure, St Pressure, St Pressure, St Pressure, St Pressure, St Pressure, St Pressure, St Prital Volume	tatic(H ₂ O"): tack(Hg"): e (liters) e (liters) retature (°F) ation (Y) tation (Y) d Flow Rate (dscfm): f r: arometric(Hg"): tatic(H ₂ O"): tack(Hg"): e (liters) e (liters)	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HCI (ppm): HF (lbs/hr): HF (lbs/hr):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000
Pressure, St Pressure, St nitial Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standar Pressure, St Pressure, St nitial Volum Weter Temp	tatic(H ₂ O"): tack(Hg"): te (liters) erature (°F) te (dscf) tat H (ΔH) d Flow Rate (dscfm): d Flow Rate (dscfm): tatic(H ₂ O"): tatic(H ₂ O"): tatic(H ₂ O"): tatic(H ₂ O"): te (liters) e (liters) e (liters)	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700 78.40	Oxygen Content(%): Nitrogen Content(%): HF (mg)	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000 12.30 7.70 80.00 0.087 0.330
Pressure, St Pressure, St Initial Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standard Test Numbe Pressure, St Pressure, St Pressure, St Pressure, St Pressure, St Nitial Volum Meter Temp Meter Volum	tatic(H ₂ O"): tack(Hg"): te (liters) e (liters) e (liters) te (dscf) tation (Y) d Flow Rate (dscfm): r: arometric(Hg"): tatic(H ₂ O"): tack(Hg"): te (liters) e (liters) e (liters) e (dscf) te (dscf)	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700 78.40 4.161	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HF (ppm): HCI (ppm): HCI (bp/hr): HCI (bs/hr): HCI (bs/hr):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000 7.70 80.00 0.087 0.330 0.887
Pressure, St Pressure, St Initial Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standard Test Numbe Pressure, St Pressure, St Pressure, St Pressure, St Pressure, St Nitial Volum Meter Temp Meter Volum	tatic(H ₂ O"): tack(Hg"): te (liters) erature (°F) te (dscf) tat H (ΔH) d Flow Rate (dscfm): d Flow Rate (dscfm): tatic(H ₂ O"): tatic(H ₂ O"): tatic(H ₂ O"): tatic(H ₂ O"): te (liters) e (liters) e (liters)	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700 78.40	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HF (ppm): HCI (ppm): HCI (bp/hr): HCI (lbs/hr): HCI (lbs/hr): HCI (lbs/hr): HCI (lbs/hr) HCI (lbs/hr) HCI (lbs/hmBtu): HCI (lbs/MMBtu): HCI (lbs/MMBtu):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000
Pressure, St Pressure, St Initial Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standard Test Numbe Pressure, St Pressure, St Pressure, St Pressure, St Pressure, St Nitial Volum Meter Temp Meter Volum	tatic(H ₂ O"): tack(Hg"): te (liters) e (liters) e (liters) te (dscf) tation (Y) d Flow Rate (dscfm): r: arometric(Hg"): tatic(H ₂ O"): tack(Hg"): te (liters) e (liters) e (liters) e (dscf) te (dscf)	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700 78.40 4.161	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HF (ppm): HCI (ppm): HCI (bp/hr): HCI (bs/hr): HCI (bs/hr):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000 7.70 80.00 0.087 0.330 0.887
Pressure, St Pressure, St Initial Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standard Test Numbe Pressure, St Initial Volum Final Volum Meter Temp Meter Calibr Meter Calibr	tatic(H ₂ O"):	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700 78.40 4.161	Oxygen Content(%):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000 7.70 80.00 0.087 0.330 0.887 1.846 0.1610 0.611
Pressure, St Pressure, St Initial Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standard Test Numbe Pressure, St Initial Volum Final Volum Meter Temp Meter Calibr Meter Calibr	tatic(H ₂ O"):	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700 78.40 4.161 1.005	Oxygen Content(%): Nitrogen Content(%): HF (mg)	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.082 0.00E+0 0.0000 0.000E+0 0.0000 0.0087 0.330 0.887 1.846 0.1610
Pressure, St Initial Volum Final Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standard Fressure, St Pressure, St Pressure, St Pressure, St Nitial Volum Meter Temp Meter Calibr Meter Calibr Average Del Dry Standard	tatic(H ₂ O"):	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700 78.40 4.161 1.005 0.010 58,209	Oxygen Content(%): Nitrogen Content(%): HF (mg) HCI (mg) HCI (ppm): HCI (ppm): HCI (bs/hr): HCI (bs/hr):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000 7.70 80.00 0.887 1.846 0.687 1.846 0.687 1.846 0.687 0.300 0.887 1.846 0.611 0.00E+0 0.611 0.00E+0 0.611 0.00E+0 0.611 0.00E+0 0.611 0.611 0.00E+0 0.611 0.00E+0 0.611 0.00E+0 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.000000 0.000000 0.00000000
Pressure, St Pressure, St Initial Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standard Test Numbe Pressure, St Initial Volum Final Volum Meter Temp Meter Calibr Meter Calibr	tatic(H ₂ O"): tack(Hg"): tack(Hg"): tack(Hg"): tatic(H ₂ O") tatic (dscf) tatic (dscf) d Flow Rate (dscfm): r: arometric(Hg"): tatic(H ₂ O") tatic(H ₂ O") tatic	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700 78.40 4.161 1.005	Oxygen Content(%):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000 7.70 80.00 0.087 0.330 0.887 1.846 0.1610 0.611 0.0614
Pressure, St Initial Volum Final Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standar Pressure, St Pressure, St Pressure, St Initial Volum Meter Temp Meter Volum Meter Calibr Average Del Dry Standard Average HCI Average HCI	tatic(H ₂ O"): tack(Hg"): tack(Hg"): tack(Hg"): tatic(H ₂ O") tatic (dscf) tatic (dscf) d Flow Rate (dscfm): r: arometric(Hg"): tatic(H ₂ O") tatic(H ₂ O") tatic	-0.25 29.772 7121.170 7241.190 77.20 4.169 1.005 0.010 58,209 4 29.790 -0.25 29.772 7241.640 7361.700 78.40 4.161 1.005 0.010 58,209 0.523	Oxygen Content(%):	7.70 80.00 0.100 0.370 1.018 2.066 0.1847 0.683 0.00E+0 0.0000 .02 12.30 7.70 80.00 0.087 0.330 0.887 1.846 0.1610 0.687 1.846 0.1610 0.00E+0 0.0000 0.320 0.087 0.000 0.087 0.000 0.087 0.000 0.087 0.000 0.000 0.087 0.000 0.087 0.000 0.087 0.000 0.087 0.000 0.000 0.087 0.000 0.087 0.000 0.087 0.000 0.087 0.000 0.087 0.000 0.087 0.000 0.000 0.087 0.000 0.087 0.000 0.000 0.087 0.000 0.000 0.000 0.000 0.087 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.000000 0.000000 0.00000000

PARTICULATE TEST RESULTS SUMMARY

Company:	Minnesota Power
Plant:	Grand Rapid, MN
Unit:	Boiler 5 Outlet Duct

Test Run Number	1	2	3	Average
Source Condition	15% Coal & 85% Bark	15% Coal & 85% Bark	15% Coal & 85% Bark	
Date	03/29/2007	03/29/2007	03/29/2007	
Start Time	8:17	12:28	15:21	
End Time	10:49	14:56	17:48	
Total Particulate:				
grains/dscf	0.0055	0.0037	0.0032	0.0041
lb/hr	3.260	2.043	1.842	2.381
Filterable PM:				
grains/dscf	0.0017	0.0021	0.0019	0.0019
lb/hr	1.039	1.125	1.081	1.082
Condensible PM (Method 202):				
grains/dscf	0.0037	0.0017	0.0013	0.0022
lb/hr	2.221	0.918	0.761	1.300
Stack Parameters:				
Gas Volumetric Flow Rate, acfm	147,952	131,836	137,161	138,983
Gas Volumetric Flow Rate, dscfm	69,769	64,032	66,791	66,864
Average Gas Temperature, °F	457.8	444.7	446.4	449.6
Average Gas Velocity, ft/sec	56.068	49.961	51.978	52.669
Flue Gas Moisture, percent by volume	17.9	16.6	16.3	16.9
Average Flue Pressure, in. Hg	29.87	29.87	29.87	
Barometric Pressure, in. Hg	29.80	29.80	29.80	
Average %CO2 by volume, dry basis	12.3	12.6	12.5	12.5
Average %O2 by volume, dry basis	7.5	7.2	7.5	7.4
Dry Molecular Wt. of Gas, lb/lb-mole	30.268	30.304	30.300	
Gas Sample Volume, dscf	121.722	77.515	80.099	
Isokinetic Variance	110.0	99.0	98.0	

Rapids Energy Center, Grand Rapids, MN Boiler No. 5 Outlet Duact Average Results Tests 1 through 3 3/29/07

Parameter	Concentration (lbs/dscf)	Emissions Rate (Ibs/hr)	gr/dscf	gr/acf	ug/Nm ³
Arsenic	< 4.46E-11	< 1.74E-04	< 3.13E-07	< 1.49E-07	< 0.715
Barium	3.40E-10	1.33E-03	2.38E-06	1.13E-06	5.448
Beryllium	< 7.44E-12	< 2.90E-05	< 5.21E-08	< 2.48E-08	< 0.119
Cadmium	1.48E-11	5.81E-05	1.04E-07	4.95E-08	0.238
Chromium	1.04E-10	4.06E-04	7.31E-07	3.48E-07	1.673
Zinc	2.06E-09	8.02E-03	1.44E-05	6.86E-06	32.945
Copper	1.84E-10	7.16E-04	1.29E-06	6.15E-07	2.947
Lead	< 3.00E-11	< 1.17E-04	< 2.10E-07	< 1.00E-07	< 0.481
Manganese	3.49E-10	1.37E-03	2.44E-06	1.16E-06	5.591
Mercury	< 7.92E-11	< 3.10E-04	< 5.54E-07	< 2.64E-07	< 1.268
Nickel	< 1.63E-10	< 6.34E-04	< 1.14E-06	< 5.40E-07	< 2.604
Selenium	< 7.44E-11	< 2.90E-04	< 5.21E-07	< 2.48E-07	< 1.192
Silver	< 8.41E-11	< 3.27E-04	< 5.89E-07	< 2.81E-07	< 1.347

Date:	03/29/2007		Condition: Boimass	
Project:	Minnisota Power		Data Taken By: MH	
Location:	Outlet Duct		Fuel Factor:	
Source:	Boiler 5			
Test Numbe	er:	1	Time: 8:17-9:17	,
Pressure, B	arometric(Hg"):	29.800	Carbon Dioxide Content(%):	12.30
Pressure, S	tatic(H ₂ O"):	1.00	Oxygen Content(%):	7.50
Pressure, S	tack(Hg"):	29.874	Nitrogen Content(%):	80.20
Initial Volun	ne (liters)	7363.16	HF (mg)	0.055
Final Volum	e (liters)	7483.34	HCI (mg)	0.100
Meter Temp	erature (°F)	85.50		
Meter Volun	ne (dscf)	4.112	HF (ppm):	0.567
Meter Calib	ration (Y)	1.005	HCI (ppm):	0.566
			HF (lbs/hr):	
			HCI (lbs/hr):	0.224
Average De	lta H (∆H)	0.010	HF (lbs/MMBtu):	0.00E+0
Dry Standar	d Flow Rate (dscfm):	69,769	HCI (Ibs/MMBtu):	0.0000
Test Numbe	er:	2	Time: 12:28-13	28
	arometric(Hg"):	29.800	Carbon Dioxide Content(%):	
	tatic(H ₂ O"):	1.00	Oxygen Content(%):	
	tack(Hg"):	29.874	Nitrogen Content(%):	80.20
,	ne (liters)	7484.5	HF (mg)	0.026
	e (liters)	7604.57	HCI (mg)	
	erature (°F)	78.50		
	ne (dscf)	4.162	HF (ppm):	0.265
	ration (Y)	1.005	HCI (ppm):	
			HF (lbs/hr):	
			HCI (lbs/hr):	
Average De	lta Η (ΔΗ)	0.010	HF (lbs/MMBtu):	
	d Flow Rate (dscfm): *	64,032	HCI (lbs/MMBtu):	
Test Numbe	۶r:	3	Time: 15:21-16	-21
	arometric(Hg"):	29.800	Carbon Dioxide Content(%):	
	tatic(H ₂ O"):	1.00	Oxygen Content(%):	
	tack(Hg"):	29.874	Nitrogen Content(%):	80.00
	ne (liters)	7606.800	HF (mg)	0.023
	e (liters)	7726.800	HCI (mg)	0.085
	erature (°F)	79.20		
	ne (dscf)	4.154	HF (ppm):	0.235
Meter Calibi	ration (Y)	1.005	HCI (ppm):	0.476
			HF (lbs/hr):	
			HCI (lbs/hr):	0.181
Average De	lta H (∆H)	0.010	HF (lbs/MMBtu):	0.00E+(
	d Flow Rate (dscfm):	66,791	HCI (lbs/MMBtu):	
Average HC		0.181	Average HF lbs/hr:	0.0751
Average HC		0.472	Average HF ppm:	0.356
	I lbs/MMBtu:	0.0000	Average HF lbs/MMBtu:	0.00E+
	/ Rate (dscfm)	66864	-	

Appendix B

Fuel and Ash Analyses

Kelley to insert pdf files in final report

Appendix C

Boiler Efficiency Determinations

1	INPUT CONDITIONS - BY TEST OR SPECIFICATION			FUEL - Subbituminou	s Coal, Minnesota				
1	Excess air: at burner/leaving boiler/econ, % by weight	25.0		15 Ultimate Analy		16 Theo Air, I	b/100 lb fuel	17 H ₂ O, lb/1	00 lb fuel
2	Entering air temperature, F	41.67		Constituent	% by weight	K1	[15] x K1	K2	[15] x K2
3	Reference temperature, F	80	Α	C	54.17	11.51	623.5		[:•]:::=
4	Fuel temperature, F	66	В	S	0.33	4.32	1.4		
5	Air temperature leaving air heater, F	352.11	С	H ₂	2.85	34.29	97.7	8.94	25.4
ô	Flue gas temperature leaving (excluding leakage), F	844.47	D	H₂O	23.54			1.00	23.
7	Moisture in air, lb/lb dry air	0.0035	Е	N ₂	0.93				
B	Additional moisture, lb/100 lb fuel	0	F	0 ₂	14.23	-4.32	-61.5		
9	Residue leaving boiler/economizer, % Total	85	G	Ash	3.95		0110		
0	Output, 1,000,000 Btu/h (MMBtu/h)	220.45	H	Total	100.00	Air	661.2	H₂O	49.
1	Additional theoretical air, lb/10,000 Btu Table 14, Item [2]	0	18	Higher heating valu	e (HHV) Btu/lb fu	al			9.4
2	CO_2 from sorbent, lb/10,000 Btu Table 14, Item [19]	0	19	Unburned carbon le					0.1
3	H_2O from sorbent, lb/10,000 Btu Table 14, Item [20]	0	20	Theoretical air, lb/1			[16H] x 100 /	[18]	7.0
4	Spent sorbent, lb/10,000 Btu Table 14, Item [24]	0	21	Unburned carbon,			[19] x [18] / 14		0.0
	COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu		1 2 1	Chibanica carbon,				1,000	0.
2	Theoretical air (corrected), lb/10,000 Btu	[20] - [21] x 1151 /	[18] -	+ [11]					6.990
3	Residue from fuel, lb/10,000 Btu	([15G] + [21]) x 100							0.043
4	Total residue, lb/10,000 Btu	[23] + [14]		-					0.043
	5		Α	At Burners		C Leaving Fu		D Leaving E	
5	Excess air, % by weight	(1 . [05] (100) _ [0	01	25.0	0.0		25.0		25.0
6	Dry air, lb/10,000 Btu	(1 + [25] / 100) x [2	2			0.004	8.734	0.004	8.7
7 8	H ₂ O from air, Ib/10,000 Btu	[26] x [7]				0.031 0.000	0.031	0.031	0.0
o 9	Additional moisture, lb/10,000 Btu H ₂ O from fuel, lb/10,000 Btu	[8] x 100 / [18]				0.519	0.000	0.000	0.0
9	Wet gas from fuel, Ib/10,000 Btu	[17H] x 100 / [18] (100 - [15G] - [21])	v 10	0 / [10]		0.519	1.016	0.519	1.0
1	CO ₂ from sorbent, lb/10,000 Btu		X 10	0/[10]			0.000		0.0
		[12]				0.000			
2	H ₂ O from sorbent, Ib/10,000 Btu	[13]		70.01		0.000	0.000	0.000	0.0
33 34	Total wet gas, lb/10,000 Btu Water in wet gas, lb/10,000 Btu	Summation [26] the Summation [27] + [0.550	9.781 0.550	0.550	9.7 0.5
35	Dry gas, lb/10,000 Btu	[33] - [34]	20] +	- [29] + [32]		0.550	9.231	0.550	9.2
36	H ₂ O in gas, % in weight	100 x [34] / [33]					5.62		5.0
37	Residue, % by weight (zero if < 0.15 lbm/10KB)	[9] x [24] / [33]					0.37		0.3
	EFFICIENCY CALCULATIONS, % Input from Fuel								
T	Losses								
	Dry Gas, %	0.0024 [35D] x ([6]							16.9
39	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6]	H1 = (3.958E-5 x T					1456.0		16.
89 10	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3]	H1 = (3.958E-5 x T H2 = [3] -32	+ 0.				1456.0 48.0		
39 40 41	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] %	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) /	+ 0. 100	4329) x T + 1062.2					7.:
39 40 41 42	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Moisture in air, %	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([6	' + 0. 100 6] - [3	4329) x T + 1062.2 8])					7.:
39 40 41 42 43	Dry Gas, % Water from fuel, as fired 6 Moisture in air, % Unburned carbon, %	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([6 [19] or [21] x 14,50	+ 0. 100 6] - [3 0 / [1	4329) x T + 1062.2 8]) 8]		based	48.0	t Btu/h	7.: 0. 0.
39 40 41 42 43 44	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Moisture in air, %	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([4 [19] or [21] x 14,50 ABMA curve, Chap	100 100 6] - [3 0 / [1 oter 2	4329) x T + 1062.2 8]) 8] 3		based		t Btu/h	7.:
39 40 41 42 43 44 45 46	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([t [19] or [21] x 14,50 ABMA curve, Chap From Chapter 10,	100 100 3] - [3 0 / [1 ter 2 Table	4329) x T + 1062.2 8]) 8] 3 14, Item [41]		based of	48.0	t Btu/h	7. 0. 0. 1. 1. 0.
39 40 41 42 43 44 45 46	Dry Gas, % Water from fuel, as fired Enthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, %	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([4 [19] or [21] x 14,50 ABMA curve, Chap	100 100 3] - [3 0 / [1 ter 2 Table	4329) x T + 1062.2 8]) 8] 3 14, Item [41]		based (48.0	t Btu/h	7. 0. 0. 1. 1. 0.
39 40 41 42 43 44 45 46 47	Dry Gas, % Water from fuel, as fired % Enthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits	H1 = (3.958É-5 × T H2 = [3] -32 [29] × ([39] - [40]) / 0.0045 × [27D] × ([4 [19] or [21] × 14.50 ABMA curve, Chap From Chapter 10, Summation [38] thr	100 6] - [3 0 / [1 oter 2 Fable	4329) x T + 1062.2 8]) 8] 3 14, Item [41] 146]		based (48.0	t Btu/h	7.: 0. 1. 1. 0. 26.
 39 40 41 42 43 44 45 46 47 48 	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, %	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([t [19] or [21] x 14.50 ABMA curve, Chap From Chapter 10, Summation [38] thr 0.0024 x [26D] x ([t	100 5] - [3 0 / [1 ter 2 Table rough 2] - [3	4329) x T + 1062.2 3] 8] 14, Item [41] [46] 3]		based	48.0	t Btu/h	7. 0. 0. 1. 1. 0. 26. -0.
89 40 41 42 43 44 45 46 45 46 48 48 49	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, %	H1 = (3.958E-5 x T H2 = (332 [29] x ([39] - [40]) / 0.0045 x [27D] x ([19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([7 0.0045 x [27D] x ([7	100 100 3] - [3 0 / [1 ter 2 Table rough 2] - [3 2] - [3	4329) x T + 1062.2 3]) 8] 3 14, Item [41] [46] 9])			48.0		7. 0. 0. 1. 1. 1. 1. 0. 26. -0. -0.
39 40 11 12 13 14 15 14 15 14 15 14 15 14 15 14 15 14 15 14 15 14 15 14 15 14 15 14 15 14 15 14 15 16 17 17 18 19 14 14 15 16 17 17 16 17 17 18 19 14 14 15 16 17 17 18 19 14 14 15 16 16 17 16 16 17 <td>Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] tuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in noisture in air, % Sensible heat in fuel, %</td> <td>H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([t [19] or [21] x 14.50 ABMA curve, Chap From Chapter 10, Summation [38] thr 0.0024 x [26D] x ([t</td> <td>100 100 3] - [3 0 / [1 ter 2 Table rough 2] - [3 2] - [3</td> <td>4329) x T + 1062.2 3]) 8] 3 14, Item [41] [46] 9])</td> <td></td> <td>based</td> <td>48.0</td> <td>t Btu/h H @ 80 ~ 1.0</td> <td>7. 0. 1. 1. 1. 0. 26. -0. -0. -0. 0.</td>	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] tuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in noisture in air, % Sensible heat in fuel, %	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([t [19] or [21] x 14.50 ABMA curve, Chap From Chapter 10, Summation [38] thr 0.0024 x [26D] x ([t	100 100 3] - [3 0 / [1 ter 2 Table rough 2] - [3 2] - [3	4329) x T + 1062.2 3]) 8] 3 14, Item [41] [46] 9])		based	48.0	t Btu/h H @ 80 ~ 1.0	7. 0. 1. 1. 1. 0. 26. -0. -0. -0. 0.
89 10 11 12 13 13 14 15 16 17 18 19 10 11	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, %	H1 = (3.958E-5 x T H2 = (332 [29] x ([39] - [40]) / 0.0045 x [27D] x ([19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([7 0.0045 x [27D] x ([7	100 5] - [3 0 / [1 ter 2 Table rough 2] - [3 2] - [3 3]) x	4329) x T + 1062.2 3]) 8] 3 14, Item [41] 146] 3]) 100 / [18]			48.0		7 0. 0. 1. 1. 0. 26. -0. -0. 0. 0.
39 40 41 42 43 44 45 46 47 48 49 50 51 52	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] % % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in dry air, % Sensible heat in fuel, % Other, %	H1 = (3.958E-5 x T H2 = (3) -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ((1 [19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([(H at T[4] - H at T[5]	100 5] - [3 0 / [1 ter 2 Table rough 2] - [3 2] - [3 3]) x	4329) x T + 1062.2 3]) 8] 3 14, Item [41] 146] 3]) 100 / [18]			48.0		7.: 0. 0. 1. 1. 0.
39 40 11 42 13 44 45 46 47 48 49 50 51 52 53	Dry Gas, % Water from fuel, as fired Enthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Teadits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS	H1 = (3.958E-5 x T H2 = (332 [29] x (199 - [40]) / 0.0045 x [27D] x ([1 [19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([2 0.0045 x [27D] x ([2 (H at T[4] - H at T] Summation [48] th 100 - [47] - [52]	100 5] - [3 0 / [1 ter 2 Table rough 2] - [3 2] - [3 3]) x	4329) x T + 1062.2 3]) 8] 3 14, Item [41] 146] 3]) 100 / [18]			48.0	H@ 80 ~ 1.0	7: 0. 0. 1. 1. 1. 26. -0. -0. -0. 0. 0. 0. 0. 74. Bir/Econ
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([f [19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, 7 Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([0.0045 x [27D] x ([(H at T[4] - H at T[Summation [48] th 100 - [47] - [52]	100 5] - [3 0 / [1 ter 2 Table rough 2] - [3 2] - [3 3]) x	4329) x T + 1062.2 3]) 8] 3 14, Item [41] 146] 3]) 100 / [18]		0.01	48.0	H@ 80 ~ 1.0	7. 0. 1. 1. 1. 26. -0. -0. -0. 0. 0. 0. 0. 0. 0. 0. 74. Bir/Econ
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55	Dry Gas, % Water from fuel, as fired Enthalpy of steam at 1 psi, T = [6] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in dry air, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 Ib/h	H1 = (3.958E-5 x T H2 = (332 (39) - (40)) / 0.0045 x (27D) x ((1 [19] or (21) x 14,50 ABMA curve. Chap From Chapter 10, Summation [38] ht 0.0024 x (26D) x ((2 0.0045 x (27D) x ((2 (H at T[4] - H at T[52] Summation [48] ht 100 - [47] - [52]	100 5] - [3 0 / [1 ter 2 Table rough 2] - [3 2] - [3 3]) x	4329) x T + 1062.2 3]) 8] 3 14, Item [41] 146] 3]) 100 / [18]		0.01	48.0 on output of plan	H@ 80 ~ 1.0	7: 0. 1. 1. 0. 266. -0. -0. -0. -0. -0. -0. -0. -0. -0. -0
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 56	Dry Gas, % Water from tuel, as fired Enthalpy of steam at 1 psi, T = [6] Tuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Moisture in air, % Moisture in air, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Wet gas weight, 1000 lb/h	$\begin{array}{l} \text{H1} = (3.958E\text{-}5 \times T\\ \text{H2} = (3)\text{-}32\\ (291 \times (139)\text{-}(401) /\\ 0.0045 \times (27D) \times ([1]\\ (19] \text{ or } (211 \times 14,50)\\ \text{ABMA curve, Chap}\\ \text{From Chapter 10,}\\ \text{Summation [38] th}\\ 0.0024 \times (26D) \times ([2]\\ 0.0045 \times (27D) \times ([2]\\ (\text{H at T[4] - H at T[3]}\\ \text{Summation [48] th}\\ 100 - [47] - [52]\\ \hline 1000 \times [10] / [53]\\ 1000 \times [54] / [18]\\ [54] \times (33) / 10\\ \end{array}$	+ 0. 100 6] - [3 0 / [1] tter 2 Table rough 2] - [3 3]) x rough	4329) x T + 1062.2 3]) 8] 3 144, Item [41] [46] 100 / [18] 100 / [18]		0.01	48.0 on output of plan Furnace 290.1	H@ 80 ~ 1.0	7: 0. 0. 1. 1. 1. 26. -0. -0. -0. 0. 0. 0. 0. 74. Bir/Econ
39 39 40 41 42 43 44 45 44 45 44 45 46 47 48 49 50 51 52 53 60 54 55 66 57	Dry Gas, % Water from fuel, as fired Enthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Moisture in air, % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Sorbent net losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Wet gas weight, 1000 lb/h Air to burners (wet), Ib/10,000 Btu	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D) x ([1 [19] or [21] x 14,50 ABMA curve. Chap From Chapter 10, Summation [38] thi 0.0024 x [26D] x ([2 0.0045 x [27D] x ([2 (H at T[4] - H at T[5] Summation [48] thi 100 - [47] - [52] 100 x [10] / [53] 1000 x [54] / [18] [54] x [33] / 10 (1 + [7]) x (1 + [25A	+ 0. 100 6] - [3 0 / [1] tter 2 Table rough 2] - [3 3]) x rough	4329) x T + 1062.2 3]) 8] 3 144, Item [41] [46] 100 / [18] 100 / [18]		0.01	48.0 on output of plan Furnace 290.1 8.765	H@ 80 ~ 1.0	7: 0. 1. 1. 0. 266. -0. -0. -0. -0. -0. -0. -0. -0. -0. -0
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 56 57 58	Dry Gas, % Water from fuel, as fired Enthalpy of steam at 1 psi, T = [6] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in dry air, % Summation of losses, % Credits Heat in dry air, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h We gas weight, 1000 lb/h Air to burners (wet), 1000 lb/h	$\begin{array}{l} \text{H1} = (3.958E\text{-}5\times\text{T} \\ \text{H2} = (332 \\ \text{H2} = (3)-32 \\ \text{(29)} \times (39) - (40) / \\ 0.0045 \times (27D) \times (10) \\ \text{(19)} \text{ or } (21) \times 14,50 \\ \text{ABMA curve. Chap} \\ \text{ABMA curve. Chap} \\ \text{ABMA curve. Chap} \\ \text{Summation} [38] \text{ thr} \\ 0.0024 \times (26D) \times (10) \\ \text{(100)} \times (27D) \times (10) \\ \text{(100)} \times (27D) \times (10) \\ \text{(100)} \times (54) / (18) \\ 1000 \times (54) / (18) \\ 1000 \times (54) / (18) \\ 1001 \times (12) \times (1 + (25A) \\ 1000 \times (54) / (18) \\ 1001 \times (12) \times (1 + (25A) \\ 1000 \times (54) / (18) \\ 1011 \times (1 + (25A) / 10) \\ 101$	+ 0. 100 3] - [3] 0 / [1 tter 2 0 / [1 tter 2 1 - [3] 2] - [3 2] - [3 2] - [3 2] - [3 3]) x	4329) x T + 1062.2 3]) 8] 3 114, Item [41] [46] 100 / [18] 100 / [18] 0) x [22]		0.01	48.0 on output of plan Furnace 290.1	H@ 80 ~ 1.0	7: 0. 1. 1. 0. 266. -0. -0. -0. -0. -0. -0. -0. -0. -0. -0
38 39 339 40 441 41 443 444 445 46 447 48 449 50 551 55 554 55 556 57 558 59	Dry Gas, % Water from fuel, as fired Enthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Moisture in air, % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Sorbent net losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Wet gas weight, 1000 lb/h Air to burners (wet), Ib/10,000 Btu	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D) x ([1 [19] or [21] x 14,50 ABMA curve. Chap From Chapter 10, Summation [38] thi 0.0024 x [26D] x ([2 0.0045 x [27D] x ([2 (H at T[4] - H at T[5] Summation [48] thi 100 - [47] - [52] 100 x [10] / [53] 1000 x [54] / [18] [54] x [33] / 10 (1 + [7]) x (1 + [25A	100 100 100 100 100 100 100 100	4329) x T + 1062.2 3]) 8] 3 14, Item [41] [46] 3]) 100 / [18] 100 / [18] 0) x [22] 0) x [22] 7H]) / [18] - 0.005		0.01	48.0 on output of plan Furnace 290.1 8.765	H@ 80 ~ 1.0	7: 0. 1. 1. 0. 266. -0. -0. -0. -0. -0. -0. -0. -0. -0. -0

	NPUT CONDITIONS - BY TEST OR SPECIFICATION			FUEL - Subbituminous	Coal, Minnesota	1			
1	Excess air: at burner/leaving boiler/econ, % by weight	23.3		15 Ultimate Analysis			b/100 lb fuel	17 H ₂ O, lb/1	100 lb fuel
2	Entering air temperature, F	39.96		Constituent	% by weight	K1	[15] x K1	K2	[15] x K2
3	Reference temperature, F	80	А		54.84	11.51	631.2		
4	Fuel temperature, F	62	В		0.33	4.32	1.4		
5	Air temperature leaving air heater, F	357.87	С		2.92	34.29	100.1	8.94	26
6	Flue gas temperature leaving (excluding leakage), F	845.08	D	H ₂ O	23.56			1.00	23
7	Moisture in air, Ib/Ib dry air	0.004	Е	N ₂	1.12				
, 8	Additional moisture, Ib/100 lb fuel	0	F	0 ₂	13.64	-4.32	-58.9		
9	Residue leaving boiler/economizer, % Total	85	G	-	3.59	4.02	00.0		
0	Output, 1,000,000 Btu/h (MMBtu/h)	225.80	н	Total	100.00	Air	673.8	H ₂ O	49
1	Additional theoretical air, lb/10,000 Btu Table 14, Item [2	0	10	Higher heating value		ol	•	•	9,
2	CO ₂ from sorbent, lb/10,000 Btu Table 14, Item [19]	0	18 19			ei			9,
					· · ·		1401 P 400 (1		
3	H ₂ O from sorbent, lb/10,000 Btu Table 14, Item [20]	0	20	Theoretical air, lb/10,			[16H] x 100 /		7.
4	Spent sorbent, lb/10,000 Btu Table 14, Item [24] COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu	0	21	Unburned carbon, %	ot tuel		[19] x [18] / 14	4,500	(
22	Theoretical air (corrected), Ib/10,000 Btu	[20] - [21] x 1151 /	[10]	. [11]					7.088
23	Residue from fuel, Ib/10,000 Btu	([15G] + [21]) x 100	0/[1	8]					0.039
24	Total residue, Ib/10,000 Btu	[23] + [14]	<u>, [</u>	~1					0.039
		() · [· ·]	A	At Burners	B Infiltration	C Leaving F	urnace	D Leaving	
5	Excess air, % by weight			23.3	0.0	,	23.3		23
26	Dry air, lb/10,000 Btu	(1 + [25] / 100) x [2	22]				8.739		8.
27	H ₂ O from air, lb/10,000 Btu	[26] x [7]				0.035	0.035	0.035	0.
8	Additional moisture, lb/10,000 Btu	[8] x 100 / [18]				0.000	0.000	0.000	0.
9	H ₂ O from fuel, lb/10,000 Btu	[17H] x 100 / [18]				0.523		0.523	l i i i i i i i i i i i i i i i i i i i
80	Wet gas from fuel, lb/10,000 Btu	(100 - [15G] - [21])	x 10	00 / [18]			1.015		1.
31	CO ₂ from sorbent, lb/10,000 Btu	[12]					0.000		0.
32	H ₂ O from sorbent, lb/10,000 Btu	[13]				0.000	0.000	0.000	0.
33	Total wet gas, lb/10,000 Btu	Summation [26] the	roua	h [32]			9.789		9.
34	Water in wet gas, lb/10,000 Btu	Summation [27] +	[28]	+ [29] + [32]		0.558	0.558	0.558	0.
35	Dry gas, lb/10,000 Btu	[33] - [34]					9.230		9.
86	H ₂ O in gas, % in weight	100 x [34] / [33]					5.70		Ę
37	Residue, % by weight (zero if < 0.15 lbm/10KB)	[9] x [24] / [33]					0.34		(
1	EFFICIENCY CALCULATIONS, % Input from Fuel								
	Losses			- 1)		1			
88	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6]	0.0024 x [35d] x ([6					4450.0		16
89 10	Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3]	$H1 = (3.958E-5 \times 1)$ H2 = [3] -32	+ 0	.4329) x T + 1062.2			1456.3 48.0		
1	%	[29] x ([39] - [40]) /	100				40.0		7
2	Moisture in air, %	0.0045 x [27D] x ([,
13	Unburned carbon, %	[19] or [21] x 14,50							(
4	Radiation and convection, %	ABMA curve, Chap				based	on output of plan	it Btu/h	1
15	Other, % (include manufacturers margin if applicable)								1
6	Sorbent net losses, % if sorbent is used	From Chapter 10,							(
17	Summation of losses, %	Summation [38] the	roug	h [46]					26
0	Credits	0.0004 y [000] - ///	01 7	201)					
8 9	Heat in dry air, % Heat in moisture in air, %	0.0024 x [26D] x ([0.0045 x [27D] x ([-(
i9	Sensible heat in fuel, %	(H at T[4] - H at T[3				0.01		H@80~1.0	-(
51	Other, %	<u>, 1 at 1[+]</u> - 11 at 1[t	- <u>,</u> , ,			0.01			(
52	Summation of credits, %	Summation [48] the	roug	h [51]		1			-(
53	Efficiency, %	100 - [47] - [52]	J						74
	KEY PERFORMANCE PARAMETERS					Leaving	Furnace	Leavin	g Blr/Econ
54	Input from fuel, 1,000,000 Btu/h	100 x [10] / [53]	_						- 30
55	Fuel rate, 1000 lb/h	1000 x [54] / [18]							3
6	Wet gas weight, 1000 lb/h	[54] x [33] / 10					297.7		29
57	Air to burners (wet), lb/10,000 Btu	(1 +[7]) x (1 + [25A	J / 1	00) x [22]			8.774		
58 59	Air to burners (wet), 1000 lb/h	[54] x [57] / 10	۰ ر I	741)/[10] 0.005			266.8		
9	Heat available, 1,000,000 Btu/h Ha [Btu/h] 68.70	[54] x {([18] - 10.30 x ([44] + [45]) + Ha					202.0		
			all	[0] x [0/] / 10,000}			303.0		
60	Heat available/lb wet gas, Btu/lb	1000 x [59] / [56]							

1	INPUT CONDITIONS - BY TEST OR SPECIFICATION	-	_	FUEL - Subbituminou							
	Excess air: at burner/leaving boiler/econ, % by weight	18.2		15 Ultimate Analys		16	1	b/100 lb fuel	17 H ₂ O, lt		
2	Entering air temperature, F	39.22		Constituent	% by weight	K1		[15] x K1	K2	[15] x	: K2
3	Reference temperature, F	80 63	AB		54.44		11.51 4.32	626.6		_	
4 5	Fuel temperature, F Air temperature leaving air heater, F	356.57	C	S H ₂	0.33 2.95	-	4.32 34.29	1.4	8.94		26.3
-		840.43		H ₂ O	23.85		34.23	101.2	1.00		20.
6	Flue gas temperature leaving (excluding leakage), F		D						1.00		23.0
7	Moisture in air, Ib/Ib dry air	0.0041	E	N ₂	0.54					_	
8	Additional moisture, lb/100 lb fuel	0	F	O ₂	13.91		-4.32	-60.1		_	
9 10	Residue leaving boiler/economizer, % Total	85	G		3.98		A :	0.00.4			50
10	Output, 1,000,000 Btu/h (MMBtu/h)	221.32	н	Total	100.00		Air	669.1	H2O		50.
11	Additional theoretical air, lb/10,000 Btu Table 14, Item [2	0	18	Higher heating valu	e (HHV). Btu/lb fu	iel					9,4
12	CO ₂ from sorbent, lb/10,000 Btu Table 14, Item [19]	0	19								0.
13	H ₂ O from sorbent, lb/10,000 Btu Table 14, Item [20]	0	0 20 Theoretical air, lb/10,000 Btu [16H] x 100 / [18]					7.1			
14	Spent sorbent, lb/10,000 Btu Table 14, Item [24]	0	21					[19] x [18] / 1			0.
		•		onbanica carbon,					1,000		0.
	COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btt	u Fuel Input									
22	Theoretical air (corrected), lb/10,000 Btu	[20] - [21] x 1151 /								7.088	
23	Residue from fuel, Ib/10,000 Btu		([15G] + [21]) × 100 / [18]							0.043	
24	Total residue, lb/10,000 Btu	[23] + [14]	1 ·						181	0.043	
5	Excess air, % by weight		Α	At Burners 18.2	B Infiltration 0.0	C	Leaving Fu	Irnace 18.2	D Leavin	g Bir/Econ	18.2
5 6	Excess air, % by weight Dry air, lb/10,000 Btu	(1 + [25] / 100) x [2	221	18.2	0.0		_	18.2 8.382			18.3
7	H ₂ O from air, Ib/10,000 Btu	[26] x [7]	22]				0.034	0.034	0.034		0.0
28	Additional moisture, Ib/10,000 Btu	[8] x 100 / [18]					0.004	0.000	0.004		0.0
20 29	H ₂ O from fuel, Ib/10,000 Btu	[17H] x 100 / [18]					0.533	0.000	0.000		0.0
30	Wet gas from fuel, lb/10,000 Btu) v 10	00 / [10]			0.555	1.019	0.555		1.0
80 81	CO ₂ from sorbent, lb/10,000 Btu	(100 - [15G] - [21]) x 100 / [18]						1.018			1.0
-			[12]				0.000		0.000		
32	H ₂ O from sorbent, Ib/10,000 Btu		[13] 0.000					0.000	0.000		0.0
33 34	Total wet gas, Ib/10,000 Btu	Summation [26] th					0.567	9.434	0.567		9.4 0.5
34 35	Water in wet gas, lb/10,000 Btu Dry gas, lb/10,000 Btu	Summation [27] + [33] - [34]	[28]	+ [29] + [32]			0.567	0.567 8.867	0.567	_	0.5 8.8
36	H ₂ O in gas, % in weight	100 x [34] / [33]						6.01			6.
37	Residue, % by weight (zero if < 0.15 lbm/10KB)	[9] x [24] / [33]						0.39			0.
	EFFICIENCY CALCULATIONS, % Input from Fuel										
	Losses			- 10							
38	Dry Gas, %	0.0024 x [35d] x ([1		1454.0			16.
39	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6]	H1 = (3.958E-5 x		3]) 0.4329) x T + 1062.2				1454.0			16.
39 40	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3]	H1 = (3.958E-5 x H2 = [3] -32	T + C	0.4329) x T + 1062.2				1454.0 48.0			
39 40 41	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired %	H1 = (3.958E-5 x H2 = [3] -32 [29] x ([39] - [40])	T + 0 / 100	0.4329) x T + 1062.2							7.
39 40	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3]	H1 = (3.958E-5 x H2 = [3] -32	T + 0 / 100 [6] -).4329) x T + 1062.2) [3])							
39 40 41 42 43	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Moisture in air, %	H1 = (3.958E-5 x H2 = [3] -32 [29] x ([39] - [40]) 0.0045 x [27D] x (T + 0 / 100 [6] -] 00 / [0.4329) x T + 1062.2 (3)) 18]			based (nt Btu/h		7.
39 40 41 42 43 44 45	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable)	H1 = (3.958E-5 x H2 = [3] -32 [29] x ([39] - [40]) , 0.0045 x [27D] x (([19] or [21] x 14,50 ABMA curve, Cha	T + 0 / 100 [6] - [00 / [pter :	0.4329) x T + 1062.2 (3) 18] 23			based (48.0	nt Btu/h		7. 0. 0. 1.
39 40 41 42 43 44 45 46	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used	H1 = (3.958E-5 x ⁻ H2 = [3] -32 [29] x ([39] - [40]). 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Cha From Chapter 10,	T + 0 / 100 [6] -] [00 / [pter : Tabl	0.4329) x T + 1062.2 (3]) 18] 23 le 14, Item [41]			based (48.0	nt Btu/h		7. 0. 0. 1. 1. 0.
39 40 41 42 43 44	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, %	H1 = (3.958E-5 x H2 = [3] -32 [29] x ([39] - [40]) , 0.0045 x [27D] x (([19] or [21] x 14,50 ABMA curve, Cha	T + 0 / 100 [6] -] [00 / [pter : Tabl	0.4329) x T + 1062.2 (3]) 18] 23 le 14, Item [41]			based o	48.0	nt Btu/h		7. 0. 0. 1. 1. 0.
39 40 41 42 43 44 45 46 47	Dry Gas, % Enthalpy of steam at 1 psi, T = [6] Water from Enthalpy of water at T = [3] % Enthalpy of water at T = [3] % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits	H1 = (3.958E-5 x ⁻¹ H2 = [3]-32 [29] x ([39] - [40]) 0.0045 x [27D] x ([[19] or [21] x 14.50 ABMA curve, Cha From Chapter 10, Summation [38] th	T + 0 / 100 [6] -] D0 / [pter : Tabl	0.4329) x T + 1062.2 (3]) 18] 23 le 14, Item [41] th [46]			based o	48.0	nt Btu/h		7. 0. 1. 1. 0. 25.
39 40 41 42 43 44 45 46 47 48	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] (uel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, %	H1 = (3.958E-5 x ⁺ H2 = (3)-32 [29] x ((39) - (40)), 0.0045 x [27D] x (([19] or [21] x 14,5(ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x ((T + 0 / 100 [6] -] D0 / [pter : Tabl moug	0.4329) x T + 1062.2 (3]) 18] 23 le 14, Item [41] h [46] (3])			based o	48.0	nt Btu/h		7. 0. 0. 1. 1. 25. -0.
39 40 41 42 43 44 45 46 47 48 49	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, %	H1 = (3.958E-5 x ²) H2 = [3] -32 [29] x ([39] - [40]), 0.0045 x [27D] x (1 [19] or [21] x 14,50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (1 0.0045 x [27D] x (1	T + 0 / 100 [6] -] 00 / [pter : Tabl moug [2] -] [2] -]	1.4329) x T + 1062.2 (3) 18] 23 le 14, Item [41] (46] (3)) (3)			based (48.0			7. 0. 1. 1. 25. -0. -0.
39 40 41 42 43 44 45 46 47 48 49 50	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] (uel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, %	H1 = (3.958E-5 x ⁺ H2 = (3)-32 [29] x ((39) - (40)), 0.0045 x [27D] x (([19] or [21] x 14,5(ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x ((T + 0 / 100 [6] -] 00 / [pter : Tabl moug [2] -] [2] -]	1.4329) x T + 1062.2 (3) 18] 23 le 14, Item [41] (46] (3)) (3)				48.0	nt Btu/h H @ 80 ~ 1.0		7. 0. 0. 1. 1. 25. -0.
9 10 11 12 13 14 15 16 17 18 19 00 11	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, %	H1 = (3.958E-5 x ²) H2 = [3] -32 [29] x ([39] - [40]), 0.0045 x [27D] x (1 [19] or [21] x 14,50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (1 0.0045 x [27D] x (1	T + 0 / 100 [6] -] 00 / [pter : Tabl roug [2] -] [2] -] [3]) x	1.4329) x T + 1062.2 (3)) (3)) 18] 23 le 14, Item [41] th [46] (3)) (3)) (30) / [18]				48.0			7. 0. 0. 1. 1. 25. -0. -0. 0. 0. -0.
9 0 1 2 3 4 5 6 7 8 9 0 1 2	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] (uel, as fired % Moisture in air, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, %	H1 = (3.958E-5x * H2 = [3] -32 [29] x ([39] - [40]) . 0.0045 x [27D] x ([19] or [21] x 14.50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (0.0045 x [27D] x ((H at T[4] - H at T[T + 0 / 100 [6] -] 00 / [pter : Tabl roug [2] -] [2] -] [3]) x	1.4329) x T + 1062.2 (3)) (3)) 18] 23 le 14, Item [41] th [46] (3)) (3)) 100 / [18]				48.0			7. 0. 0. 1. 1. 25. -0. -0. -0. 0.
9 40 41 42 43 44 45 46 47 48 49 50 51 52 53	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in dry air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, %	H1 = (3.958E-5 x ² H2 = [3] -32 [29] x ([39] - [40]). 0.0045 x [27D] x (([19] or [21] x 14,50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x ((0.0045 x [27D] x ((H at T[4] - H at T[Summation [48] th	T + 0 / 100 [6] -] 00 / [pter : Tabl roug [2] -] [2] -] [3]) x	1.4329) x T + 1062.2 (3)) (3)) 18] 23 le 14, Item [41] th [46] (3)) (3)) 100 / [18]			0.01	48.0	H @ 80 ~ 1.0		7 0. 1. 1. 1. 255. -0. -0. 0. 0. -0. 74.
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53	Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Teaditis Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS	H1 = (3.958E-5 x ² H2 = [3] -32 [29] x ([39] - [40]), 0.0045 x [27D] x (1 [19] or [21] x 14,50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (1 0.0045 x [27D] x (1 (H at T[4] - H at T] Summation [48] th 100 - [47] - [52]	T + 0 / 100 [6] -] 00 / [pter : Tabl roug [2] -] [2] -] [3]) x	1.4329) x T + 1062.2 (3)) (3)) 18] 23 le 14, Item [41] th [46] (3)) (3)) 100 / [18]				48.0	H @ 80 ~ 1.0	ing Bir/Eco	7 0. 0. 1. 1. 1. 25. -0. -0. 0. 0. 0. -0. 74.
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in closses, % Credits Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h	H1 = (3.958E-5 x ⁻¹ H2 = [3]-32 [29] x ([39] - [40]), 0.0045 x [27D] x ([[19] or [21] x 14,5(ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x ((0.0045 x [27D] x ([(H at T[4] - H at T] Summation [48] th 100 - [47] - [52]	T + 0 / 100 [6] -] 00 / [pter : Tabl roug [2] -] [2] -] [3]) x	1.4329) x T + 1062.2 (3)) (3)) 18] 23 le 14, Item [41] th [46] (3)) (3)) 100 / [18]			0.01	48.0	H @ 80 ~ 1.0		7 0. 0. 1. 1. 1. 25. -0. -0. -0. 0. 0. -0. 74.
39 40 41 42 43 44 45 46 47 48 49 50 51 52 54 55	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] (bel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/n	H1 = (3.958E-5 x ⁻ H2 = [3] -32 [29] x ([39] - [40]). 0.0045 x [27D] x (1 [19] or [21] x 14,50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (1 0.0045 x [27D] x (1 (H at T[4] - H at T] Summation [48] th 100 - [47] - [52]	T + 0 / 100 [6] -] 00 / [pter : Tabl roug [2] -] [2] -] [3]) x	1.4329) x T + 1062.2 (3)) (3)) 18] 23 le 14, Item [41] th [46] (3)) (3)) 100 / [18]			0.01	48.0 on output of plan	H @ 80 ~ 1.0		7. 0. 0. 1. 1. 25. -0. -0. -0. -0. -0. -0. -0. -0. -0. -0
39 40 41 42 44 45 46 47 48 49 50 51 52 55 56	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] (uel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Wet gas weight, 1000 lb/h	H1 = (3.958E-5 x ² H2 = [3]-32 [29] x ([39] - [40]), 0.0045 x [27D] x (1 [19] or [21] x 14,50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (1 0.0045 x [27D] x (1 (H at T[4] - H at T] Summation [48] th 100 - [47] - [52] 100 x [10] / [53] 1000 x [54] / [18]	T + 0 / 100 [6] - [00 / [pter : Tabl nroug [2] - [2] - [3]) x	1.4329) x T + 1062.2 (31) 18] 23 24 23 23 23 23 23 23 23 23 23 23			0.01	48.0	H @ 80 ~ 1.0		7. 0. 0. 1. 1. 25. -0. -0. -0. -0. -0. -0. -0. -0. -0. -0
39 40 41 42 43 44 5 6 5 5 5 6 5 5 6 5 5 6 5 5 5 6 5 5 6 5 7 5 5 6 7 </td <td>Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] (bel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/n</td> <td>H1 = (3.958E-5 x⁻ H2 = [3] -32 [29] x ([39] - [40]). 0.0045 x [27D] x (1 [19] or [21] x 14,50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (1 0.0045 x [27D] x (1 (H at T[4] - H at T] Summation [48] th 100 - [47] - [52]</td> <td>T + 0 / 100 [6] - [00 / [pter : Tabl nroug [2] - [2] - [3]) x</td> <td>1.4329) x T + 1062.2 (31) 18] 23 24 23 23 23 23 23 23 23 23 23 23</td> <td></td> <td></td> <td>0.01</td> <td>48.0 on output of play Furnace 276.9</td> <td>H @ 80 ~ 1.0</td> <td></td> <td>77 0. 0. 1. 1. 255 -0. -0. -0. -0. -0. -0. -0. -0. -0. -0.</td>	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] (bel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/n	H1 = (3.958E-5 x ⁻ H2 = [3] -32 [29] x ([39] - [40]). 0.0045 x [27D] x (1 [19] or [21] x 14,50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (1 0.0045 x [27D] x (1 (H at T[4] - H at T] Summation [48] th 100 - [47] - [52]	T + 0 / 100 [6] - [00 / [pter : Tabl nroug [2] - [2] - [3]) x	1.4329) x T + 1062.2 (31) 18] 23 24 23 23 23 23 23 23 23 23 23 23			0.01	48.0 on output of play Furnace 276.9	H @ 80 ~ 1.0		77 0. 0. 1. 1. 255 -0. -0. -0. -0. -0. -0. -0. -0. -0. -0.
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in closses, % Credits Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Wet gas weight, 1000 lb/h	H1 = (3.958E-5 x ⁻¹ H2 = (3)-32 (29) x ((39) - [40]), 0.0045 x [27D] x (1 (19) or (21) x 14,5(ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (1 0.0045 x [27D] x (1 (H at T[4] - H at T] Summation [48] th 100 - [47] - [52] 100 x [10] / [53] 1000 x [54] / [18] (54] x [33] / 10 (1 + [7]) x (1 + [25/	T + 0 / 1000 [6] -] 00 / [pter : Tabl mroug [2] -] [2] -] [2] -] [2] -] [2] -] [3]) x	1.4329) x T + 1062.2 (3)) 18] 23 16 14, Item [41] 16 [46] (3)) 100 / [18] 100 / [18] 00) x [22]			0.01	48.0 on output of plan Furnace 278.9 8.416	H @ 80 ~ 1.0		7 0. 0. 1. 1. 1. 25. -0. -0. 0. 0. 0. -0. 74.
39 40 41 42 43 44 54 64 7 84 90 51 52 53 54 55 56 57 58 54 55 56 57 58 56 57 58	Dry Gas, % Water from Lenthalpy of steam at 1 psi, T = [6] (bel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in dry air, % Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Wet gas weight, 1000 lb/h Air to burners (wet), 1000 lb/h	H1 = (3.958E-5 x ² H2 = [3]-32 [29] x ([39]-[40]). 0.0045 x [27D] x (1 [19] or [21] x 14,50 ABMA curve, Cha From Chapter 10, Summation [38] th 0.0024 x [26D] x (1 0.0045 x [27D] x (1 (H at T[4] - H at T[0.0045 x [27D] x (1 (H at T[4] - H at T[4	T + 0 / 100 [6] -] D0 / [pter : Tabl rroug [2] -] [2] -] [2] -] [2] -] [3]) x mroug	1.4329) x T + 1062.2 (3)) 18] 23 16 14, Item [41] 16 [46] (3)) 100 / [18] 100 / [18] 00) x [22]			0.01	48.0 on output of plan Furnace 278.9 8.416	H @ 80 ~ 1.0		7. 0. 0. 1. 1. 25. -0. -0. -0. -0. -0. -0. -0. -0. -0. -0

	NPUT CONDITIONS - BY TEST OR SPECIFICATION			FUEL - Subbituminous	Coal, Minnesota	1					
1	Excess air: at burner/leaving boiler/econ, % by weight	22.3		15 Ultimate Analysis			heo Air. I	b/100 lb fuel	17 H ₂ O, lb/1	00 lb fu	el
2	Entering air temperature, F	44.61		Constituent	% by weight	K1	,	[15] x K1	K2	[15] x	
3	Reference temperature, F	80	Α	С	29.57		11.51	340.3			
4	Fuel temperature, F	62	В		0.04		4.32	0.2			
5	Air temperature leaving air heater, F	409.77	С	H ₂	2.78		34.29	95.4	8.94		24.
6	Flue gas temperature leaving (excluding leakage), F	881.09	D	H₂O	43.60				1.00		43.
7	Moisture in air, lb/lb dry air	0.00325	Е	N ₂	0.30						
8	Additional moisture, lb/100 lb fuel	0	F	O ₂	22.06		-4.32	-95.3			
9	Residue leaving boiler/economizer, % Total	85	G	Ash	1.65						
0	Output, 1,000,000 Btu/h (MMBtu/h)	227.85	Н	Total	100.00		Air	340.6	H ₂ O		68
11	Additional theoretical air, lb/10,000 Btu Table 14, Item [2]	0	18	Higher heating value	(HHV), Btu/lb fu	el					8,9
12	CO2 from sorbent, lb/10,000 Btu Table 14, Item [19]	0	19	Unburned carbon los	s, % fuel input						0.
13	H ₂ O from sorbent, lb/10,000 Btu Table 14, Item [20]	0	20			[18]		3.7			
4	Spent sorbent, lb/10,000 Btu Table 14, Item [24]	0	21	Unburned carbon, %	of fuel			[19] x [18] / 14	,500		0
	COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu	Fuel Input									
22	Theoretical air (corrected), lb/10,000 Btu	[20] - [21] x 1151 /								3.774	
23	Residue from fuel, Ib/10,000 Btu	([15G] + [21]) x 100) / [1	8]						0.020	
24	Total residue, lb/10,000 Btu	[23] + [14]	•	At Durnara	D Infiltration		oouina F	112000	Dlag	0.020 Dir/Ease	
25	Excess air, % by weight		A	At Burners 22.3	B Infiltration 0.0		eaving Fi	urnace 22.3	D Leaving	DIF/ECON	22.
26	Drv air. 1b/10.000 Btu	(1 + [25] / 100) x [2	21	22.3	0.0		_	4.615			4.6
27	H ₂ O from air, Ib/10,000 Btu	[26] x [7]					0.015	0.015	0.015		0.0
28	Additional moisture, Ib/10,000 Btu	[8] x 100 / [18]					0.000	0.000	0.000		0.0
29	H ₂ O from fuel, lb/10,000 Btu	[17H] x 100 / [18]					0.763		0.763		
30	Wet gas from fuel, lb/10,000 Btu	(100 - [15G] - [21])	x 10	0 / [18]				1.094			1.0
31	CO ₂ from sorbent, lb/10,000 Btu	[12]						0.000			0.0
32	H ₂ O from sorbent, lb/10,000 Btu	[13]					0.000	0.000	0.000		0.0
33	Total wet gas, Ib/10,000 Btu	Summation [26] thr	ona	h [32]				5.725			5.7
34	Water in wet gas, Ib/10,000 Btu	Summation [27] + [0.778	0.778	0.778		0.7
35	Dry gas, lb/10,000 Btu	[33] - [34]						4.947		•	4.9
36	H ₂ O in gas, % in weight	100 x [34] / [33]						13.59			13.
37	Residue, % by weight (zero if < 0.15 lbm/10KB)	[9] x [24] / [33]						0.30			0
	EFFICIENCY CALCULATIONS, % Input from Fuel										
38	Losses Dry Gas, %	0.0024 [35D] x ([6]	- [3])		1				1	9
39	Water from Enthalpy of steam at 1 psi, T = [6]	$H1 = (3.958E-5 \times T)$	- [J] - + 0	4329) x T + 1062.2				1474.4			3
10	fuel, as fired Enthalpy of water at $T = [3]$	H2 = [3] -32	τU	.4020/ X 1 + 1002.2				48.0			
11	%	[29] x ([39] - [40]) /	100								10
2	Moisture in air, %	0.0045 x [27D] x ([0
13	Unburned carbon, %	[19] or [21] x 14,50									0
4	Radiation and convection, %	ABMA curve, Chap	oter 2	23			based	on output of plan	t Btu/h		1
15 16	Other, % (include manufacturers margin if applicable)	From Chapter 10	Tabl	a 14. Itom [41]							1
16	Sorbent net losses, % if sorbent is used Summation of losses, %	From Chapter 10, Summation [38] thr				l					22
T /	Credits	Sammation [36] th	Jug	וסדן יי							
8	Heat in dry air, %	0.0024 x [26D] x ([2	2] - [3])							-0
19	Heat in moisture in air, %	0.0045 x [27D] x ([2	2] - [3])							0
50 51	Sensible heat in fuel, % Other, %	(H at T[4] - H at T[3	3]) x	100 / [18]			0.01		H @ 80 ~ 1.0		0
52	Summation of credits, %	Summation [48] thr	000	h [51]							-0
53	Efficiency, %	100 - [47] - [52]	Jug	·· [- ']							77
	KEY PERFORMANCE PARAMETERS						Leaving	Furnace	Leavin	g Blr/Eco	
54	Input from fuel, 1,000,000 Btu/h	100 x [10] / [53]									29
55	Fuel rate, 1000 lb/h	1000 x [54] / [18]						100.0	ļ		3
56	Wet gas weight, 1000 lb/h	[54] x [33] / 10	1/44	0) v [22]				168.0 4.630			16
57 58	Air to burners (wet), lb/10,000 Btu Air to burners (wet), 1000 lb/h	(1 +[7]) x (1 + [25A [54] x [57] / 10	1/10	JUJ X [22]				4.630			
59	Heat available, 1,000,000 Btu/h	[54] x {([18] - 10.30) x [1	7H]) / [18] - 0.005				130.9			
-	Ha [Btu/h] 81.54	x ([44] + [45]) + Ha	at T	[5] x [57] / 10.0003				278.5			
50	Ha [Btu/h] 81.54 Heat available/lb wet gas, Btu/lb	x ([44] + [45]) + Ha 1000 x [59] / [56]	at T	[5] x [57] / 10,000}				278.5			

NPUT CONDITIONS - BY TEST OR SPECIFICATION			FUEL - Subbituminous C	oal, Minnesota				
Excess air: at burner/leaving boiler/econ, % by weight	20.5		15 Ultimate Analysis		16 Theo Air, I	b/100 lb fuel	17 H ₂ O, lb/1	00 lb fuel
	48.19		Constituent	% by weight	K1	[15] x K1	K2	[15] x K2
Reference temperature, F	80	Α	С	29.01	11.51	333.9		
Fuel temperature, F	64		S	0.05		0.2		
Air temperature leaving air heater, F	409.77	_	H ₂	2.98	34.29	102.3		26.
Flue gas temperature leaving (excluding leakage), F	857.90	D	H ₂ O	46.02			1.00	46.
Moisture in air, lb/lb dry air	0.0044	Е	N ₂	0.42				
Additional moisture, lb/100 lb fuel	0	F	O ₂	20.35	-4.32	-87.9		
Residue leaving boiler/economizer, % Total	85	G	Ash	1.16				
Output, 1,000,000 Btu/h (MMBtu/h)	219.94	н	Total	100.00	Air	348.5	H ₂ O	72
Additional theoretical air, lb/10,000 Btu Table 14, Item [2	0	18	Higher heating value (HHV), Btu/lb fue	əl			8,9
CO2 from sorbent, lb/10,000 Btu Table 14, Item [19]	0	19	Unburned carbon loss	, % fuel input				0
H ₂ O from sorbent, lb/10,000 Btu Table 14, Item [20]	0	20	Theoretical air, lb/10,0	100 Btu		[16H] x 100 / [[18]	3.9
Spent sorbent, lb/10,000 Btu Table 14, Item [24]	0	21	Unburned carbon, % of	of fuel		[19] x [18] / 14	1,500	0
COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu	Fuel Input							
Theoretical air (corrected), lb/10,000 Btu	[20] - [21] x 1151 /	[18]	+ [11]					3.878
		U / [1	6]					0.015
Total residue, ID/TU,000 Btu	[23] + [14]	Δ	At Burners	B Infiltration		urnace		
Excess air, % by weight							Leaving	20.
Dry air, lb/10,000 Btu	(1 + [25] / 100) x [2	22]	20.0	0.0		4.671		4.6
					0.021	0.021	0.021	0.0
Additional moisture, lb/10,000 Btu	[8] x 100 / [18]				0.000	0.000	0.000	0.0
H ₂ O from fuel, Ib/10,000 Btu	[17H] x 100 / [18]				0.815		0.815	
Wet gas from fuel, lb/10,000 Btu	(100 - [15G] - [21])	x 10	0 / [18]			1.105		1.1
CO ₂ from sorbent, lb/10,000 Btu	[12]					0.000		0.0
H ₂ O from sorbent, lb/10,000 Btu	[13]				0.000	0.000	0.000	0.0
Total wet gas, lb/10,000 Btu		rougł	n [32]			5.797		5.7
Water in wet gas, Ib/10,000 Btu					0.835	0.835	0.835	0.0
Dry gas, lb/10,000 Btu	[33] - [34]					4.962		4.9
H ₂ O in gas, % in weight	100 x [34] / [33]					14.41		14
Residue, % by weight (zero if < 0.15 lbm/10KB)	[9] x [24] / [33]				<u> </u>	0.23		0
•								
Dry Gas, %	0.0004 [05.1] /[/	21 10						0
Water from Enthelpu of stoom at 1 pci T [6]	0.0024 x [35d] x ([6					1460 7		9
Water from Enthalpy of steam at 1 psi, T = [6]	H1 = (3.958E-5 x T				<u> </u>	1462.7		9
fuel, as fired Enthalpy of water at T = [3]	H1 = (3.958E-5 x 1 H2 = [3] -32	+ 0.	4329) x T + 1062.2			1462.7 48.0		
	H1 = (3.958E-5 x T	+ 0. 100	4329) x T + 1062.2					9 11 0
fuel, as fired Enthalpy of water at T = [3]	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) /	- + 0. 100 6] - [3	4329) x T + 1062.2 3])					11 0 0
fuel, as fired % Enthalpy of water at T = [3] Moisture in air, % Unburned carbon, % Radiation and convection, %	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([- + 0. 100 6] - [3 0 / [1	4329) x T + 1062.2 3]) 8]		based		t Btu/h	11 0 0 1
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable)	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap	+ 0. 100 6] - [(0 / [1 oter 2	4329) x T + 1062.2 3]) 8] 3		based	48.0	t Btu/h	11 0 0 1 1
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbert net losses, % if sorbert is used	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap From Chapter 10,	+ 0. 100 6] - [3 0 / [1 oter 2 Table	4329) x T + 1062.2 3]) 8] 3 9 14, Item [41]		based of	48.0	t Btu/h	11 C C 1 1 1 0
fuel, as fired % Enthalpy of water at T = [3] Moisture in air, % Unburned carbon, % Unburned carbon, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, %	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap	+ 0. 100 6] - [3 0 / [1 oter 2 Table	4329) x T + 1062.2 3]) 8] 3 9 14, Item [41]		based o	48.0	t Btu/h	11 C C 1 1 1 0
fuel, as fired Enthalpy of water at T = [3] Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th	⁻ + 0. 100 6] - [3 0 / [1 oter 2 Table rough	4329) x T + 1062.2 3]) 8] 3 9 14, Item [41] 146]		based	48.0	t Btu/h	11 0 0 1 1 1 0 23
fuel, as fired % Enthalpy of water at T = [3] Moisture in air, % Unburned carbon, % Unburned carbon, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, %	H1 = (3.958E-5 x T H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap From Chapter 10,	⁻ + 0. 100 6] - [3 0 / [1 0 / [1 0 rer 2 Table rough 2] - [3	4329) x T + 1062.2 3]) 8] 3 9 14, Item [41] 1 [46] 3])		based	48.0	t Btu/h	11 0 0 1 1 0 23 -0
fuel, as fired % Enthalpy of water at T = [3] Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, %	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([⁻ + 0. 100 6] - [(0 / [1 oter 2 Table rough 2] - [(2] - [(4329) x T + 1062.2 3]) 8] 3 2 14, Item [41] 1 [46] 3])		based 0	48.0	t Btu/h H @ 80 ~ 1.0	11 0 1 1 23 -0 0 0 0
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, %	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([(H at T[4] - H at T]	Table 7 - [3] - [3	4329) x T + 1062.2 3]) 8] 3 4 14, Item [41] 6 [46] 3]) 100 / [18]			48.0		11 0 0 1 1 1 0 23 -0 0 0 0 0 0 0 0
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, %	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([(H at T[4] - H at T]]	Table 7 - [3] - [3	4329) x T + 1062.2 3]) 8] 3 4 14, Item [41] 6 [46] 3]) 100 / [18]			48.0		111 0 0 1 1 1 0 23 23 -0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, %	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([(H at T[4] - H at T]	Table 7 - [3] - [3	4329) x T + 1062.2 3]) 8] 3 4 14, Item [41] 6 [46] 3]) 100 / [18]		0.01	48.0 on output of plan	H@ 80 ~ 1.0	111 0 0 23 -0 0 0 0 0 0 0 0 0 0 0 0 77
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([(H at T[4] - H at T]; Summation [48] th 100 - [47] - [52]	Table 7 - [3] - [3	4329) x T + 1062.2 3]) 8] 3 4 14, Item [41] 6 [46] 3]) 100 / [18]		0.01	48.0	H@ 80 ~ 1.0	111 0 0 1 1 1 0 23 23 -0 0 0 0 0 0 0 0 0 77 77 Blr/Econ
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Addiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Sorbent net losses, % if sorbent is used Summation of losses, % Gredits Gredits Heat in moisture in air, % Sensible heat in fuel, % Other, % Efficiency, % Efficiency, % Efficiency, %	$\begin{array}{l} \text{H1} = (3.958E-5 \times 1\\ \text{H2} = (3)-32\\ (29) \times (39) - [40) / \\ 0.0045 \times (27D) \times ([\\ (19] or (211 \times 14.50\\ \text{ABMA curve, Chay}\\ \text{From Chapter 10,}\\ \text{Summation [38] th}\\ 0.0024 \times (26D) \times ([\\ 0.0045 \times (27D) \times ([\\ (H at T[4] - H at T[\\ 0.0045 \times (27D) \times ([\\ (H at T[4] - H at T[\\ 100 - [47] - [52] \\ 100 \times (10] / [53] \end{array}$	Table 7 - [3] - [3	4329) x T + 1062.2 3]) 8] 3 4 14, Item [41] 6 [46] 3]) 100 / [18]		0.01	48.0 on output of plan	H@ 80 ~ 1.0	111 C C C C C C C C C C C C C
fuel, as fired Enthalpy of water at T = [3] % % Moisture in air, % Unburned carbon, % Radiation and convection, % 0 Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % 6 Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Guter, % Summation of credits, % Efficiency, % EFFICERORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 Ib/h Fuel rate, 1000 Ib/h	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D) x ([[19] or [21] x 14.50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([(H at T[4] - H at T] Summation [48] th 100 - [47] - [52] 100 x [10] / [53] 1000 x [54] / [18]	Table 7 - [3] - [3	4329) x T + 1062.2 3]) 8] 3 4 14, Item [41] 6 [46] 3]) 100 / [18]		0.01	48.0 on output of plan	H@ 80 ~ 1.0	111 C C C 1 1 1 C C C C C C C C C C C C C
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % if sorbent is used Summation of losses, % Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Wet gas weight, 1000 lb/h	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([(H at T[4] - H at T]; Summation [48] th 100 - [47] - [52] 1000 x [10] / [53] 1000 x [54] / [18] [54] x [33] / 10	- + 0. 100 6] - [(0 / [1 bter 2 7 Table rough 2] - [(3]) x rough	4329) x T + 1062.2 3]) 8] 3 2 14, Item [41] 1 [46] 3]) 100 / [18] 1 [51]		0.01	48.0 on output of plan Furmace 165.3	H@ 80 ~ 1.0	111 0 0 23 -0 0 0 0 0 0 0 0 0 0 0 0 77
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Addiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % if sorbent is used Summation of losses, % Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % Efficiency, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 Ib/h Wet gas weight, 1000 Ib/h Air to burners (wet), Ib/10,000 Btu Hoto Ib/h	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([(H at T[4] - H at T]] Summation [48] th 100 - [47] - [52] 100 x [10] / [53] 1000 x [54] / [18] [54] x (33] / 10 (1 + [7]) x (1 + [25A]	- + 0. 100 6] - [(0 / [1 bter 2 7 Table rough 2] - [(3]) x rough	4329) x T + 1062.2 3]) 8] 3 2 14, Item [41] 1 [46] 3]) 100 / [18] 1 [51]		0.01	48.0 on output of plan Furnace 165.3 4.692	H@ 80 ~ 1.0	111 C C C 1 1 1 C C C C C C C C C C C C C
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Badiation and convection, % Badiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Sorbent net losses, % Summation of losses, % Credits Heat in moisture in air, % Sensible heat in fuel, % Summation of credits, % Efficiency, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 Ib/h Wet gas weight, 1000 Ib/h Air to burners (wet), 100/10,000 Btu	$\begin{array}{l} \text{H1} = (3.958E-5 \times 1\\ \text{H2} = (3)-32\\ $	- + 0. 100 6] - [(1) 0 / [1] Table rough 2] - [(2) 3]) x rough rough - [(1) - [(1) - [(1)] - [(1)]	4329) x T + 1062.2 3]) 8] 3 1 [46] 3]) 100 / [18] 100 / [18] 100 / [18] 100 / [18] 100 / [18]		0.01	48.0 on output of plan Furmace 165.3	H@ 80 ~ 1.0	111 0 0 1 1 1 0 0 0 0 0 0 0 0 0 0 0 0 0
fuel, as fired Enthalpy of water at T = [3] % Moisture in air, % Unburned carbon, % Addiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % if sorbent is used Summation of losses, % Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % Efficiency, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 Ib/h Wet gas weight, 1000 Ib/h Air to burners (wet), Ib/10,000 Btu Hoto Ib/h	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x ([(H at T[4] - H at T]] Summation [48] th 100 - [47] - [52] 100 x [10] / [53] 1000 x [54] / [18] [54] x (33] / 10 (1 + [7]) x (1 + [25A]	- + 0. 100 6] - [(1) 0 / [1 100 / [1 Table rough 2] - [(1) 2] - [(1) 3]) x rough - [1 / 10 0 x [1	4329) x T + 1062.2 3]) 8] 3 14. Item [41] 1 [46] 3]) 100 / [18] 100 / [18] 100 x [22] 7H]) / [18] - 0.005		0.01	48.0 on output of plan Furnace 165.3 4.692	H@ 80 ~ 1.0	111 C C C 1 1 1 C C C C C C C C C C C C C
	Entering air temperature, F Reference temperature, F Fuel temperature, F Fuel temperature leaving air heater, F Flue gas temperature leaving (excluding leakage), F Moisture in air, Ib/Ib dry air Additional moisture, Ib/100 Ib fuel Residue leaving bolier/economizer, % Total Output, 1,000,000 Btu/h (MMBtu/h) Additional theoretical air, Ib/10,000 Btu Table 14, Item [2] CO ₂ from sorbent, Ib/10,000 Btu Table 14, Item [2] Spent sorbent, Ib/10,000 Btu Table 14, Item [24] COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu Theoretical air (corrected), Ib/10,000 Btu Theoretical air (corrected), Ib/10,000 Btu Excess air, % by weight Dry air, Ib/10,000 Btu Additional moisture, Ib/10,000 Btu H ₂ O from fuel, Ib/10,000 Btu H ₂ O from sorbent, Ib/10,000 Btu	Entering air temperature, F 48.19 Reference temperature, F 80 Fuel temperature, F 64 Air temperature, E 64 Air temperature, E 64 Air temperature, leaving air heater, F 409.77 Flue gas temperature leaving (excluding leakage), F 857.90 Moisture in air, Ib/Ib dry air 0.0044 Additional moisture, Ib/100 Ib fuel 0 Residue leaving boiler/economizer, % Total 85 Output, 1,000,000 Btu/h (MMBtu/h) 219.94 Additional theoretical air, Ib/10,000 Btu Table 14, Item [2] 0 CO2, from sorbent, Ib/10,000 Btu Table 14, Item [2] 0 COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu Fuel Input 0 Theoretical air (corrected), Ib/10,000 Btu [2]6] + [21] × 1151/ Residue from fuel, Ib/10,000 Btu [1]6] + [21] × 100 / [18] H ₂ O from fuel, Ib/10,000 Btu [1]6] / 100 / 1[8] H ₂ O from sorbent, Ib/10,000 Btu [1]2] / 100 / [18] H ₂ O from sorbent, Ib/10,000 Btu [1]2] / 12] / 100 / [18] H ₂ O from sorbent, Ib/10,000 Btu [1]3] Total residue, Ib/10,000 Btu [1]2] <	Entering air temperature, F 48.19 Reference temperature, F 80 Air temperature, F 64 Air temperature leaving air heater, F 64 Air temperature leaving (excluding leakage), F 857.90 Moisture in air, Ib/Ib dry air 0.0044 Additional moisture, Ib/100 Ib fuel 0 Residue leaving boiler/economizer, % Total 85 Goutput, 1.000,000 Btu/h (MMBtu/h) 219.94 Additional moisture, Ib/10,000 Btu Table 14, Item [2] 0 Additional moisture, Ib/10,000 Btu Table 14, Item [2] 0 Additional theoretical air, Ib/10,000 Btu Table 14, Item [2] 0 Additional theoretical air, Ib/10,000 Btu 19 Hy Additional theoretical air, Ib/10,000 Btu 19 0 Hy Of rom sorbent, Ib/10,000 Btu 10 20 Spent sorbent, Ib/10,000 Btu [20] - [21] x 1151/[18] 21 COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu [115G] + [21] x 100/[11 100/[11 Total residue, Ib/10,000 Btu [12] x 1151/[18] Ho/[18] HyO from air, Ib/10,000 Btu [12] x 117/[14] x 100/[18] </td <td>Entering air temperature, F 48.19 Constituent Reference temperature, F 80 A C Fuel temperature, F 64 B S Air temperature leaving air heater, F 409.77 C Hz Fue gas temperature leaving (excluding leakage), F 857.90 D HyO Moisture in air, Ib/Ib dry air 0.0044 E Nz Additional moisture, Ib/10 lb fuel 0 F Oz Residue leaving biler/economizer, % Total 85 G Ash Output, 1,000,000 Btu/h (MMBtu/h) 219.94 H Total Additional theoretical air, Ib/10,000 Btu Table 14, Item [2] 0 18 Higher heating value (CO2, from sorbent, Ib/10,000 Btu Table 14, Item [2] 0 20 Theoretical air, Ib/10,00 Spent sorbent, Ib/10,000 Btu Table 14, Item [24] 0 21 Inburned carbon loss COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu [21]-[21] x 1151 / [18] + [11] Residue infortuel, Ib/10,000 Btu [23] + [14] A At Burners 20.5 Dry air, Ib/1</td> <td>Entering air temperature, F 48.19 Constituent % by weight Reference temperature, F 80 A C 29.01 Fuel temperature, F 64 B S 0.05 Air temperature leaving air heater, F 409.77 C H₂ 2.98 Flue gas temperature leaving (excluding leakage), F 857.90 D H_QO 46.02 Moisture in air, Ib/10 dry air 0.0044 E N₂ 0.42 Additional moisture, Ib/10 016 fuel 0 F O₂ 20.35 Residue leaving boiler/economizer, % Total 85 G Ash 1.16 Output, 1,000,000 Btu/ fMB/Bu/h) 219.94 H Total 100.00 Additional theoretical air, Ib/10,000 Btu Table 14, Item [19] 0 19 Unburned carbon loss, % Iuel input H₂O from sorbent, Ib/10,000 Btu Table 14, Item [24] 0 21 Unburned carbon % of fuel COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu [115G] + [21] × 1100 / [18] 111 111 Residue from fuel, Ib/10,000 Btu [12] × 110/ [18]</td> <td>Entering air temperature, F 48.19 Constituent % by weight K1 Reference temperature, F 80 A C 29.01 11.51 Fuel temperature leaving air heater, F 409.77 C H₂ 2.98 34.29 Flue gas temperature leaving (excluding leakage), F 805.700 D H₂O 46.02 Moisture in air, Ib/To dry air 0.0044 E N₂ 0.42 Additional moisture, Ib/100 lb fuel 0 F O₂ 20.35 -4.32 Residue leaving bolic/economizer, % Total 85 G Ash 1.16 Output, 1,000.000 Ash 1.66 Additional moisture, Ib/10,000 Btu Table 14, Item [2] 0 18 Higher heating value (HHV), Btu/lb fuel Oig, from sorbent, Ib/10,000 Btu Ash 1.16 Output, 1,000.000 Btu Asi Si (G) Net (HHV), Btu/lb fuel CO2, from sorbent, Ib/10,000 Btu Table 14, Item [2] 0 18 Higher heating value (HHV), Btu/lb fuel COMBUS/list (G) Si (G) Net (HHV), Btu/lb (D) Si (G) Net (HV), Btu/lb (D)</td> <td>Entering air temperature, F 48.19 Constituent % by weight K1 [15] 1 K1 Reference temperature, F 80 A C 29.01 11.51 333.9 Fuel temperature leaving excluding air teater, F 409.77 C H_a 2.98 34.29 102.3 Fue gas temperature leaving (excluding leakage), F 4857.90 H_bQ_O 46.02</td> <td>Entering air temperature, F 48.19 Consituent % by weight K1 [15] xK1 k2 Reference temperature, F 80 A C 29.01 11.51 333.3 Fuel temperature, F 64 B S 0.05 4.32 0.2 Air temperature leaving excluding leekage), F 807.7 C H₂ 2.98 34.29 102.3 8.94 Plue gas temperature leaving (excluding leekage), F 807.0 0.004 E N₂ 0.46.02 0.00 Moisture in air, bi/b dry air 0.0044 E N₂ 0.42 0.42 0.00 Moisture in air, bi/b dry air 0.0044 E N₂ 0.42 0.00 Moisture in air, bi/b dry air 0.004 E N₂ 0.42 0.00 Moisting blanceconomizer, % Total 85 G.Ash 1.16 0.00 Moisting blanceconomizer, % Total 0.02 1.00 1.00 Air 348.5 H₂O Additional theoretical air, bi/10.000 Btu Table 14, Item [2] 0 18 Higher heating value (HHV), Bu/b fuel</td>	Entering air temperature, F 48.19 Constituent Reference temperature, F 80 A C Fuel temperature, F 64 B S Air temperature leaving air heater, F 409.77 C Hz Fue gas temperature leaving (excluding leakage), F 857.90 D HyO Moisture in air, Ib/Ib dry air 0.0044 E Nz Additional moisture, Ib/10 lb fuel 0 F Oz Residue leaving biler/economizer, % Total 85 G Ash Output, 1,000,000 Btu/h (MMBtu/h) 219.94 H Total Additional theoretical air, Ib/10,000 Btu Table 14, Item [2] 0 18 Higher heating value (CO2, from sorbent, Ib/10,000 Btu Table 14, Item [2] 0 20 Theoretical air, Ib/10,00 Spent sorbent, Ib/10,000 Btu Table 14, Item [24] 0 21 Inburned carbon loss COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu [21]-[21] x 1151 / [18] + [11] Residue infortuel, Ib/10,000 Btu [23] + [14] A At Burners 20.5 Dry air, Ib/1	Entering air temperature, F 48.19 Constituent % by weight Reference temperature, F 80 A C 29.01 Fuel temperature, F 64 B S 0.05 Air temperature leaving air heater, F 409.77 C H ₂ 2.98 Flue gas temperature leaving (excluding leakage), F 857.90 D H _Q O 46.02 Moisture in air, Ib/10 dry air 0.0044 E N ₂ 0.42 Additional moisture, Ib/10 016 fuel 0 F O ₂ 20.35 Residue leaving boiler/economizer, % Total 85 G Ash 1.16 Output, 1,000,000 Btu/ fMB/Bu/h) 219.94 H Total 100.00 Additional theoretical air, Ib/10,000 Btu Table 14, Item [19] 0 19 Unburned carbon loss, % Iuel input H ₂ O from sorbent, Ib/10,000 Btu Table 14, Item [24] 0 21 Unburned carbon % of fuel COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu [115G] + [21] × 1100 / [18] 111 111 Residue from fuel, Ib/10,000 Btu [12] × 110/ [18]	Entering air temperature, F 48.19 Constituent % by weight K1 Reference temperature, F 80 A C 29.01 11.51 Fuel temperature leaving air heater, F 409.77 C H ₂ 2.98 34.29 Flue gas temperature leaving (excluding leakage), F 805.700 D H ₂ O 46.02 Moisture in air, Ib/To dry air 0.0044 E N ₂ 0.42 Additional moisture, Ib/100 lb fuel 0 F O ₂ 20.35 -4.32 Residue leaving bolic/economizer, % Total 85 G Ash 1.16 Output, 1,000.000 Ash 1.66 Additional moisture, Ib/10,000 Btu Table 14, Item [2] 0 18 Higher heating value (HHV), Btu/lb fuel Oig, from sorbent, Ib/10,000 Btu Ash 1.16 Output, 1,000.000 Btu Asi Si (G) Net (HHV), Btu/lb fuel CO2, from sorbent, Ib/10,000 Btu Table 14, Item [2] 0 18 Higher heating value (HHV), Btu/lb fuel COMBUS/list (G) Si (G) Net (HHV), Btu/lb (D) Si (G) Net (HV), Btu/lb (D)	Entering air temperature, F 48.19 Constituent % by weight K1 [15] 1 K1 Reference temperature, F 80 A C 29.01 11.51 333.9 Fuel temperature leaving excluding air teater, F 409.77 C H _a 2.98 34.29 102.3 Fue gas temperature leaving (excluding leakage), F 4857.90 H _b Q_O 46.02	Entering air temperature, F 48.19 Consituent % by weight K1 [15] xK1 k2 Reference temperature, F 80 A C 29.01 11.51 333.3 Fuel temperature, F 64 B S 0.05 4.32 0.2 Air temperature leaving excluding leekage), F 807.7 C H₂ 2.98 34.29 102.3 8.94 Plue gas temperature leaving (excluding leekage), F 807.0 0.004 E N₂ 0.46.02 0.00 Moisture in air, bi/b dry air 0.0044 E N₂ 0.42 0.42 0.00 Moisture in air, bi/b dry air 0.0044 E N₂ 0.42 0.00 Moisture in air, bi/b dry air 0.004 E N₂ 0.42 0.00 Moisting blanceconomizer, % Total 85 G.Ash 1.16 0.00 Moisting blanceconomizer, % Total 0.02 1.00 1.00 Air 348.5 H₂O Additional theoretical air, bi/10.000 Btu Table 14, Item [2] 0 18 Higher heating value (HHV), Bu/b fuel

_	NPUT CONDITIONS - BY TEST OR SPECIFICATION			FUEL - Subbituminous (Coal. Minnesota	1			
1	Excess air: at burner/leaving boiler/econ, % by weight	22.9		15 Ultimate Analysis			lb/100 lb fuel	17 H ₂ O, lb/1	00 lb fuel
2	Entering air temperature, F	47.82	-	Constituent	% by weight	K1	[15] x K1	K2	[15] x K2
3	Reference temperature, F	47.02	Α	C	29.42	11.51	338.6	TK2	[15] X 12
4	Fuel temperature, F	64	В	S	0.04	4.32	0.2		
5	Air temperature leaving air heater, F	400.57	С	H ₂	2.87	34.29	98.3	8.94	25
6	Flue gas temperature leaving (excluding leakage), F	874.18	D	H ₂ O	44.65			1.00	44
7	Moisture in air, Ib/Ib dry air	0.0055	E	N ₂	0.44			1.00	
· .			_	-		4.00	00.0		
8	Additional moisture, Ib/100 lb fuel	0	F	0 ₂	20.79	-4.32	-89.8		
9 10	Residue leaving boiler/economizer, % Total Output, 1,000,000 Btu/h (MMBtu/h)	85	G	Ash	1.79 100.00	Air	247.0	1100	70
10		220.06	н	Total	100.00	Alf	347.3	H2O	70
11	Additional theoretical air, lb/10,000 Btu Table 14, Item [2	0	18	Higher heating value	HHV) Btu/lb fu	ما			8,9
12	CO ₂ from sorbent, lb/10,000 Btu Table 14, Item [19]	0	19	Unburned carbon loss		ei			0,3
_		0	_				[40] II 400 /	[4.0]	
13 14	H ₂ O from sorbent, lb/10,000 Btu Table 14, Item [20]		20	Theoretical air, lb/10,0			[16H] x 100 /		3.8
14	Spent sorbent, lb/10,000 Btu Table 14, Item [24]	0	21	Unburned carbon, %	offuel		[19] x [18] / 14	4,500	0.
(COMBUSTION GAS CALCULATIONS, Quantity/10,000 Btu	I Fuel Input							
22	Theoretical air (corrected), lb/10,000 Btu	[20] - [21] x 1151 /							3.871
23	Residue from fuel, Ib/10,000 Btu	([15G] + [21]) x 10	U / [1	8]					0.022
24	Total residue, lb/10,000 Btu	[23] + [14]	•	At Purpore	D Infiltration		urpaga		0.022 Bir/Econ
25	Excess air, % by weight		A	At Burners 22.9	B Infiltration 0.0	C Leaving I	-urnace 22.9	D Leaving	Bir/Econ 22.9
25 26	Dry air, lb/10,000 Btu	(1 + [25] / 100) x [2	221	22.9	0.0		4.756		4.7
27	H ₂ O from air, lb/10,000 Btu	[26] x [7]	[2]			0.026	0.026	0.026	4.7
28									
28 29	Additional moisture, Ib/10,000 Btu	[8] x 100 / [18]				0.000	0.000	0.000 0.789	0.0
	H ₂ O from fuel, lb/10,000 Btu	[17H] x 100 / [18]		0 / [40]		0.789	1.400	0.789	
30	Wet gas from fuel, lb/10,000 Btu	(100 - [15G] - [21])	X IU	JU / [18]			1.100		1.1
31	CO ₂ from sorbent, lb/10,000 Btu	[12]					0.000		0.0
32	H ₂ O from sorbent, lb/10,000 Btu	[13]				0.000	0.000	0.000	0.0
33	Total wet gas, Ib/10,000 Btu	Summation [26] th					5.882		5.8
34	Water in wet gas, Ib/10,000 Btu	Summation [27] +	[28] -	+ [29] + [32]		0.815	0.815	0.815	0.8
35	Dry gas, lb/10,000 Btu	[33] - [34]					5.067		5.0
36	H ₂ O in gas, % in weight	100 x [34] / [33]					13.85		13.
37	Residue, % by weight (zero if < 0.15 lbm/10KB)	[9] x [24] / [33]					0.32		0.
	EFFICIENCY CALCULATIONS, % Input from Fuel								
	EFFICIENCY CALCULATIONS, % Input from Fuel Losses								
838	Losses Dry Gas, %	0.0024 x [35d] x ([4				1			9
38 39	Losses Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6]	H1 = (3.958E-5 x 7		3]) .4329) x T + 1062.2			1470.9		
38 39 40	Losses Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired Enthalpy of water at T = [3]	H1 = (3.958E-5 x H2 = [3] -32	Γ+0	.4329) x T + 1062.2			1470.9 48.0		9.
38 39 40 41	Losses Dry Gas, % Water from Enthalpy of steam at 1 psi, T = [6] fuel, as fired %	H1 = (3.958E-5 x H2 = [3] -32 [29] x ([39] - [40]) /	Г + 0 100	.4329) x T + 1062.2					9.
38 39 40 41 42	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, %	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([Г + 0 100 6] - [.4329) x T + 1062.2 3])					9 11, 0,
38 39 40 41 42 43	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, %	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50	Γ + 0 100 6] - [00 / [⁻	.4329) x T + 1062.2 3]) 18]			48.0	- Di <i>1</i> -	9 111 0. 0.
38 39 40 41 42 43 44	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, %	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([Γ + 0 100 6] - [00 / [⁻	.4329) x T + 1062.2 3]) 18]		based		it Btu/h	9. 111. 0. 0. 0.
38 39 40 41 42 43 44 45	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable)	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap	F + 0 100 6] - [00 / [oter 2	.4329) x T + 1062.2 3]) 18] 23		basec	48.0	it Btu/h	9. 11. 0. 0. 1. 1.
38 39 40 41 42 43 44 45 46	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap From Chapter 10,	F + 0 100 6] - [00 / [oter 2	.4329) x T + 1062.2 3]) 18] 23 e 14, Item [41]		based	48.0	it Btu/h	9 111. 0. 0. 1. 1. 0. 0.
38 39 40 41 42 43 44 45 46	Losses Dry Gas, % Water from Finthalpy of steam at 1 psi, T = [6] fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, %	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap	F + 0 100 6] - [00 / [oter 2	.4329) x T + 1062.2 3]) 18] 23 e 14, Item [41]		basec	48.0	it Btu/h	9. 11. 0. 0. 1. 1.
38 39 40 41 42 43 44	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap From Chapter 10,	F + 0 100 6] - [00 / [00 / [Tabl roug	.4329) x T + 1062.2 3]) 18] 23 e 14, Item [41] h [46]		basec	48.0	it Btu/h	9 111. 0. 0. 1. 1. 0. 0.
38 39 40 41 42 43 44 45 46 47 48	Losses Dry Gas, % Water from Finthalpy of steam at 1 psi, T = [6] fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, %	H1 = (3.958E-5 x H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,5C ABMA curve, Chap From Chapter 10, Summation [38] th	Γ + 0 100 6] - [00 / [0] [0] [0] [0] [.4329) x T + 1062.2 3]) 18] 23 e 14, Item [41] h [46] 3])		based	48.0	it Btu/h	9 111 0 0 1 1 1 0 2 3
38 39 40 41 42 43 44 45 46 47 48 49	Losses Dry Gas, % Water from Finhalpy of steam at 1 psi, T = [6] Finhalpy of water at T = [3] Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % fs orbent is used Summation of losses, % Credits Heat in dry air, %	H1 = (3.958E-5 x 1 H2 = (332 [29] x ((39] - (40)) / 0.0045 x (27D] x (([19] or [21] x 14,5C ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([[+ 0 [100 [6] - [[0 / [[0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 / []0 /	.4329) x T + 1062.2 3]) 18] 23 e 14, Item [41] h [46] 3])		basec	48.0	t Btu/h H @ 80 ∼ 1.0	9 111 0 1 1 1 1 1 1 2 3 -0 0 0 0 0
38 39 40 41 42 43 44 45 46 47 48 49 50	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbert net losses, % fi sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, %	H1 = (3.958E-5 x + H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x (([19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ((0.0045 x [27D] x (((H at T[4] - H at T[F + 0 100 6] - [00 / [0] [00 / [0]] 0 / [0] [0 / [0]] 0 / [0]]	4329) x T + 1062.2 3]) 8] 23 e 14, Item [41] h [46] 3]) 3]) 100 / [18]			48.0		9. 111. 0. 0. 1. 1. 1. 0. 23. -0. 0. 0.
8 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, %	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chag From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x (] (H at T[4] - H at T[Summation [48] th	F + 0 100 6] - [00 / [0] [00 / [0]] 0 / [0] [0 / [0]] 0 / [0]]	4329) x T + 1062.2 3]) 8] 23 e 14, Item [41] h [46] 3]) 3]) 100 / [18]			48.0		9 111. 0 0 1 1 1 2 3 2 3 2 3 0 0 0 0 0 0 0 0 0 0 0 0 0 0
8 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbert net losses, % fi sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, %	H1 = (3.958E-5 x + H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x (([19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ((0.0045 x [27D] x (((H at T[4] - H at T[F + 0 100 6] - [00 / [0] [00 / [0]] 0 / [0] [0 / [0]] 0 / [0]]	4329) x T + 1062.2 3]) 8] 23 e 14, Item [41] h [46] 3]) 3]) 100 / [18]			48.0		9 111. 0 0 11. 1. 1. 1. 0 23. 23. 0 0 0 0 0 0 0 0 0 0 0
38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, % Aadiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chag From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x (] (H at T[4] - H at T[Summation [48] th	F + 0 100 6] - [00 / [0] [00 / [0]] 0 / [0] [0 / [0]] 0 / [0]]	4329) x T + 1062.2 3]) 8] 23 e 14, Item [41] h [46] 3]) 3]) 100 / [18]		0.01	48.0	H@80~1.0	9 111. 0 0 1 1 1 2 3 2 3 2 3 0 0 0 0 0 0 0 0 0 0 0 0 0 0
38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53	Losses Dry Gas, % Water from Finhalpy of steam at 1 psi, T = [6] Finhalpy of water at T = [3] Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, %	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chag From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x (] (H at T[4] - H at T[Summation [48] th	F + 0 100 6] - [00 / [0] [00 / [0]] 0 / [0] [0 / [0]] 0 / [0]]	4329) x T + 1062.2 3]) 8] 23 e 14, Item [41] h [46] 3]) 3]) 100 / [18]		0.01	48.0	H@80~1.0	9 9 111 0 0 11 1 1 1 1 0 23 23 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
838 39 40 41 42 43 44 45 44 45 46 47 48 49 50 51 52 53 6 7 7 7 7 7 7 7 7 7 7 7 7 7	Losses Dry Gas, % Water from fuel, as fired % Moisture in air, % Unburned carbon, % Aadiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x (] (H at T[4] - H at T[Summation [48] th 100 - [47] - [52]	F + 0 100 6] - [00 / [0] [00 / [0]] 0 / [0] [0 / [0]] 0 / [0]]	4329) x T + 1062.2 3]) 8] 23 e 14, Item [41] h [46] 3]) 3]) 100 / [18]		0.01	48.0	H@80~1.0	9 111 0 0 1 1 1 0 0 2 3 3 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
38 39 40 41 42 43 44 45 44 45 44 49 50 51 52 53	Losses Dry Gas, % Water from fuel, as fired Enthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in moisture in air, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x (1 [19] or [21] x 14,50 ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x (] (H at T[4] - H at T[Summation [48] th 100 - [47] - [52] 1000 x [10] / [53] 1000 x [54] / [18] [54] x [33] / 10	F + 0 100 6] - [00 / [00 / [100 / [10	.4329) x T + 1062.2 3]) 18] 23 e 14, Item [41] h [46] 3]) 100 / [18] h [51]		0.01	48.0 I on output of plan	H@80~1.0	9 11:1 0 0 1 1 1 0 1 23 -0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
338 339 40 41 42 43 44 45 46 47 48 49 50 51 52 53 53 6 54 55 56 57	Losses Dry Gas, % Water from fuel, as fired Tenthalpy of steam at 1 psi, T = [6] % Moisture in air, % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % Credits Heat in dry air, % Heat in dry air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 Ib/h Wet gas weight, 1000 Ib/h Air to burners (wet), Ib/10,000 Btu	H1 = (3.958E-5 x] H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x ([[19] or [21] x 14,55 ABMA curve, Chag From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x (] (H at T[4] - H at T[Summation [48] th 100 - [47] - [52] 100 x [10] / [53] 1000 x [54] / [18] [54] x [33] / 10 (1 + [7]) x (1 + [25A	F + 0 100 6] - [00 / [00 / [00 / [100	.4329) x T + 1062.2 3]) 18] 23 e 14, Item [41] h [46] 3]) 100 / [18] h [51]		0.01	48.0 I on output of plan g Furnace 168.0 4.782	H@80~1.0	9 111 0 0 11 1 1 1 1 1 0 0 0 0 0 0 0 0 0
38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58	Losses Dry Gas, % Water from Finhalpy of steam at 1 psi, T = [6] Finhalpy of water at T = [3] Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbert net losses, % Credits Heat in for air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % EY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Air to burners (wet), 1b/10,000 Btu Air to burners (wet), 1000 lb/h	$\begin{array}{l} \text{H1} = (3.958E-5 \times 1) \\ \text{H2} = (3)-32 \\ \text{H3} = $	F + 0 7 100 6] - [00 / [00 / [100 / [1	.4329) x T + 1062.2 3)) 18] 23 e 14, Item [41] h [46] 3]) 100 / [18] h [51] 200) x [22]		0.01	48.0 I on output of plan	H@80~1.0	9 111 0 0 11 1 1 1 1 1 0 0 0 0 0 0 0 0 0
38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57	Losses Dry Gas, % Water from fuel, as fired Enthalpy of steam at 1 psi, T = [6] Enthalpy of water at T = [3] % Unburned carbon, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbent net losses, % if sorbent is used Summation of losses, % Credits Heat in dry air, % Heat in dry air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % KEY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Wet gas weight, 1000 lb/h Air to burners (wet), lb/10,000 Btu Air to burners (wet), 0b/10,000 Btu/h	H1 = (3.958E-5 x 1 H2 = [3] -32 [29] x ([39] - [40]) / 0.0045 x [27D] x (1 [19] or [21] x 14,5C ABMA curve, Chap From Chapter 10, Summation [38] th 0.0024 x [26D] x ([0.0045 x [27D] x (] (H at T[4] - H at T[Summation [48] th 100 - [47] - [52] 1000 x [10] / [53] 1000 x [54] / [18] [54] x [33] / 10 (1 + [7]) x (1 + [25A [54] x ([31] / 10.33]	F + 0 7 100 6] - [00 / [00 / [00 / [100 / [10	.4329) x T + 1062.2 3]) 18] 23 24 16 [46] 100 / [18] 100 / [18] 100 / [18] 100 × [22] 7H]) / [18] - 0.005		0.01	48.0 I on output of plan g Furnace 168.0 4.782	H@80~1.0	9 111 0 0 11 1 1 1 1 1 0 0 0 0 0 0 0 0 0
38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58	Losses Dry Gas, % Water from Finhalpy of steam at 1 psi, T = [6] Finhalpy of water at T = [3] Moisture in air, % Unburned carbon, % Radiation and convection, % Radiation and convection, % Radiation and convection, % Other, % (include manufacturers margin if applicable) Sorbert net losses, % Credits Heat in for air, % Heat in moisture in air, % Sensible heat in fuel, % Other, % Summation of credits, % Efficiency, % EY PERFORMANCE PARAMETERS Input from fuel, 1,000,000 Btu/h Fuel rate, 1000 lb/h Air to burners (wet), 1b/10,000 Btu Air to burners (wet), 1000 lb/h	$\begin{array}{l} \text{H1} = (3.958E-5 \times 1) \\ \text{H2} = (3)-32 \\ \text{H3} = $	F + 0 7 100 6] - [00 / [00 / [00 / [100 / [10	.4329) x T + 1062.2 3]) 18] 23 24 16 [46] 100 / [18] 100 / [18] 100 / [18] 100 × [22] 7H]) / [18] - 0.005		0.01	48.0 I on output of plan g Furnace 168.0 4.782	H@80~1.0	9 111 0 0 11 1 1 1 1 1 0 0 0 0 0 0 0 0 0

Appendix D

Wood Based Fuel Deliveries for Rapids Energy (1/1/2007 – 6/30/2007

Southern Research Institute/USEPA April 2008

REC Wood Burn 01/01 to 06/30, 2007

VENDOR	TYPE	Total Lbs Delivered	Number of Trips	Tons Delivered	Tons/Trip	Miles From REC	gal fuel used	CO2 emitted (ton)
Ainsworth Bemidji	Bark	14,208,802	336	7,104	21.1	69	3567	35
B Nelson	Bark	3,734,940	87	1,867	21.5	116	1553	15
Cass Forest Products	Bark	6,489,660	138	3,245	23.5	53	1125	11
Cook Logging	Bark	1,310,720	24	655	27.3	40	148	1
Covington Trucking	Bark	3,636,560	76	1,818	23.9	80	935	9
Dick Walsh Forest					-			
Product	Bark	35,298,778	618	17,649	28.6	85	8082	79
Dukek Logging	Bark	10,371,620	205	5,186	25.3	95	2996	29
Erickson Mills	Chips	303,320	6	152	25.3	75	69	1
Erickson Mills	Shredded	4,022,480	78	2,011	25.8	75	900	9
Erickson Timber	Bark	12,666,820	230	6,333	27.5	131	4635	45
Hi Tech Milling	Chips	5,147,680	105	2,574	24.5	26	420	4
Northland Biomass	Bark	8,489,580	190	4,245	22.3	5	146	1
J&A Logging	Chips	552,800	12	276	23.0	48	89	1
Lonza	Bark	1,702,864	54	851	15.8	5	42	0
MR Chips	Blandin	8,741,840	163	4,371	26.8	0	0	0
MR Chips	Private	11,479,260	199	5,740	28.8	0	0	0
Muller Trucking	Bark	770,300	15	385	25.7	53	122	1
Norbord Minnesota	Bark	3,551,400	80	1,776	22.2	82	1009	10
Potlatch Lumber Co	Bark	24,731,240	465	12,366	26.6	69	4936	48
Rajala Mill	Bark	941,220	28	471	16.8	40	172	2
Rajala Mill	Chips	2,935,060	70	1,468	21.0	40	431	4
Rajala Mill	Shredded	42,160	1	21	21.1	40	6	0
Rajala Timber Co	Bark	11,697,800	259	5,849	22.6	14	558	5
Scheff Logging	Bark	3,478,670	75	1,739	23.2	29	335	3
Wagner Forest Products	Bark	3,381,740	65	1,691	26.0	26	260	3
Total				89,844			32,536	318
Blandin				82,881				

Total Wood Burn

172,725

Appendix E

Dust Collector and Electrostatic Precipitator Data

Southern Research Institute/USEPA April 2008

Run ID	Dust Collector Pressure Drop (in. wc)	Panel A Voltage	Panel B Voltage	Panel C Voltage
1	-5.2	268	274	324
2	-5.2	276	308	335
3	-4.8	286	338	336
4	-8.4	287	372	335
5	-6.9	280	373	345
6	-7.4	285	370	347

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Summary of Electrostatic P	recipitator	Voltages and Dr	ist Collector P	ressure Drop
Summary of Electrostatic I	recipitator	, onuges and De		ressure prop