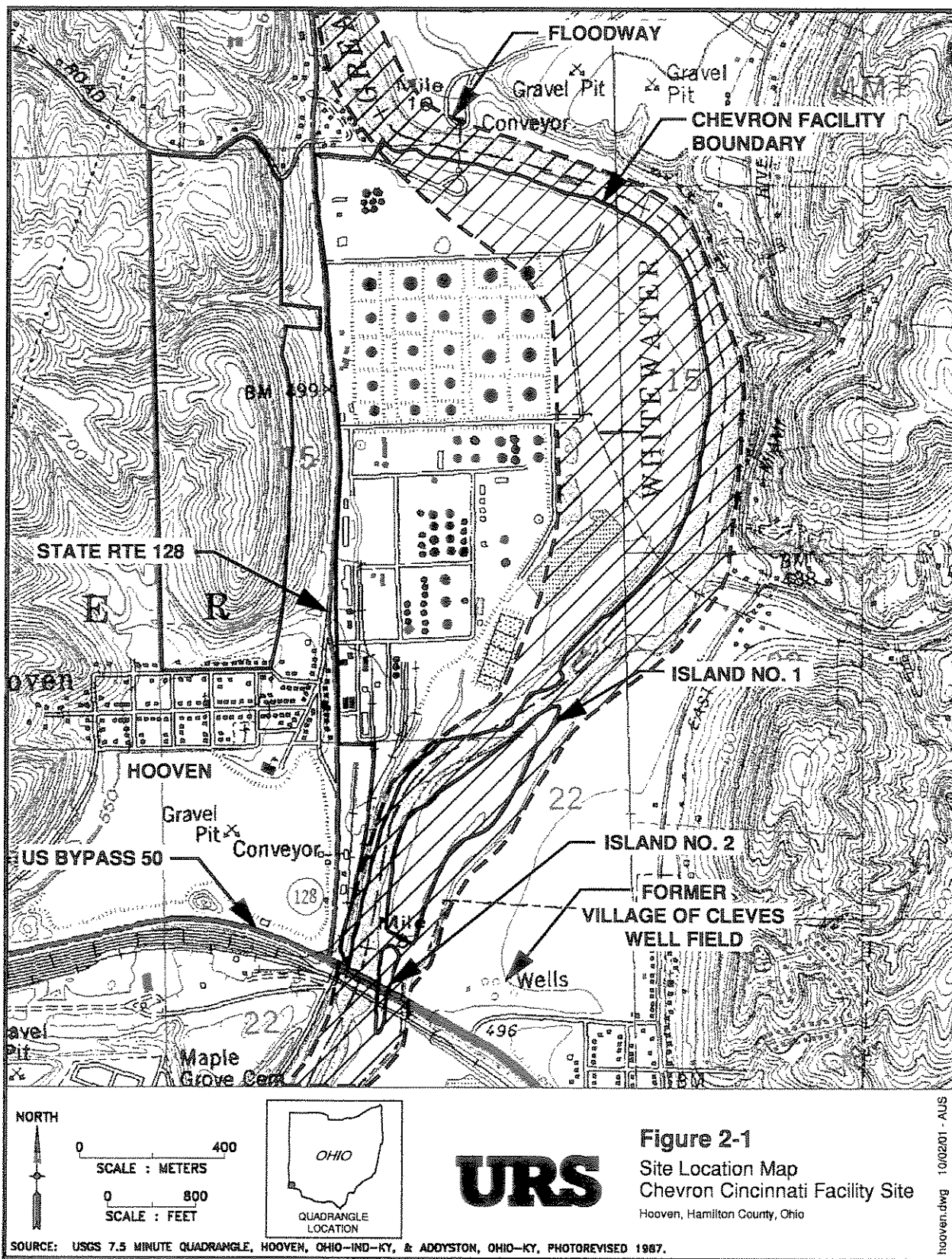


US EPA ARCHIVE DOCUMENT



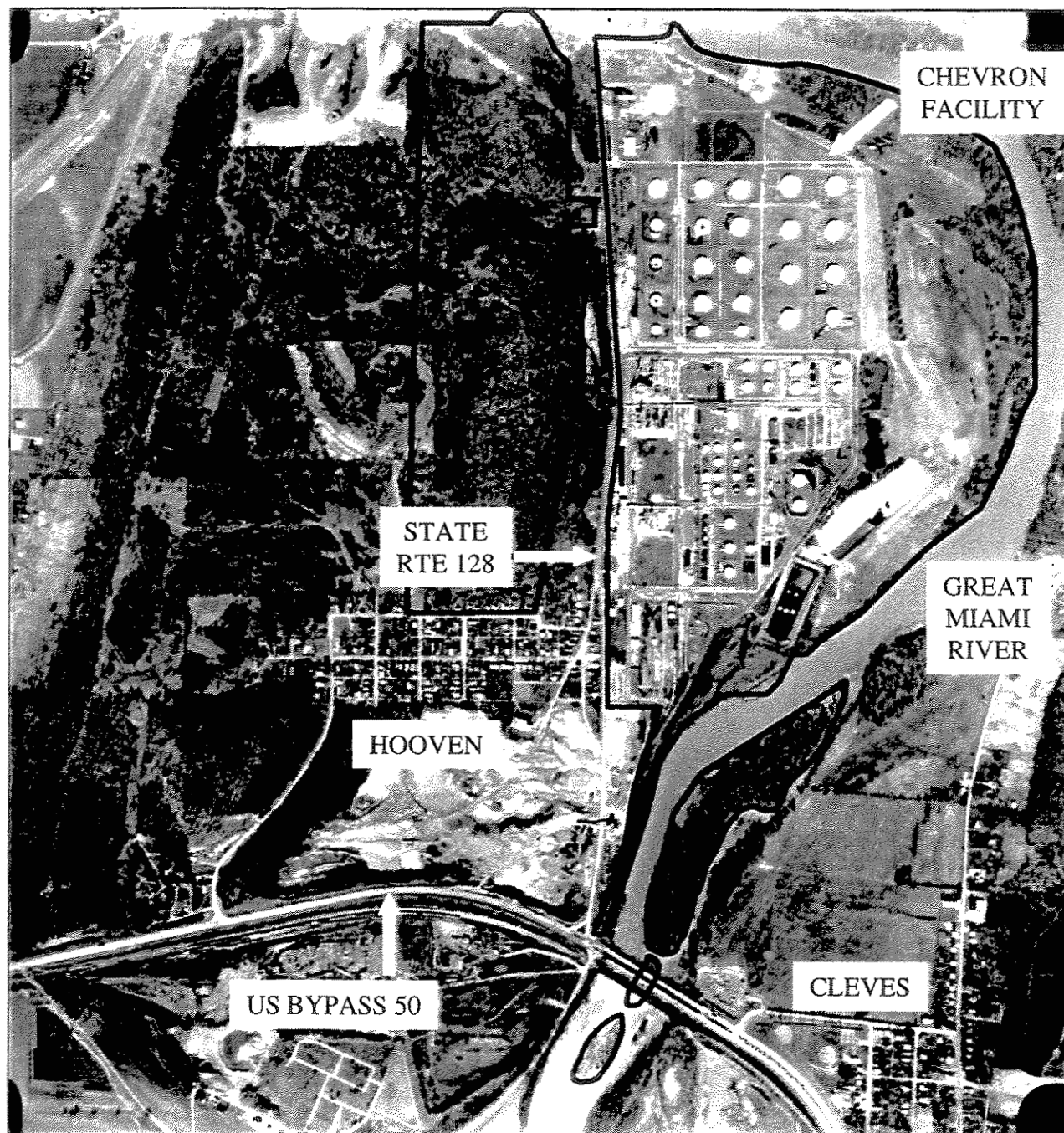
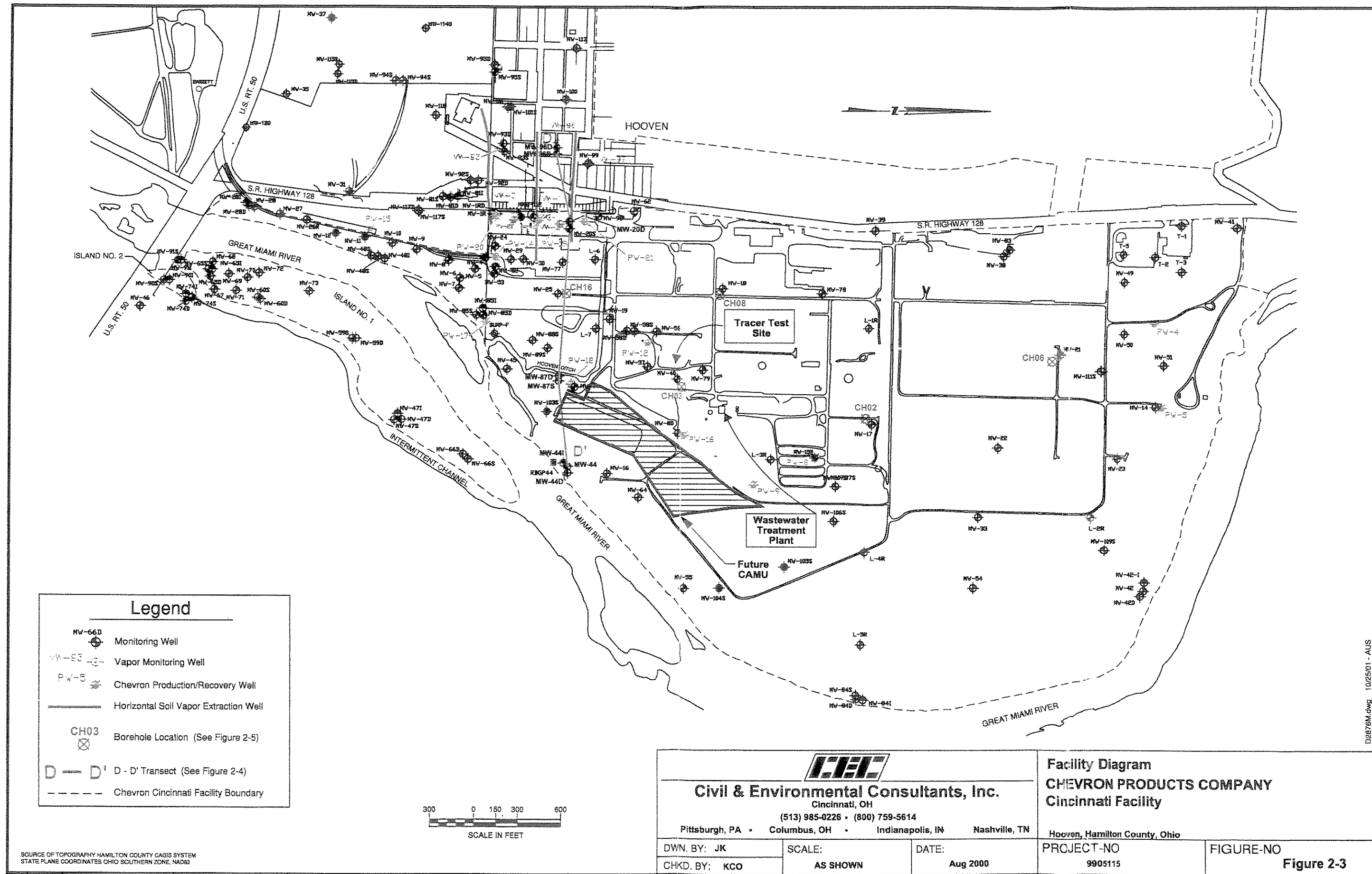
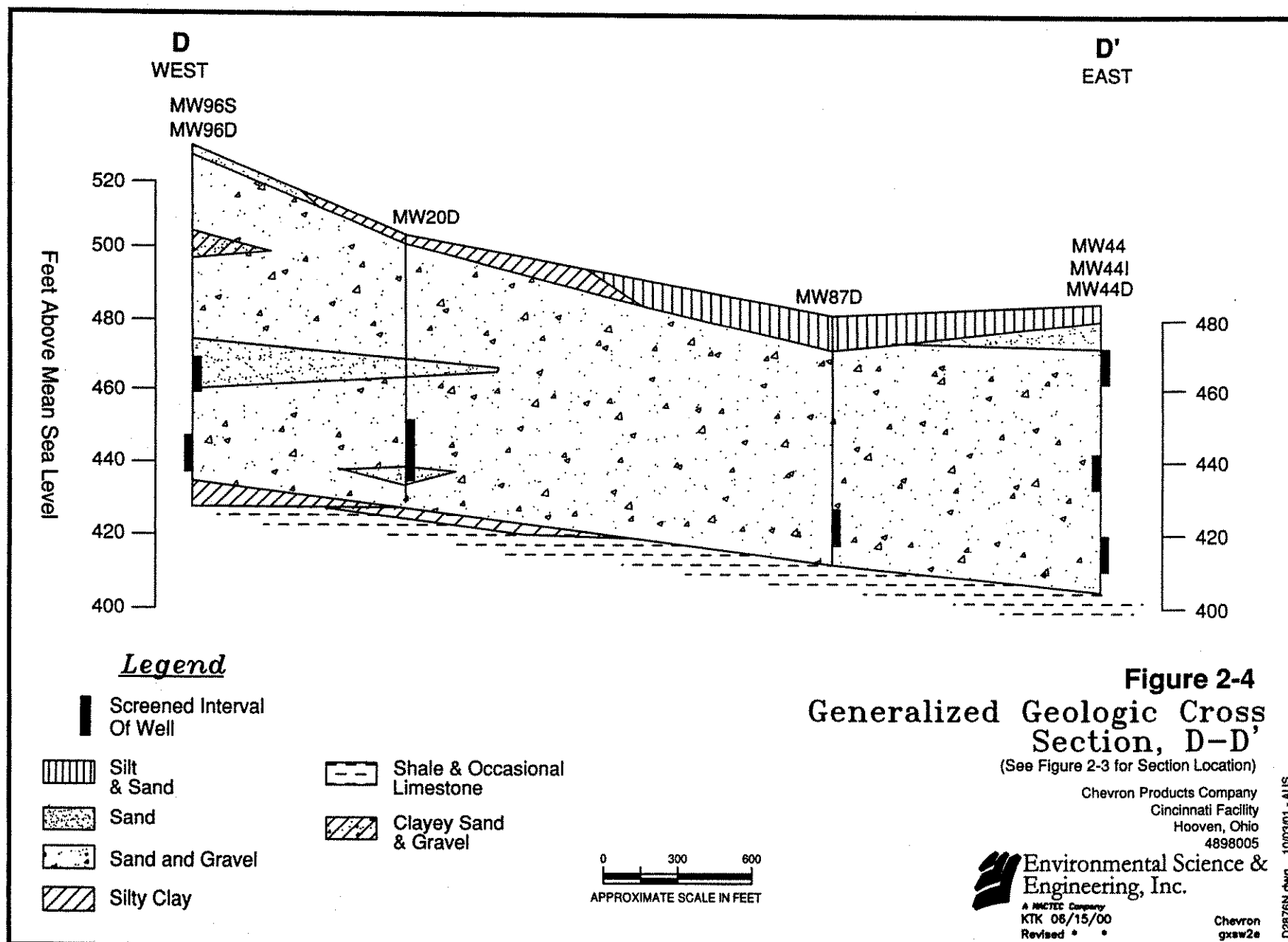


Figure 2-2
 Aerial Photograph of the Chevron Cincinnati Facility in March 1975.
 Most above grade structures were removed after 1986.





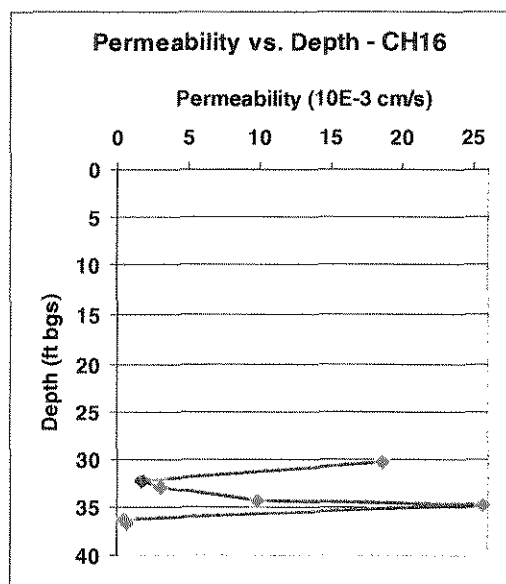
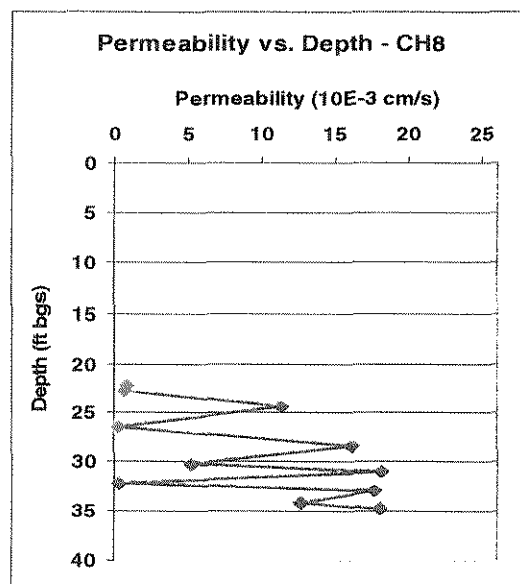
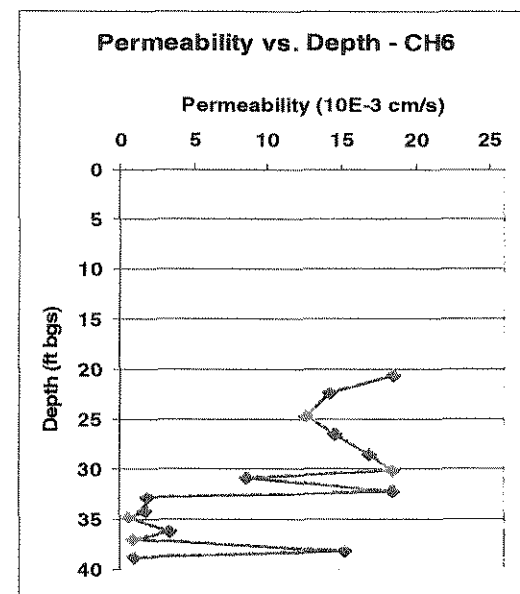
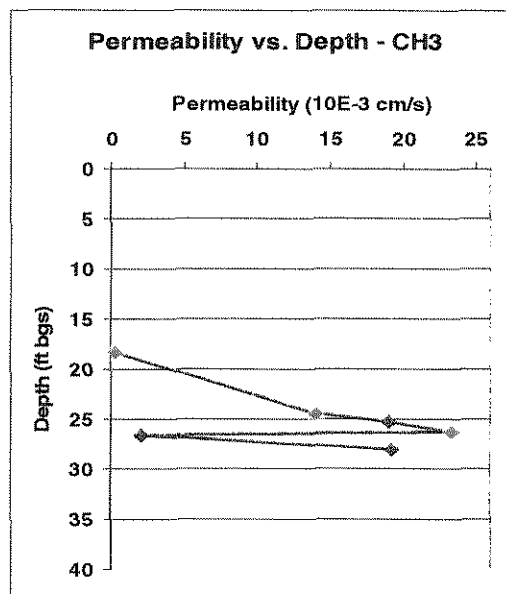
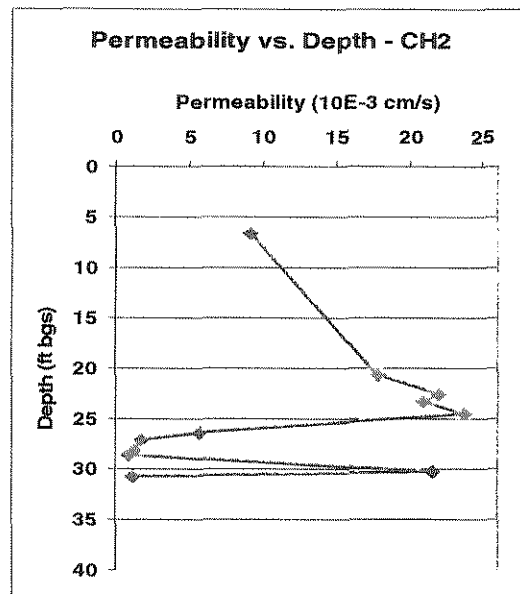


Figure 2-5
Permeability versus Depth
from Borings CH2 - CH16.
(see Figure 2-3
for boring locations)

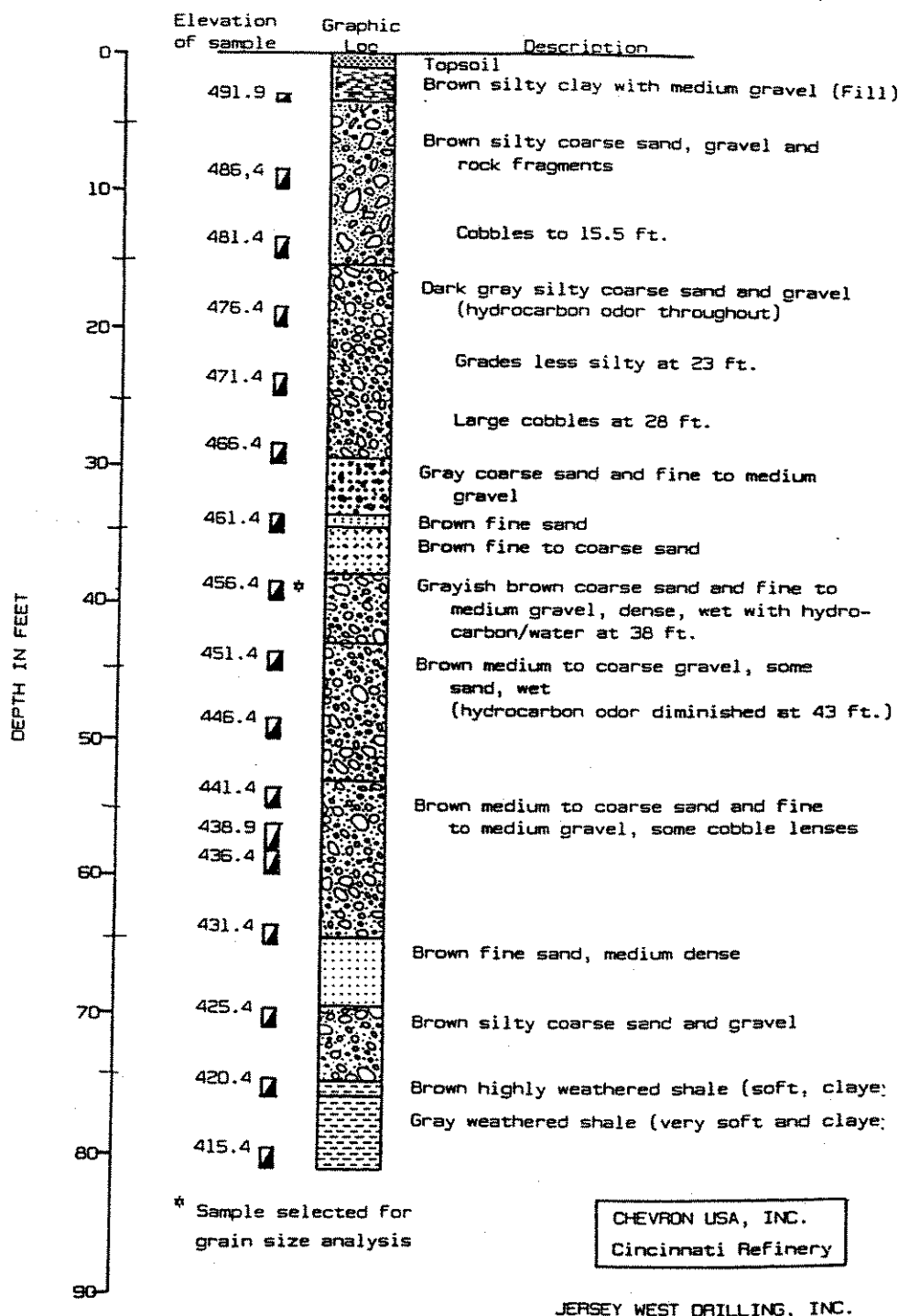
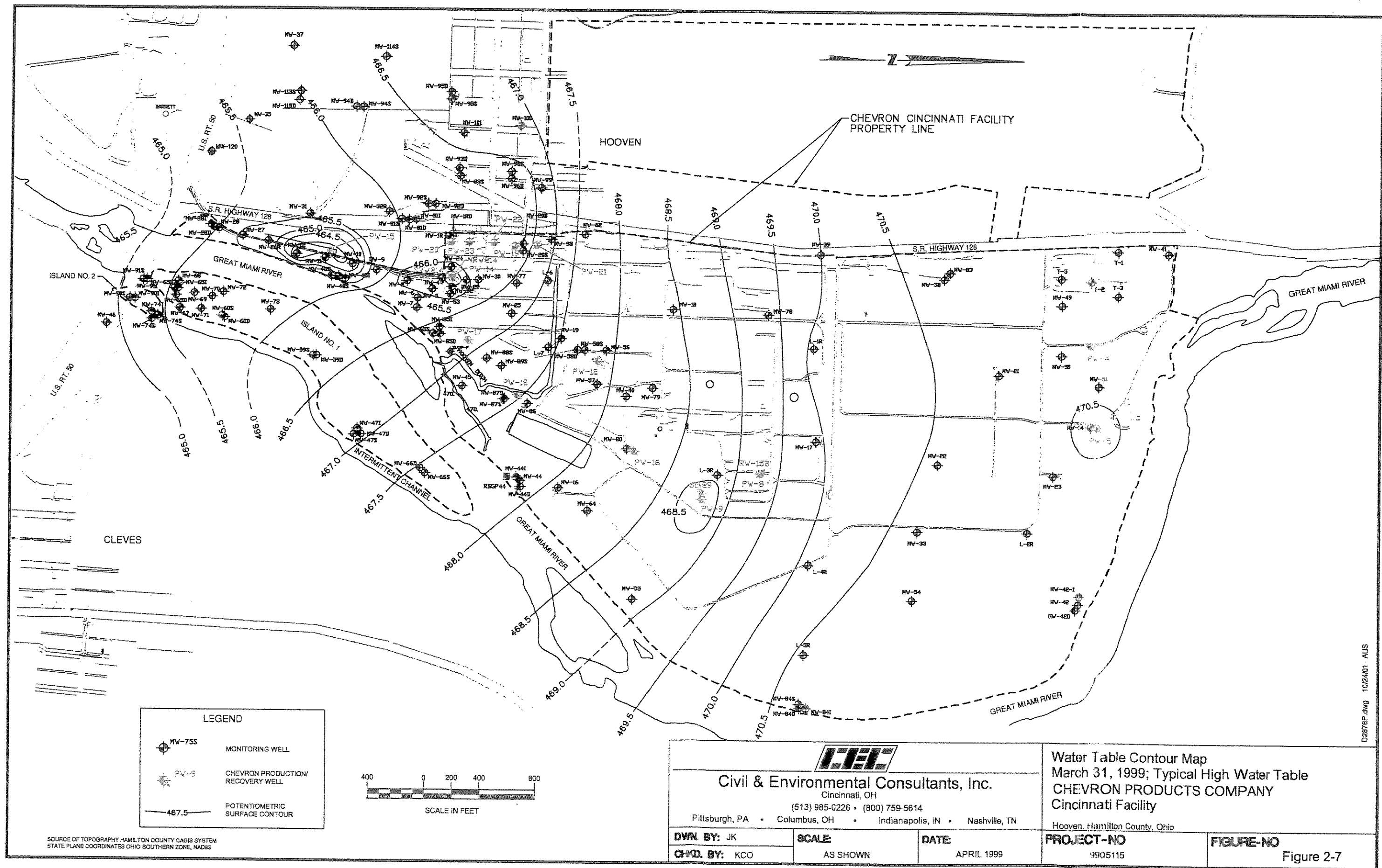
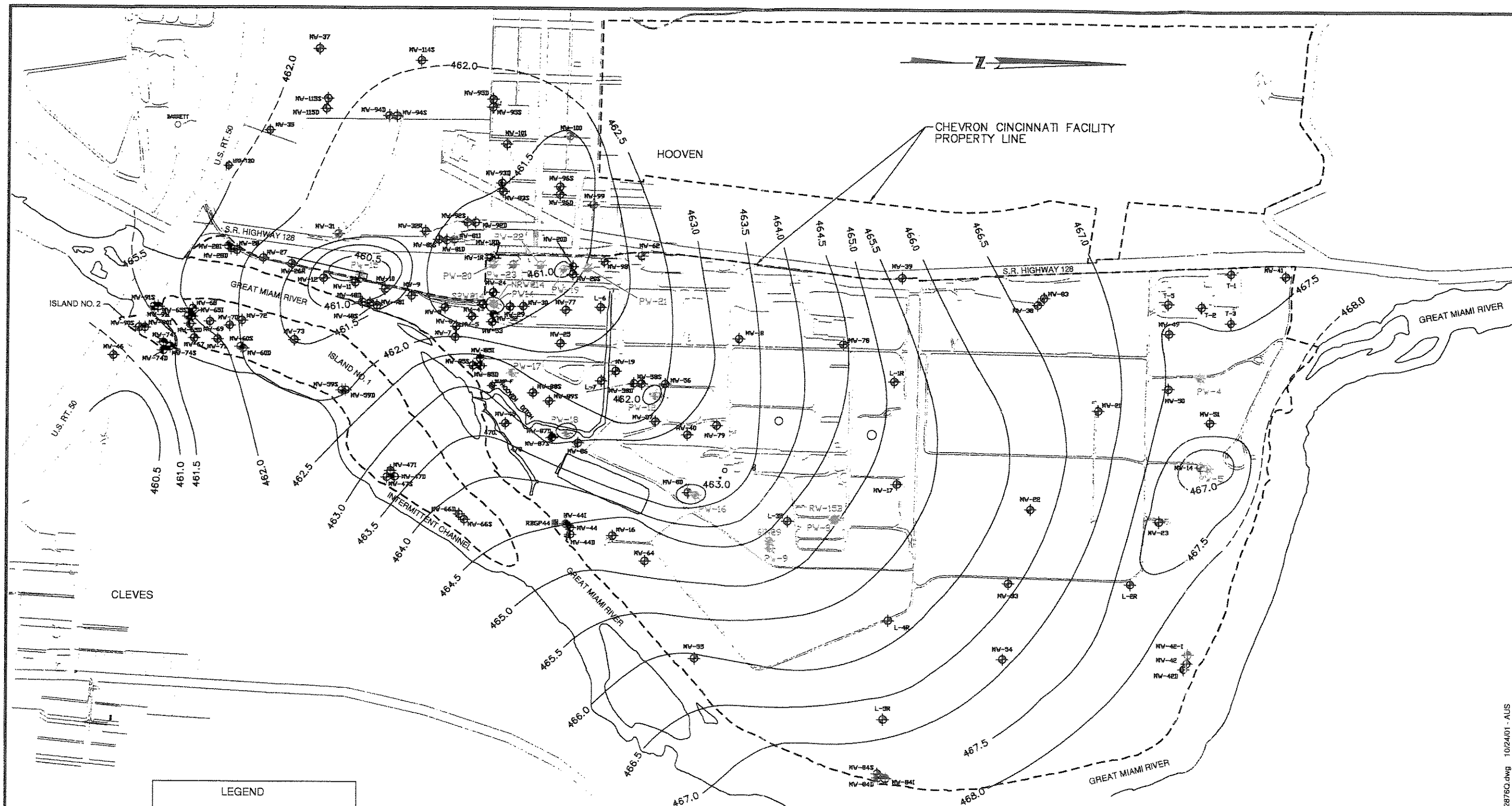


Figure 2-6
Lithology Log of MW-20D



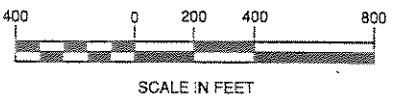


LEGEND


MV-75S MONITORING WELL

PW-9 CHEVRON PRODUCTION/RECOVERY WELL

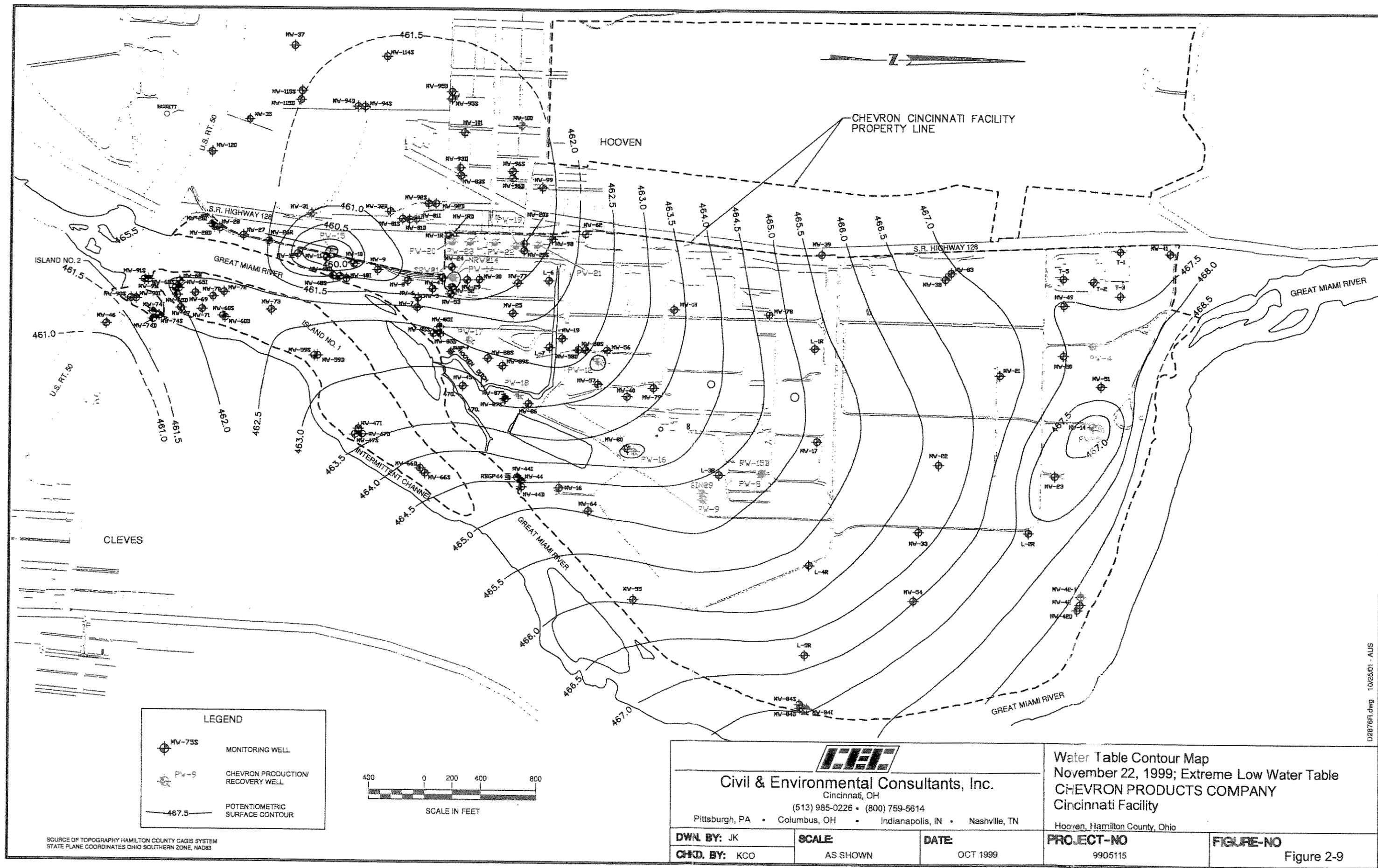
467.5 POTENTIOMETRIC SURFACE CONTOUR



SOURCE OF TOPOGRAPHY HAMILTON COUNTY CAGIS SYSTEM
STATE PLANE COORDINATES OHIO SOUTHERN ZONE, NAD83

 Civil & Environmental Consultants, Inc. Cincinnati, OH (513) 985-0226 • (800) 759-5614 Pittsburgh, PA • Columbus, OH • Indianapolis, IN • Nashville, TN		Water Table Contour Map September 24, 1999; Typical Low Water Table CHEVRON PRODUCTS COMPANY Cincinnati Facility Hooven, Hamilton County, Ohio	
		PROJECT-NO 9905115	FIGURE-NO Figure 2-8
DWN. BY: JK CHKD. BY: KCO	SCALE: AS SHOWN	DATE: OCT 1999	

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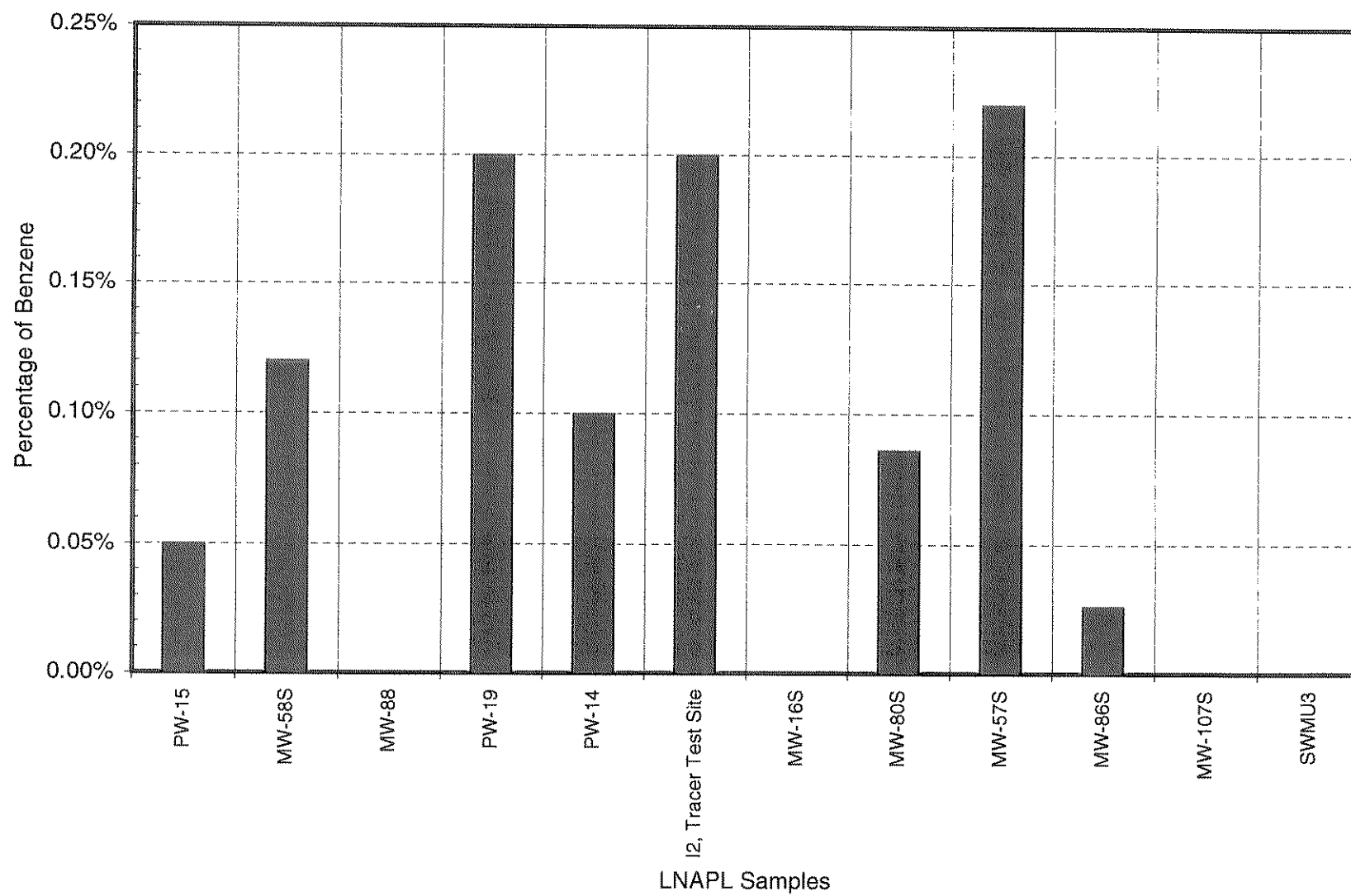


Figure 2.10. Summary of Benzene Analyses of LNAPL Samples

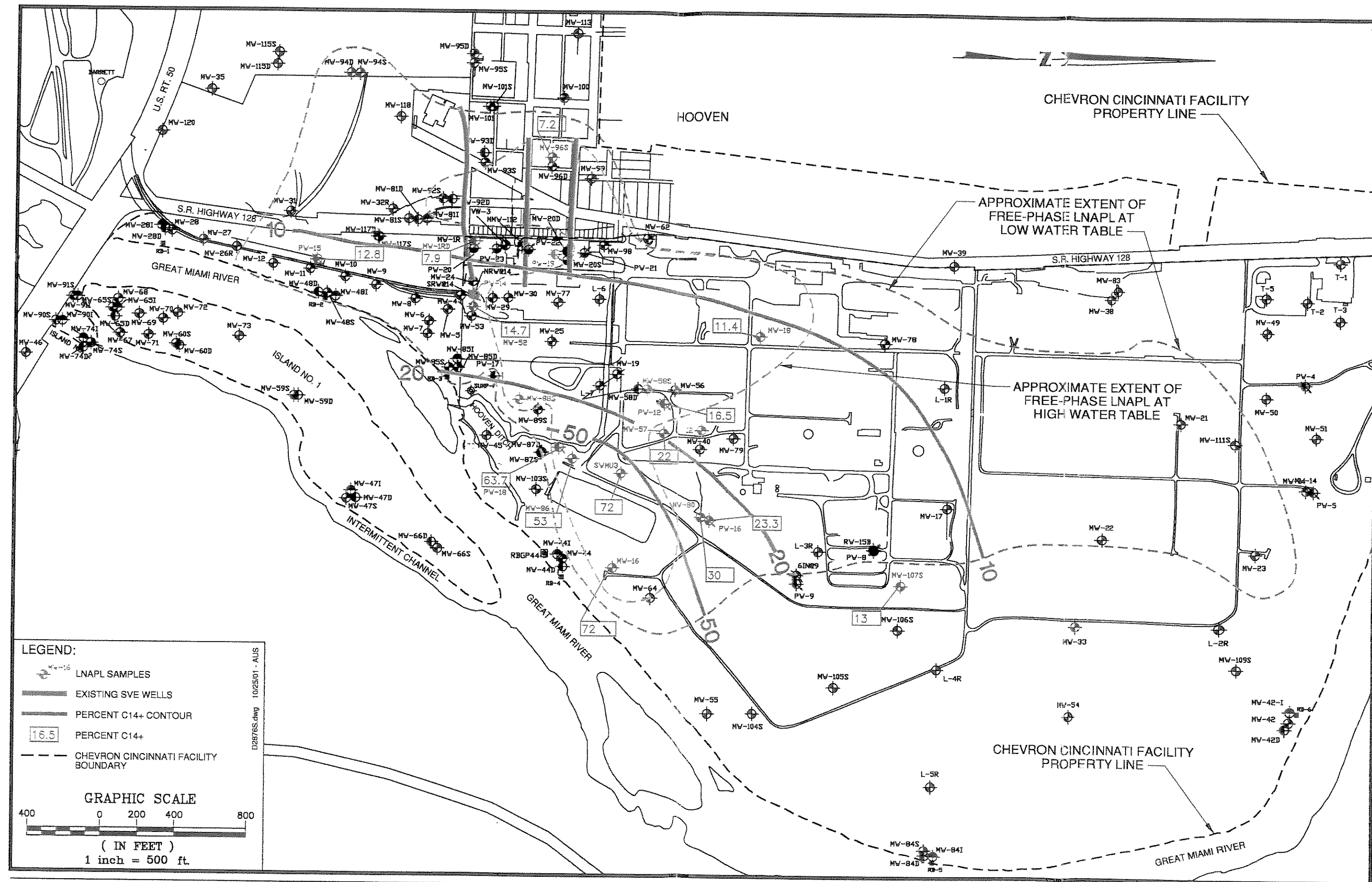
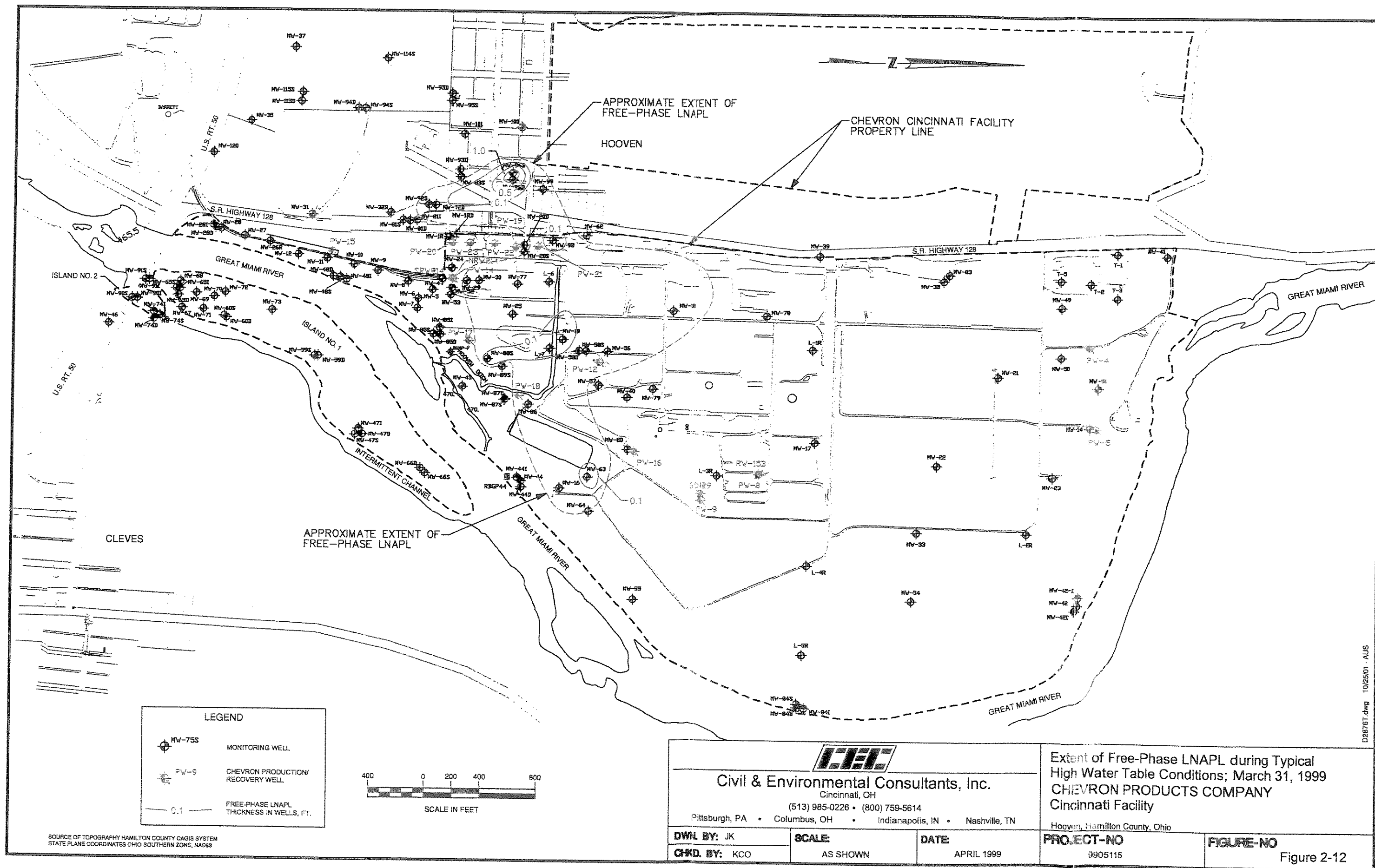
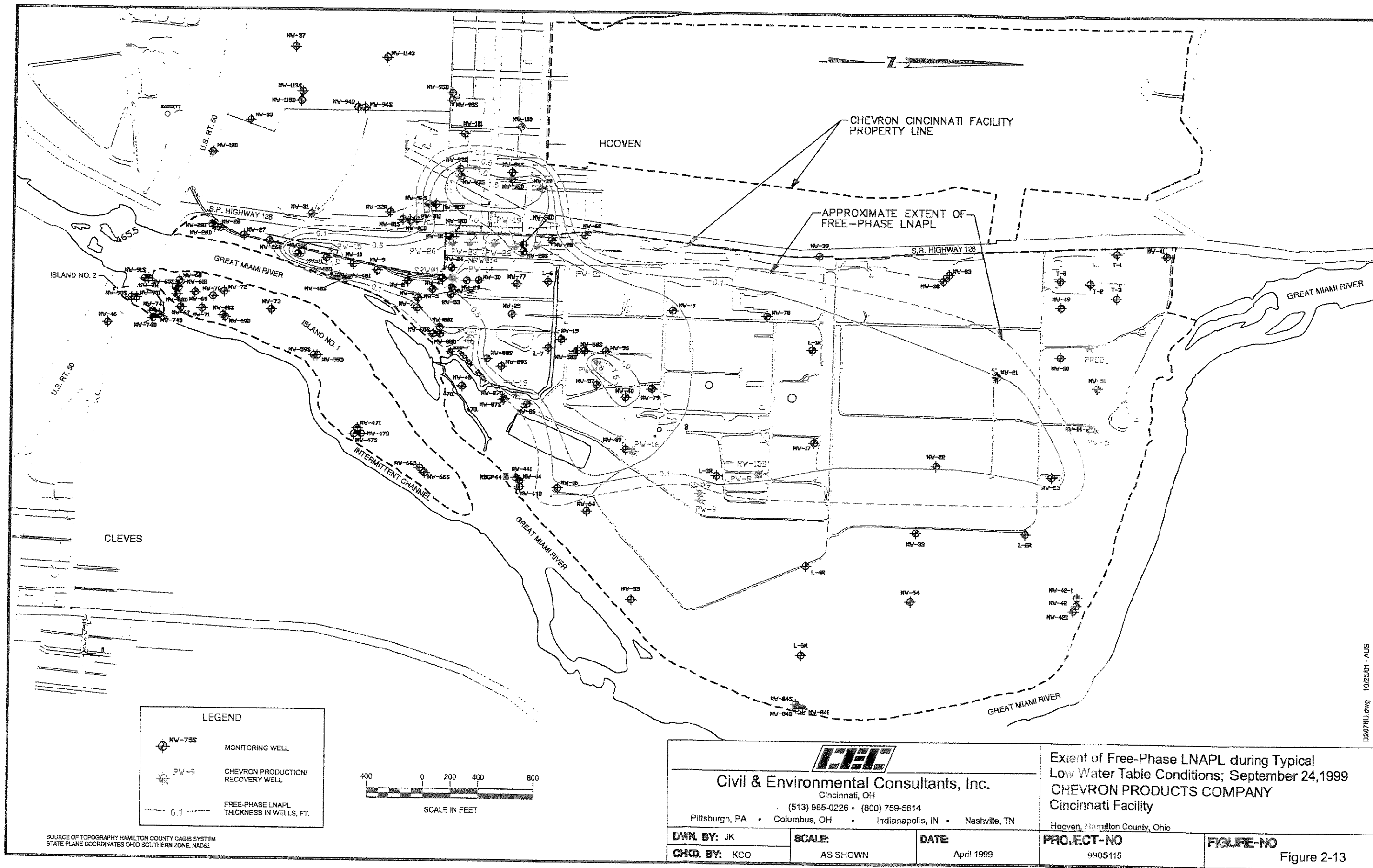
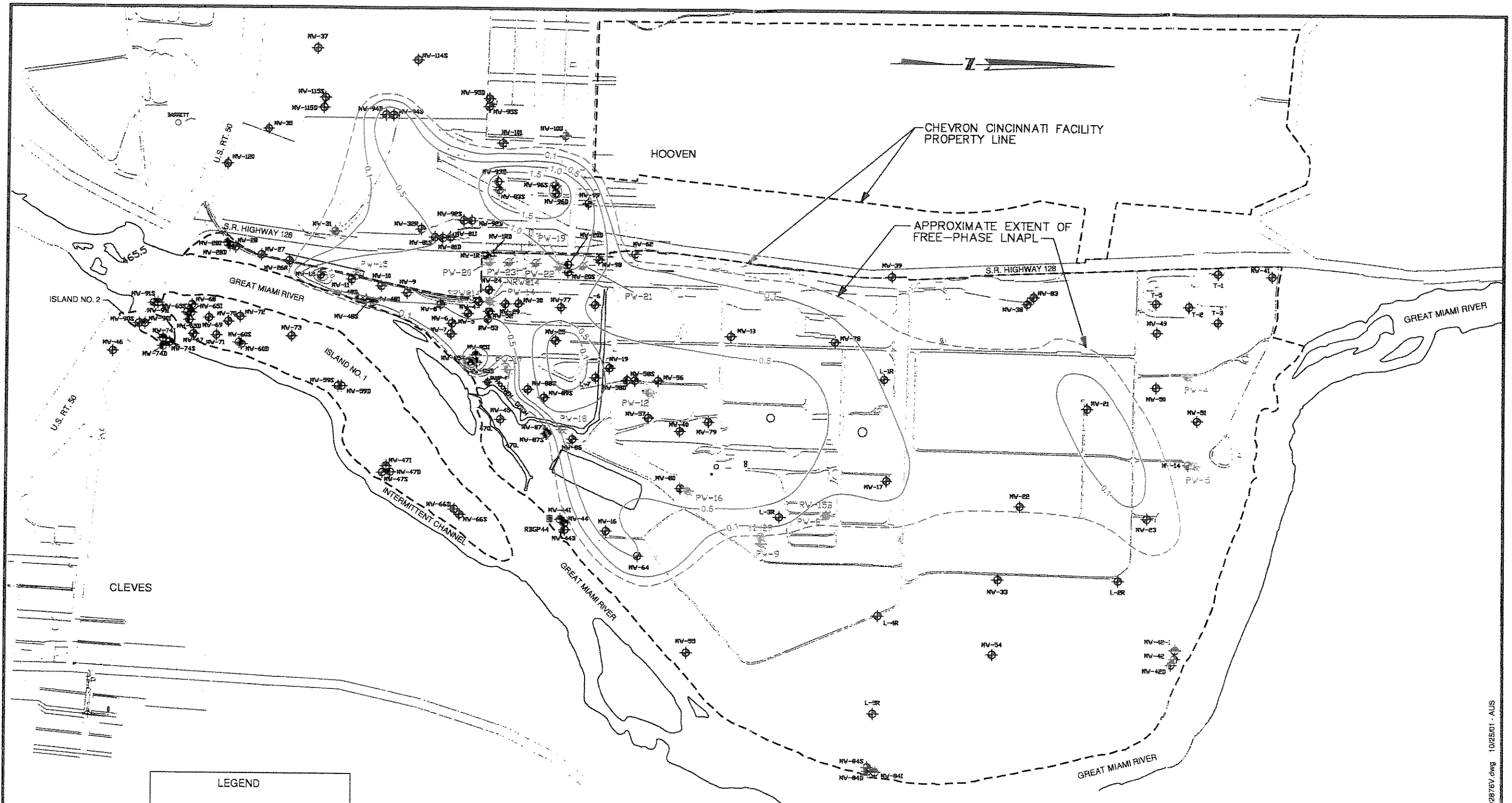


Figure 2-11. Distribution of Hydrocarbon Fractions Heavier than C14



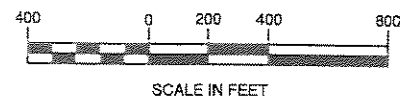
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LEGEND

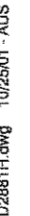
HV-75S MONITORING WELL
 PW-9 CHEVRON PRODUCTION/RECOVERY WELL
 0.1 FREE-PHASE LNAPL THICKNESS IN WELLS, FT.

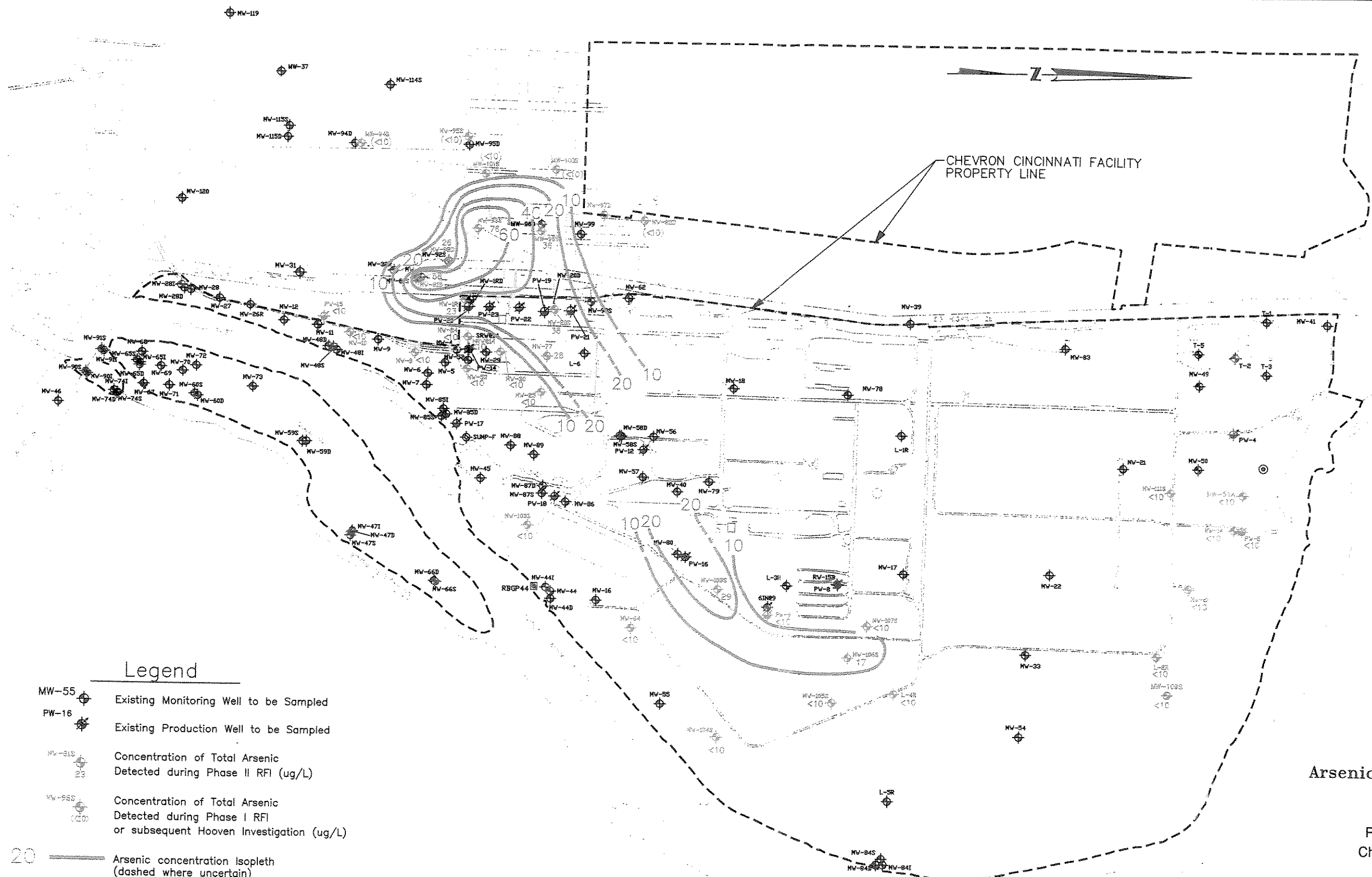


SOURCE OF TOPOGRAPHY HAMILTON COUNTY CAGIS SYSTEM
STATE PLANE COORDINATES OHIO SOUTHERN ZONE, NAD83

 Civil & Environmental Consultants, Inc. Cincinnati, OH (513) 985-0226 • (800) 759-5614 Pittsburgh, PA • Columbus, OH • Indianapolis, IN • Nashville, TN			Extent of Free-Phase LNAPL during Extreme Low Water Table; November 22, 1999 CHEVRON PRODUCTS COMPANY Cincinnati Facility Hoguen, Hamilton County, Ohio	
DWN. BY: JK CHD. BY: KCO	SCALE: AS SHOWN	DATE: April 1999	PROJECT-NO 9905115	FIGURE-NO Figure 2-14

D2876V.dwg 10/25/01 - AUS





Legend

- MW-55 Existing Monitoring Well to be Sampled
- PW-16 Existing Production Well to be Sampled
- MW-310 Concentration of Total Arsenic Detected during Phase II RFI (ug/L)
- MW-585 Concentration of Total Arsenic Detected during Phase I RFI or subsequent Hooven Investigation (ug/L)
- 20 Arsenic concentration isopleth (dashed where uncertain)

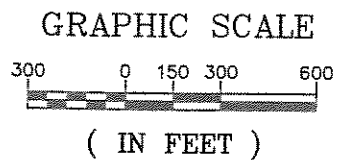


Figure 2-17
Arsenic in Groundwater
Isopleth Map

RCRA Facility Investigation
Chevron Products Company
Cincinnati Facility
Hooven, Ohio
4898005

Environmental Science & Engineering, Inc.
A MACTEC Company
RED 01/13/00 chevron/rfireport
Revised RED 03/08/00 arsgwiso

D2676X.DWG 10/25/01 - AUS

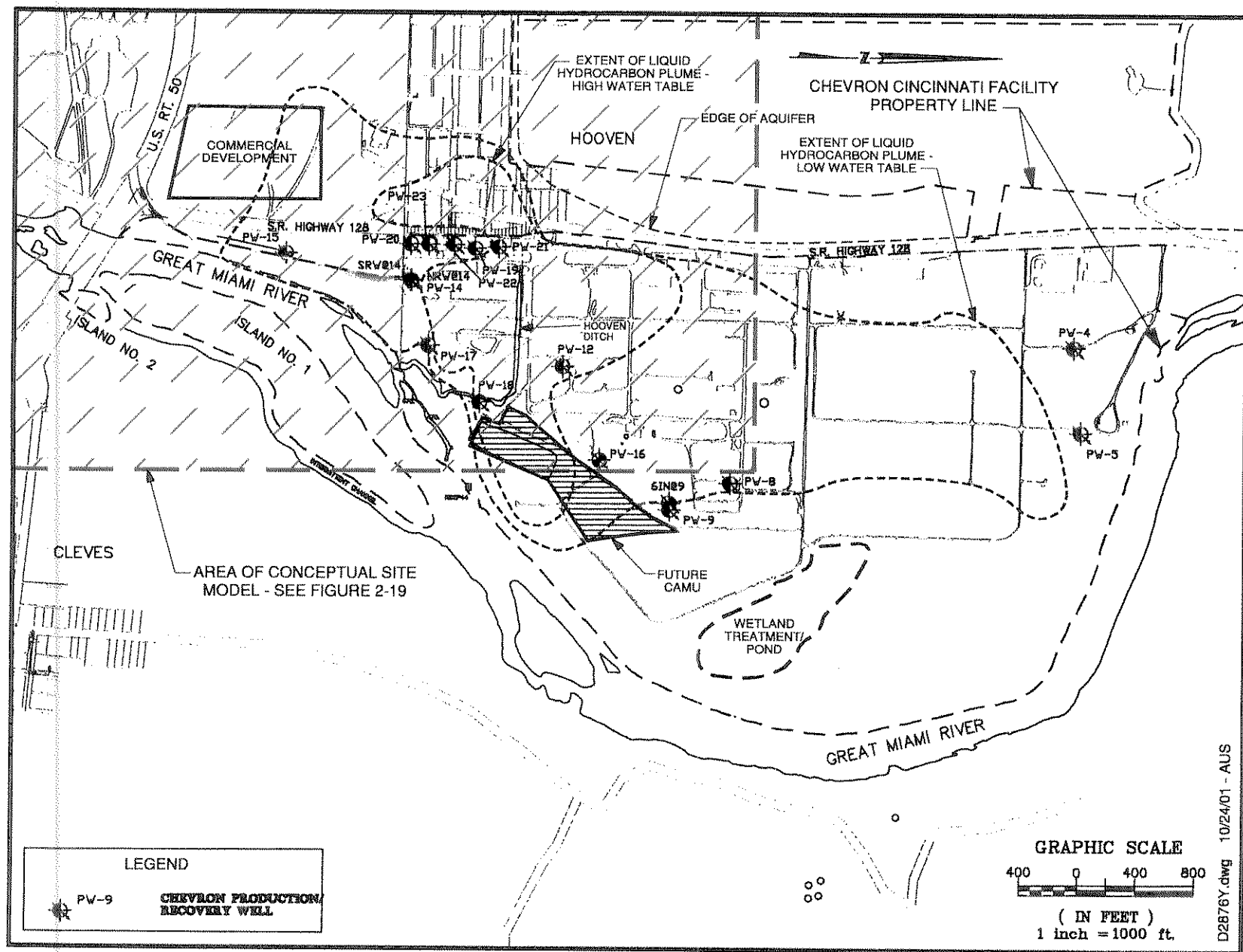


Figure 2-18. Site Map

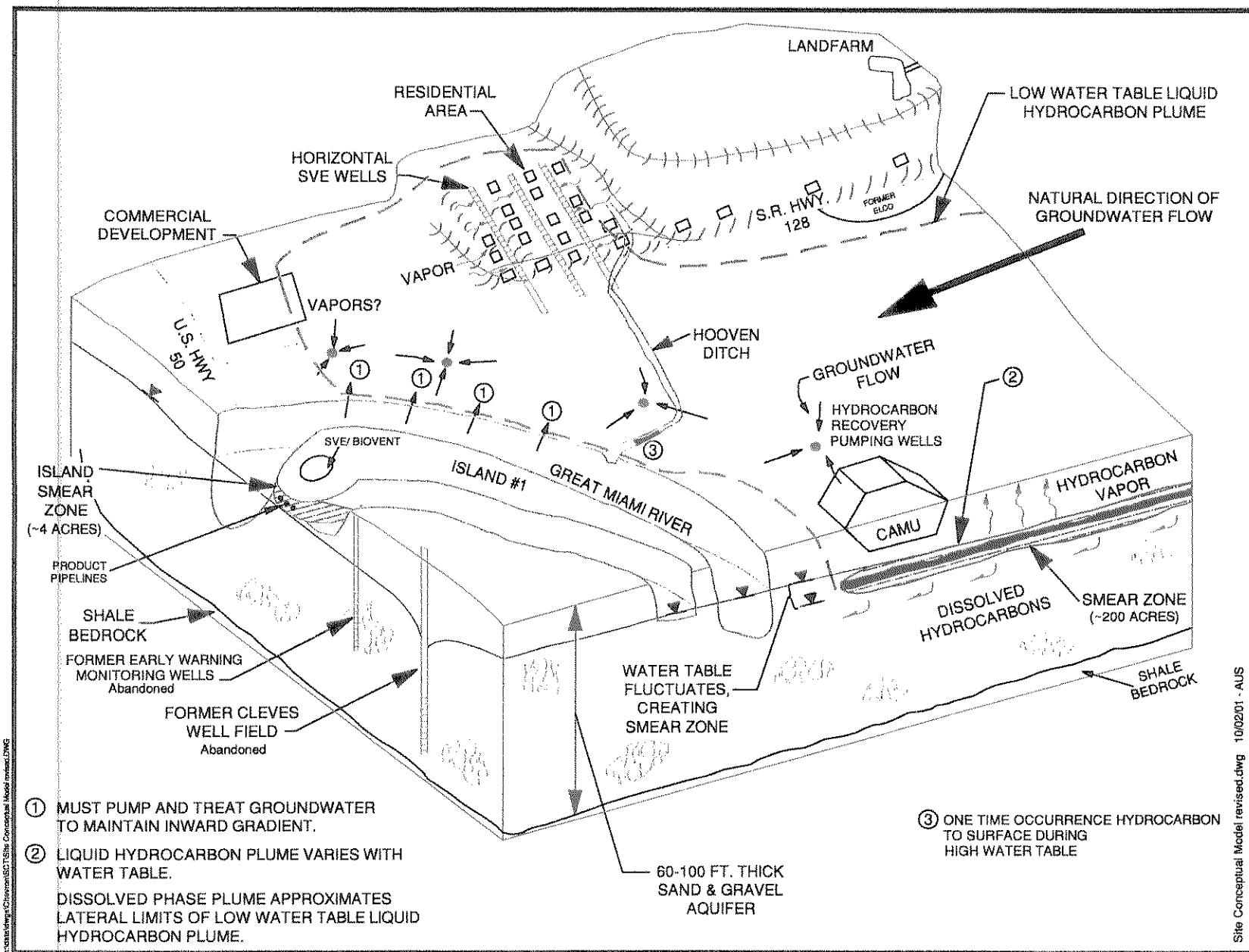


Figure 2-19. Site Conceptual Model, CHEVRON CINCINNATI FACILITY

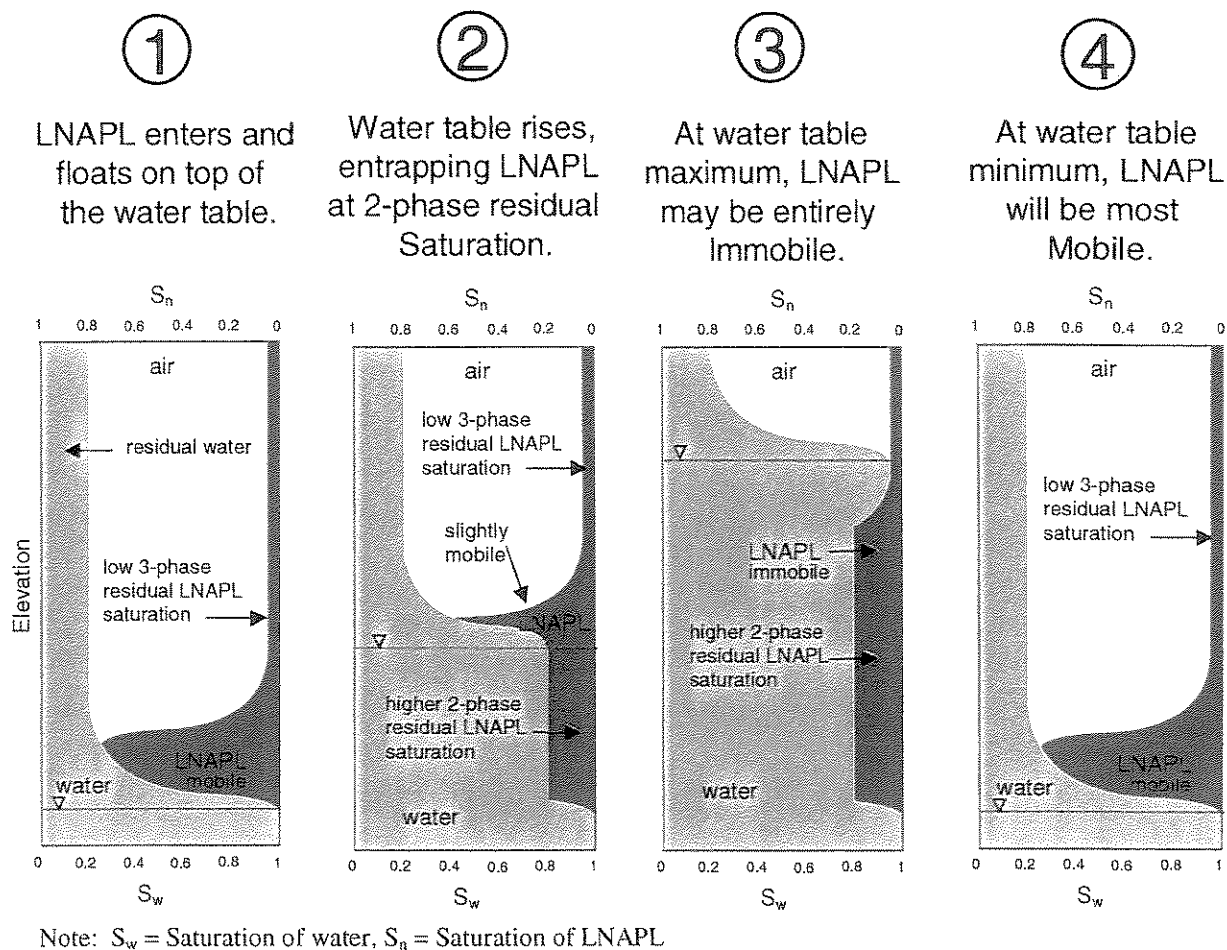


Figure 2-20

Schematic of LNAPL Redistribution by a Fluctuating Water Table

This illustration is included to represent conceptual development of the Chevron site only. It is not intended to propose or endorse a specific layout or development plan.

MIXED USE SCENARIO

based on voting results from 4/2/97 CAP meeting and 5/7/97 CAP meeting.

Plan revisions approved by CAP on 4/4/01.

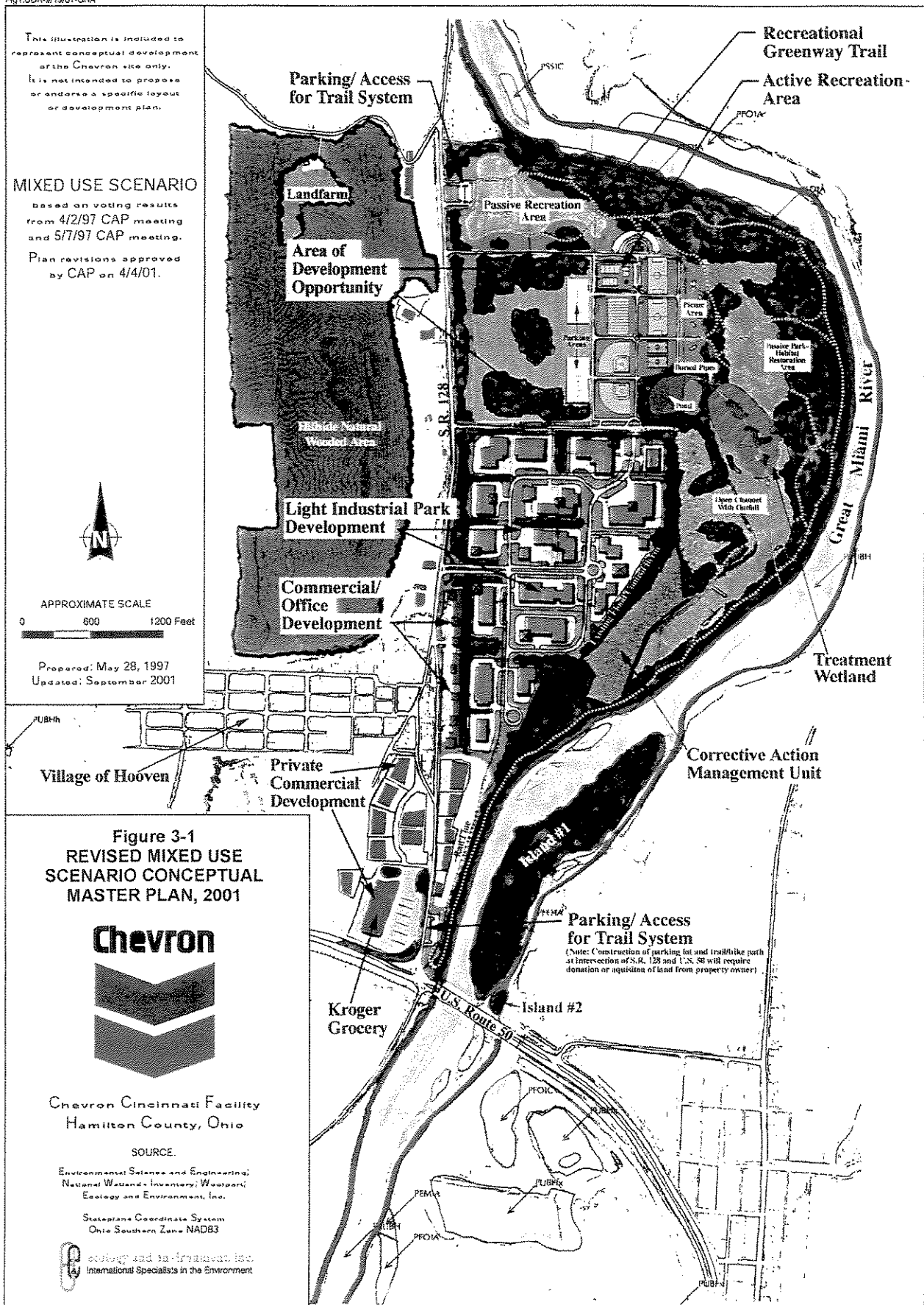
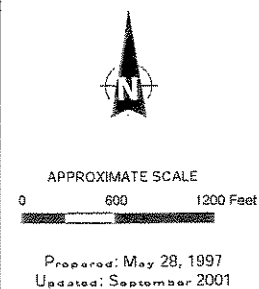


Figure 3-1
REVISED MIXED USE
SCENARIO CONCEPTUAL
MASTER PLAN, 2001



Chevron Cincinnati Facility
Hamilton County, Ohio

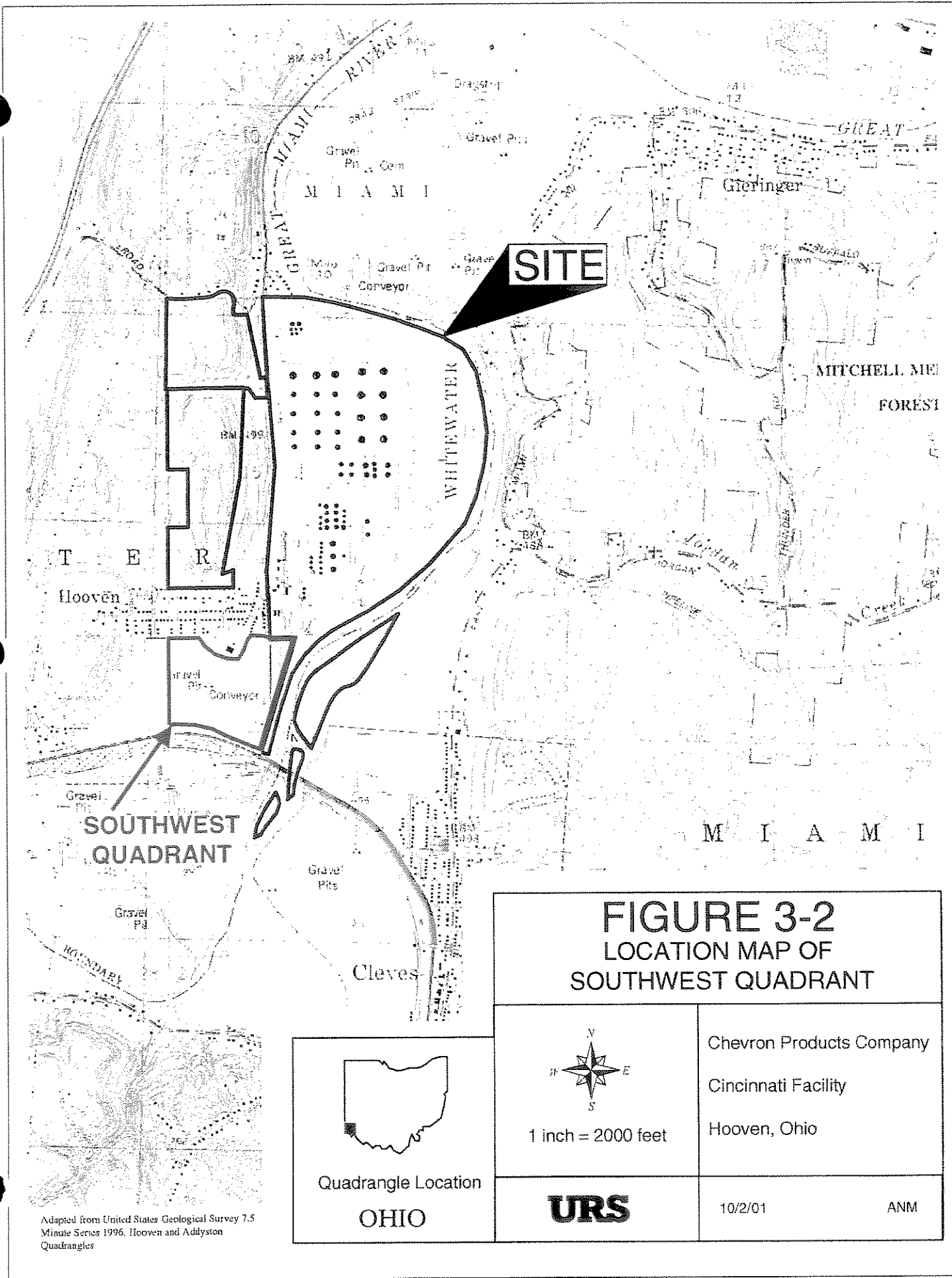
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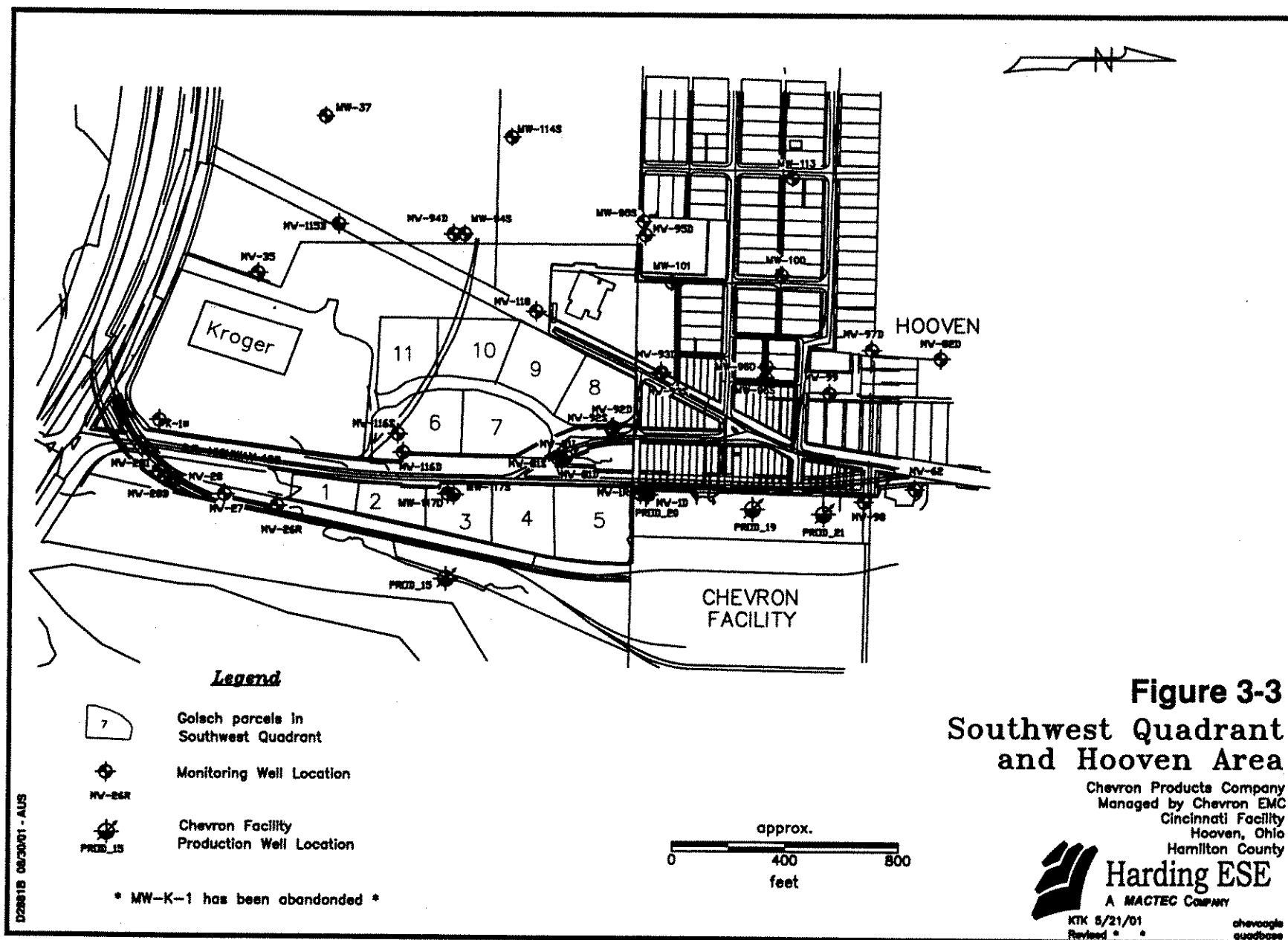
Environmental Science and Engineering;
National Wetland Inventory; Wetland;
Ecology and Environment, Inc.

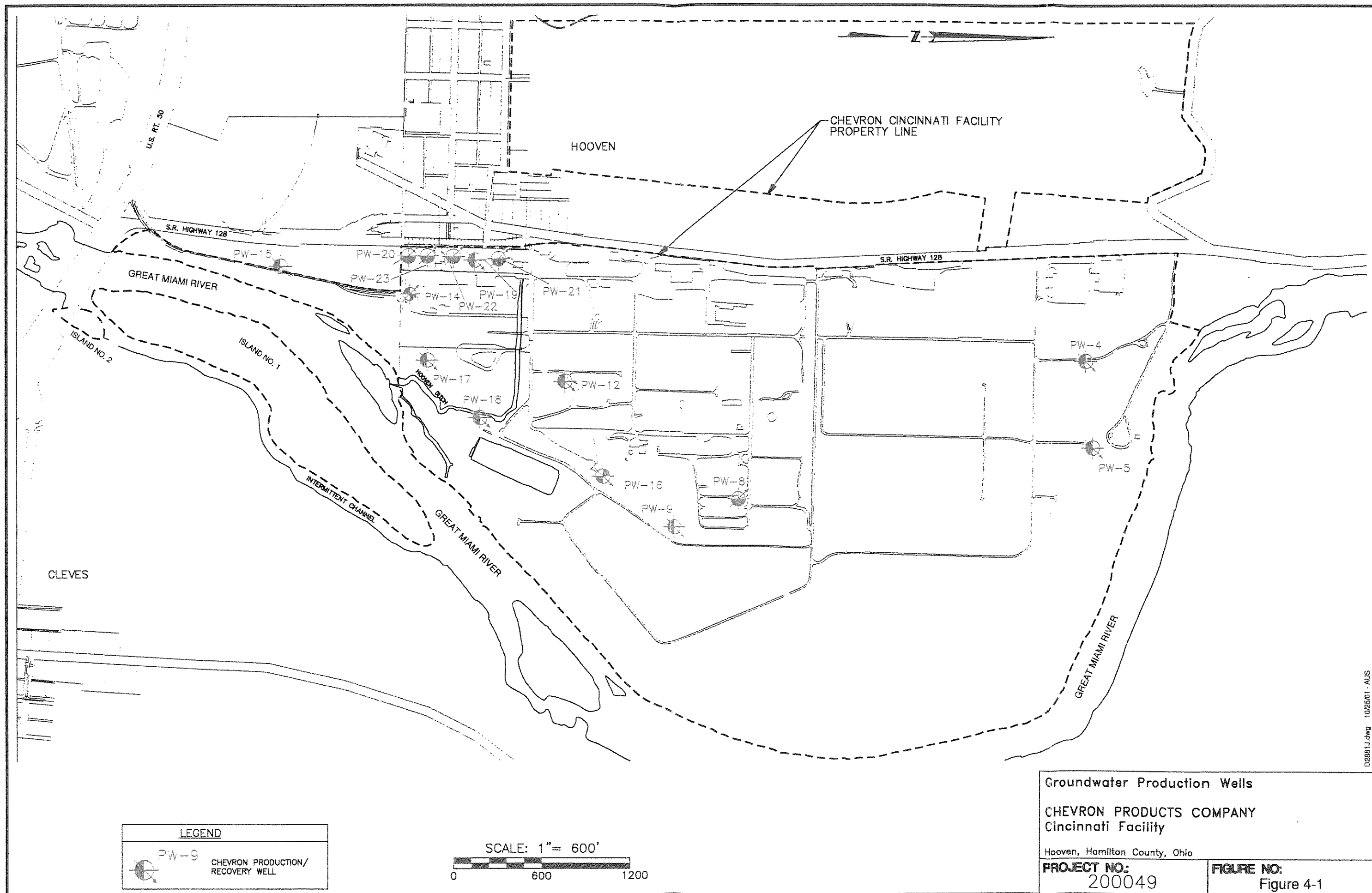
Stateplane Coordinate System
Ohio Southern Zone NAD83



Ecology and Environment, Inc.
International Specialists in the Environment







controlled by measuring the effluent dissolved oxygen (DO) concentration and the oxygen feed is set so that the effluent DO remains at 1.5 mg O₂/L (see Figure 4-2).

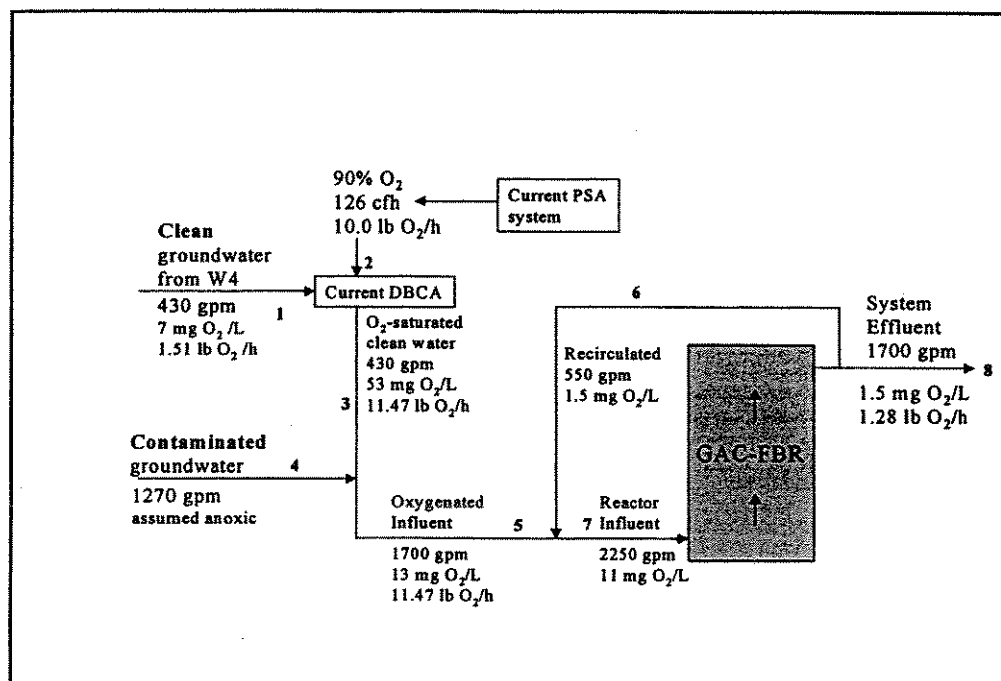


Figure 4-2

**Chevron Cincinnati GAC-FBR System Schematic
for High Water Table Operation**

During fall and winter, the focus of the pump-and-treat operation shifts to free-phase LNAPL recovery. As a result, the groundwater pumping rate may double, to 3400 gpm, of which 860 gpm is clean oxygen carrier water from PW 4 or 5. This requires that both treatment trains be used; in essence two of the systems depicted in Figure 4-2 are operated in parallel. At times, the system is oxygen-limited, i.e., even with the full 340 cfh oxygen generating capacity in use, the water flow rate must be reduced to meet the 1.5 mg O₂/L parameter in the system effluent.

The effluent from the FBR system is conveyed to an impoundment where it is polished before discharge to the Great Miami River.

Figure 4-3: Summary of Chevron Cincinnati Facility Free-Phase LNAPL Recovery

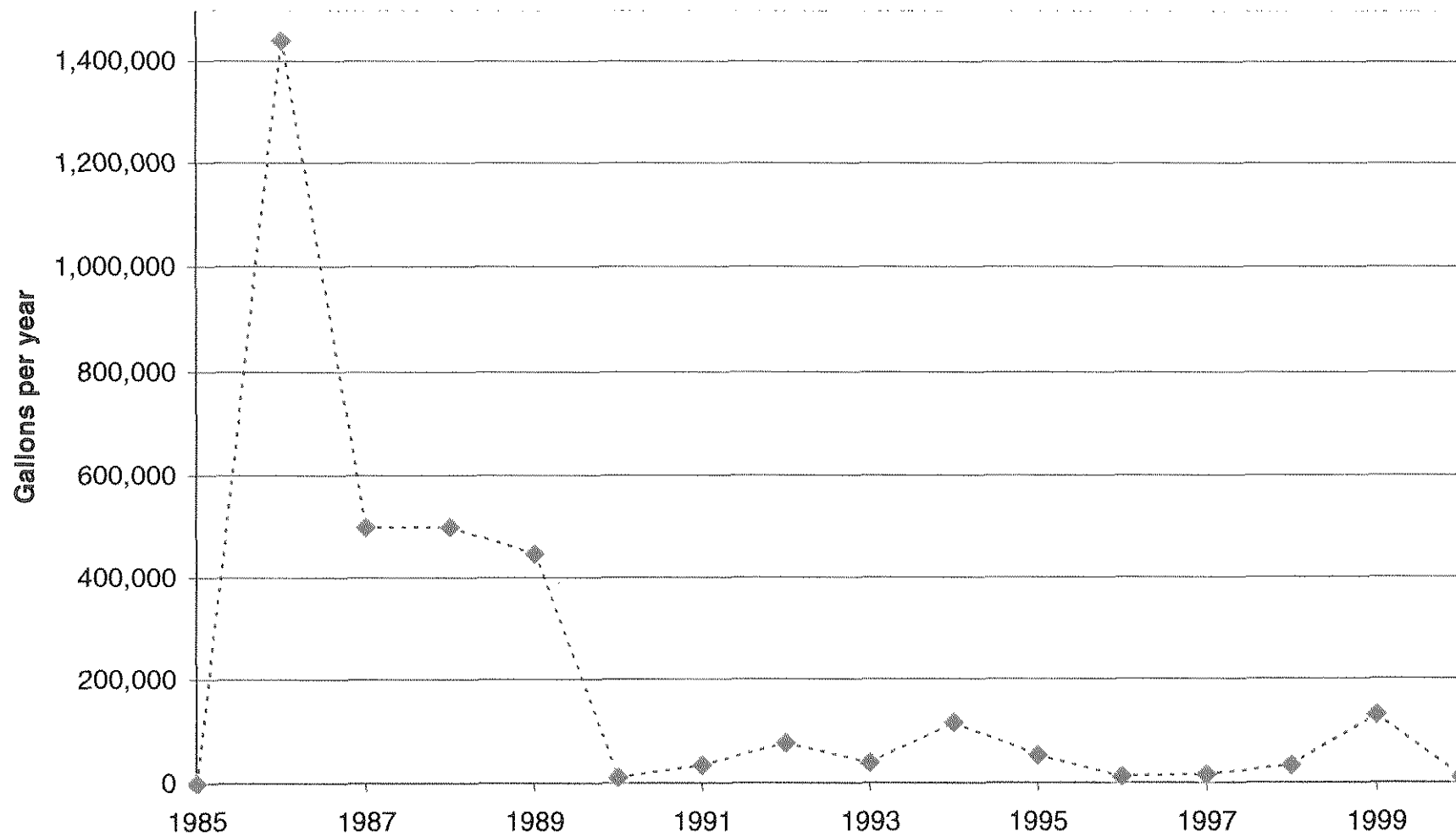
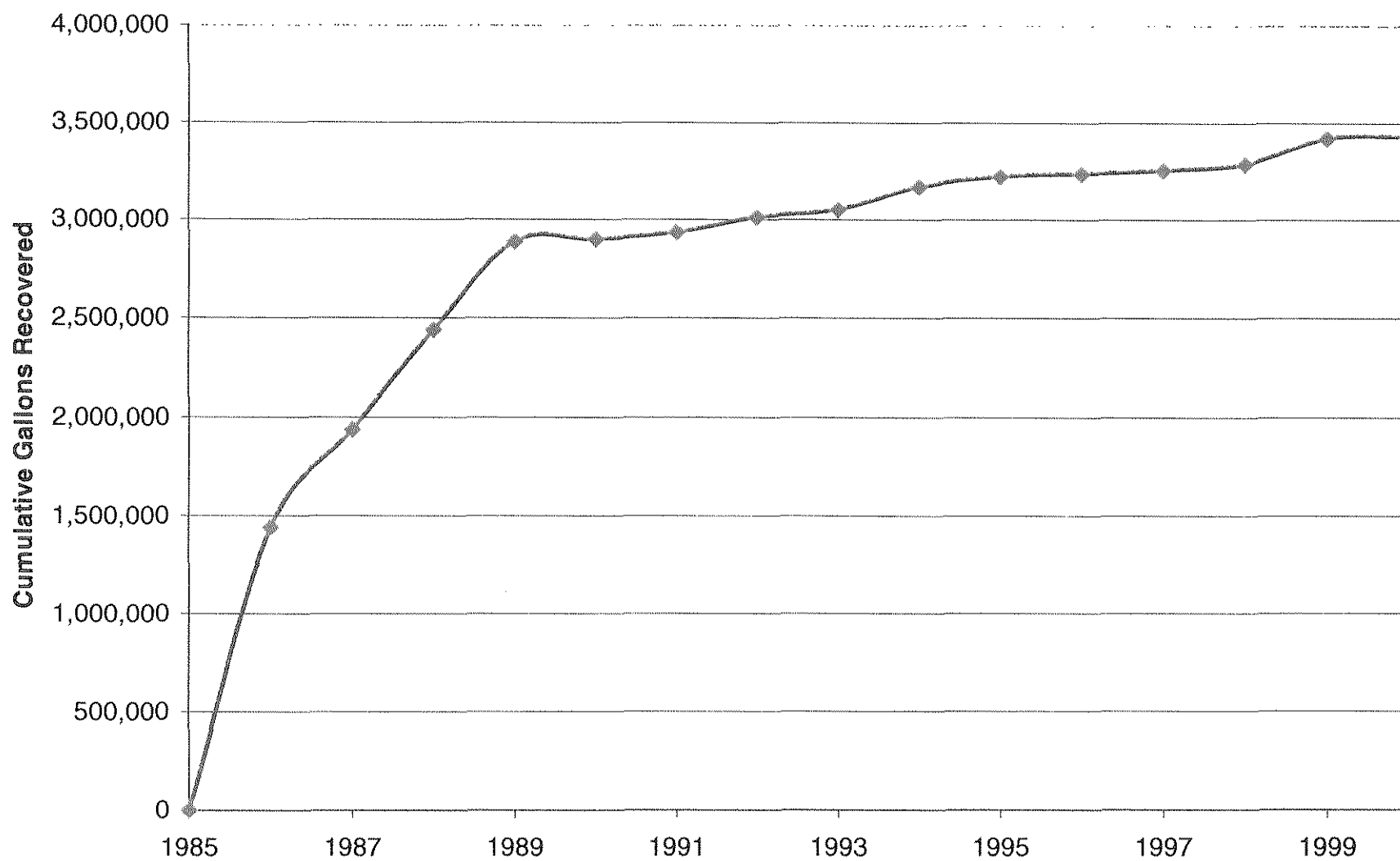


Figure 4-4: Cumulative Free-Phase LNAPL Recovery



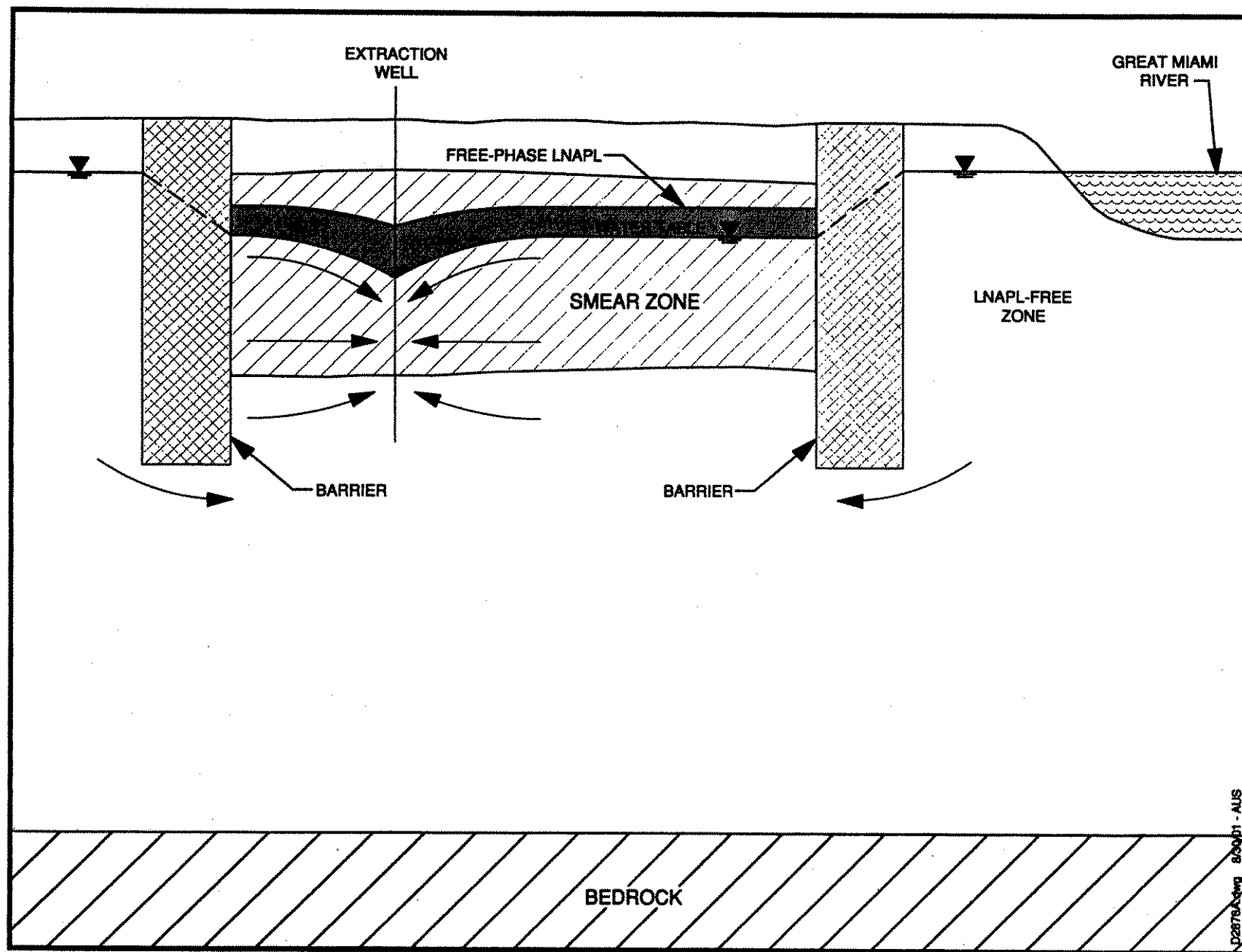


Figure 6-1. Conceptual Design of Partially-Penetrating Barriers at the Chevron Cincinnati Facility

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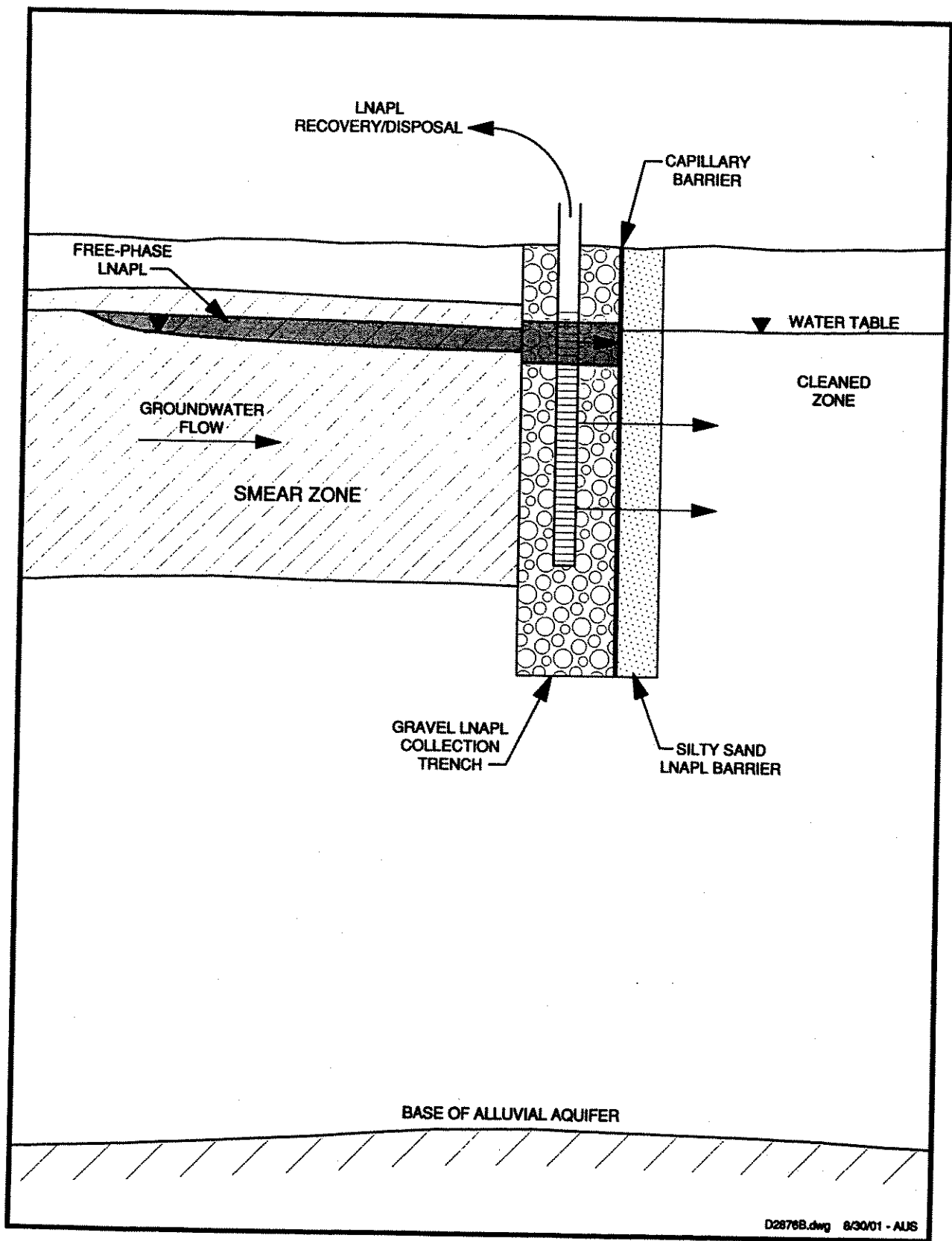


Figure 6-2. Conceptual Design of Capillary Barrier System at the Chevron Cincinnati Facility

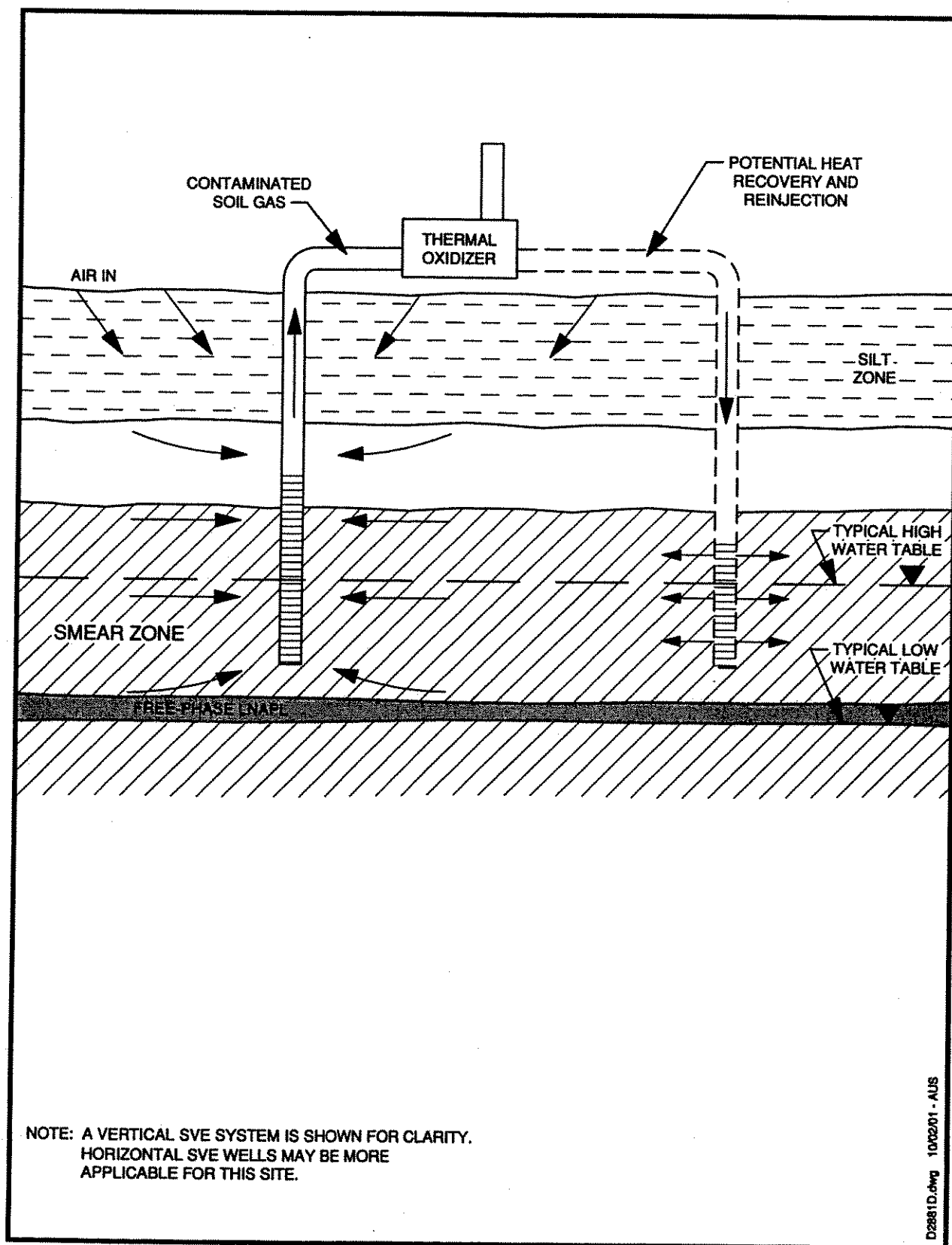


Figure 6-3. Conceptual Design of SVE at the Chevron Cincinnati Facility

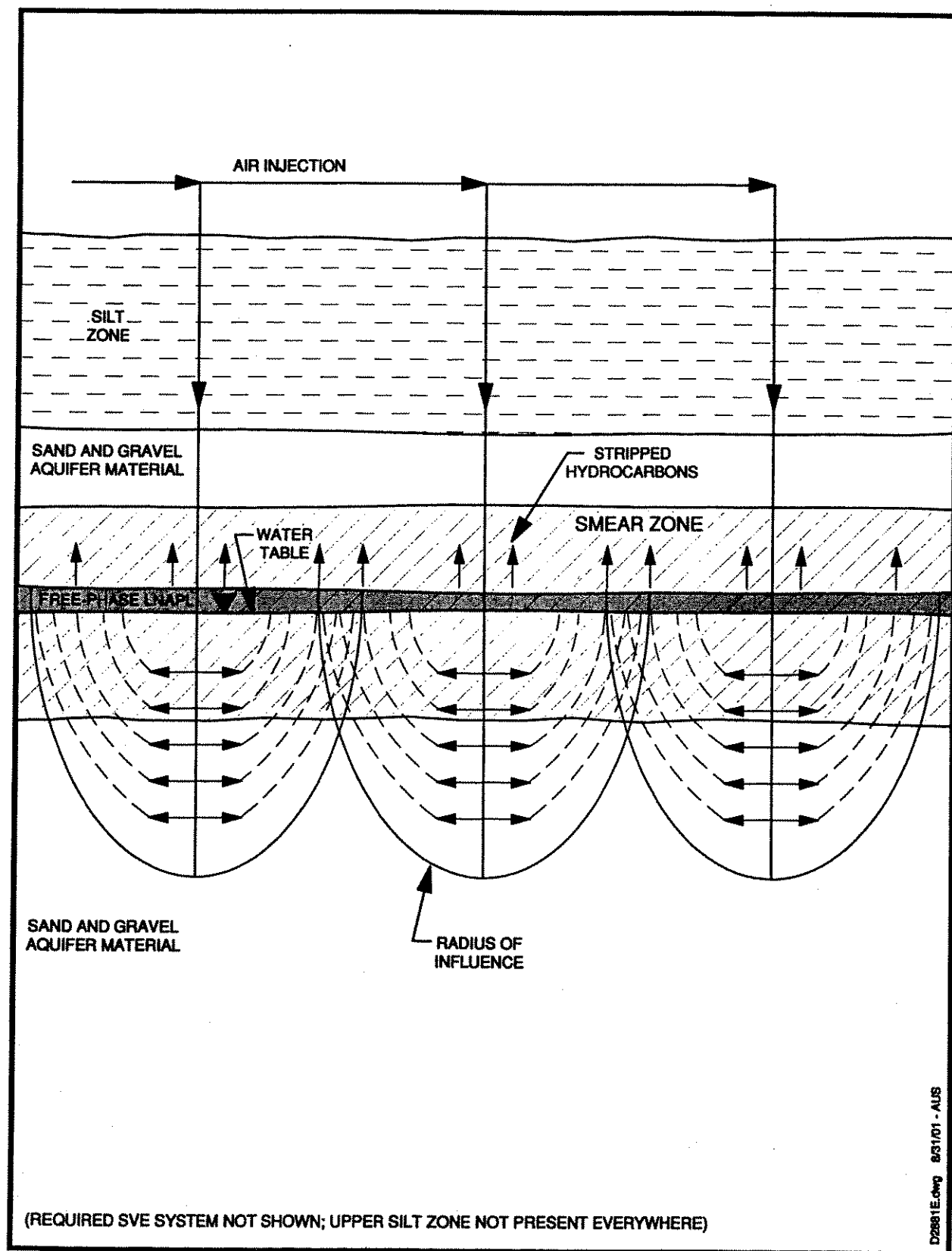


Figure 6-4. Conceptual Design of In-Situ Air Sparging System at the Chevron Cincinnati Facility

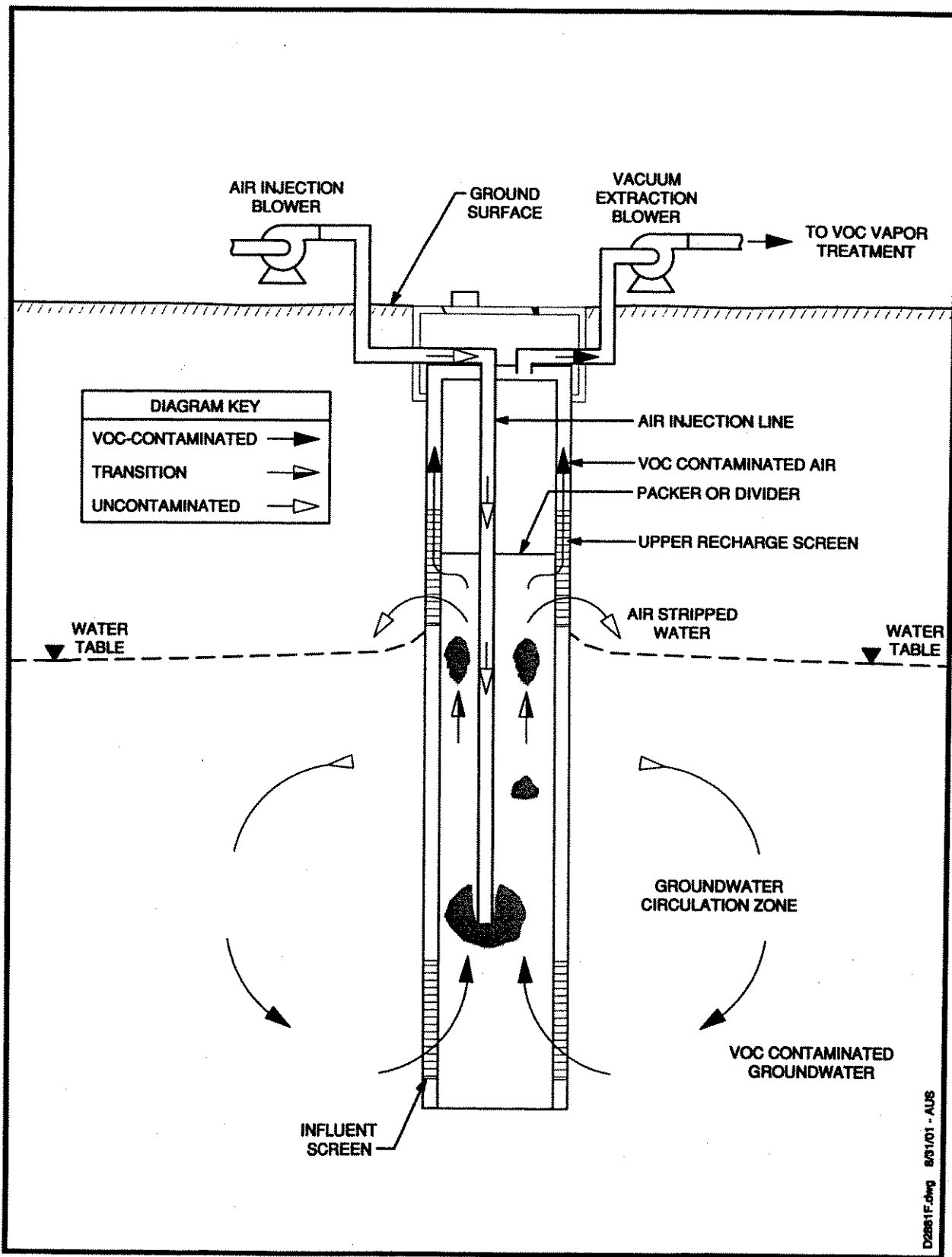


Figure 6-5. Conceptual Design for Groundwater Circulation Well Technology at the Chevron Cincinnati Facility

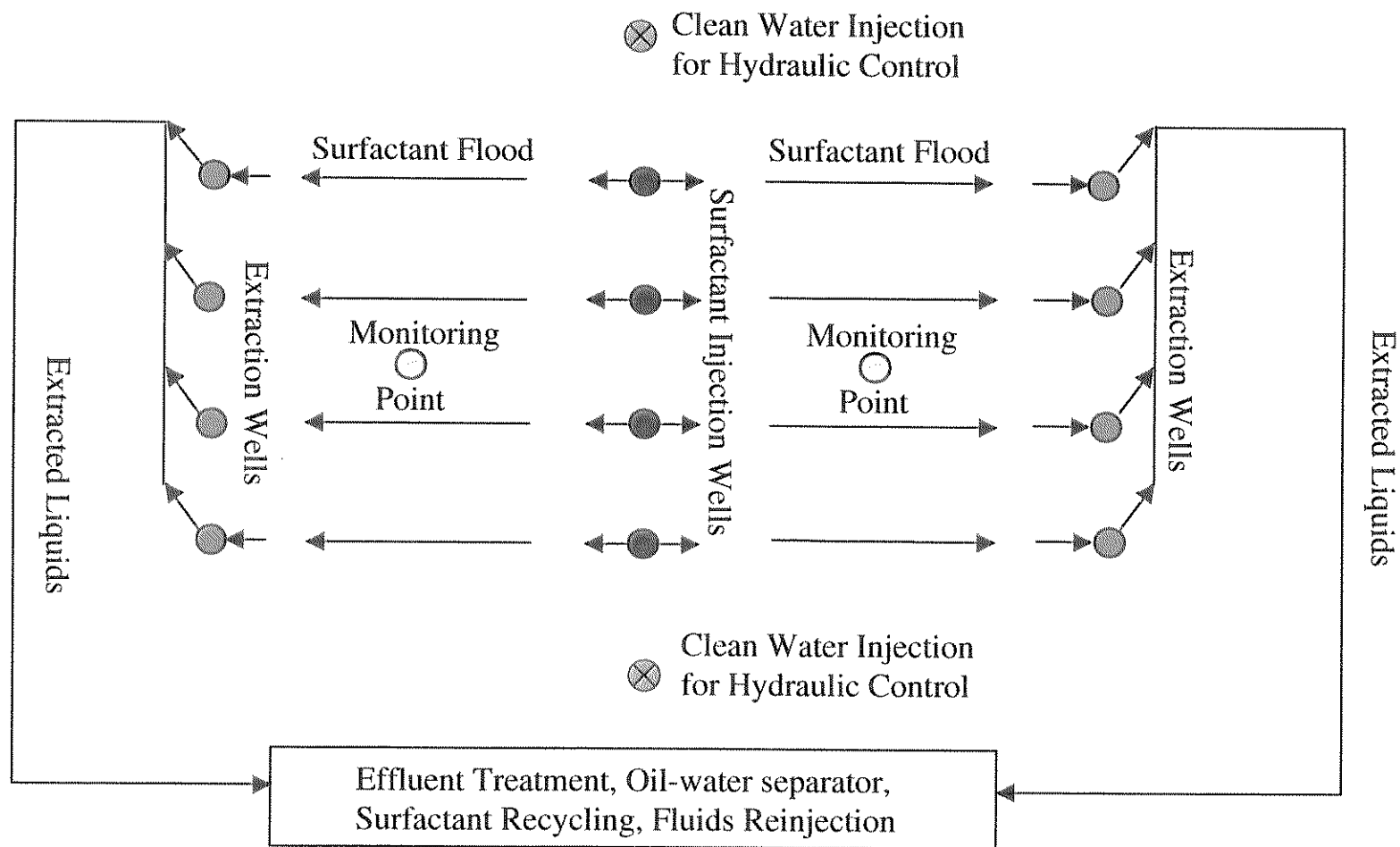


Figure 6-6
Illustration of Dual Line Drive for Surfactant Flooding (Plan View)

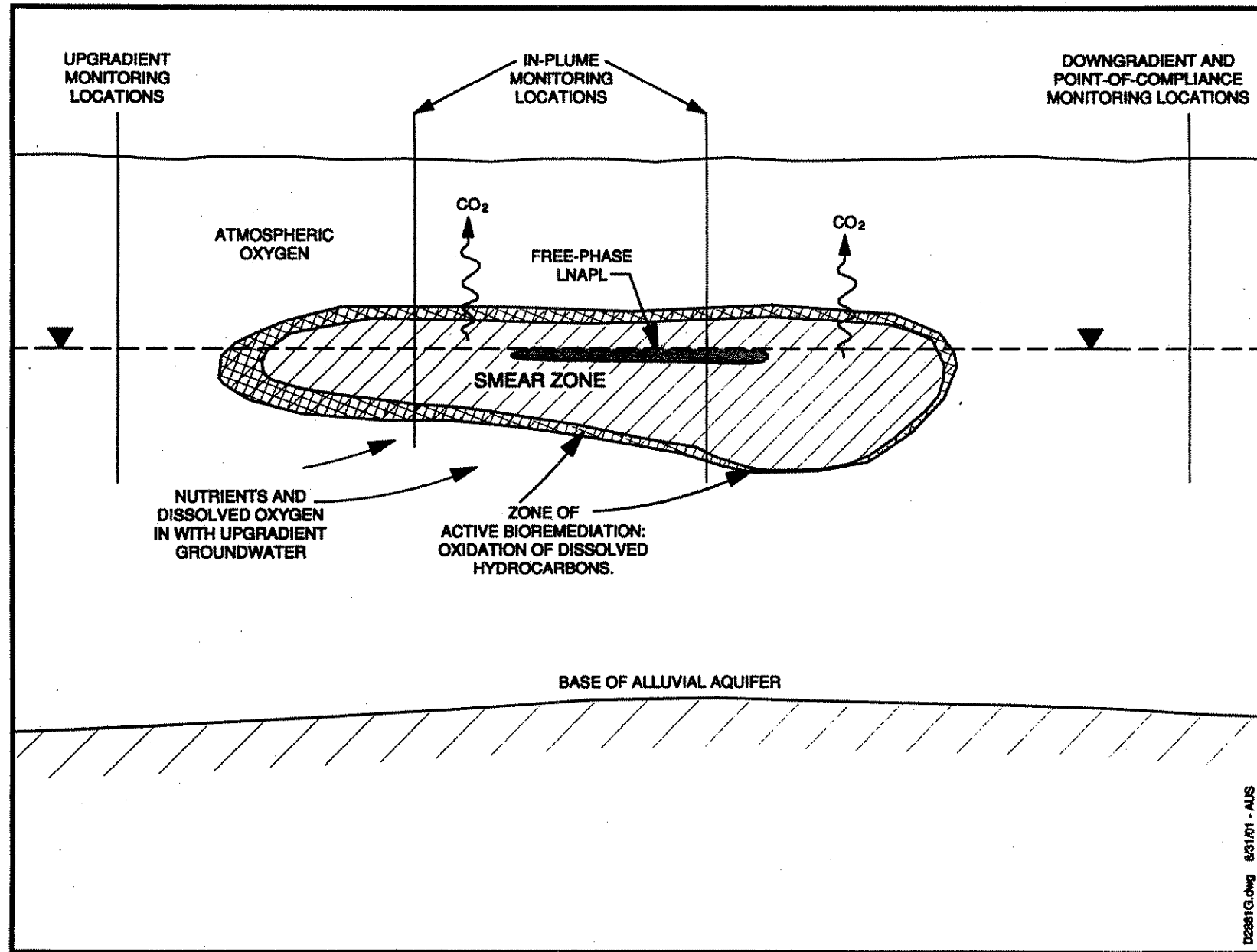


Figure 6-7. Conceptual Design for Monitored Natural Attenuation Technology at the Chevron Cincinnati Facility

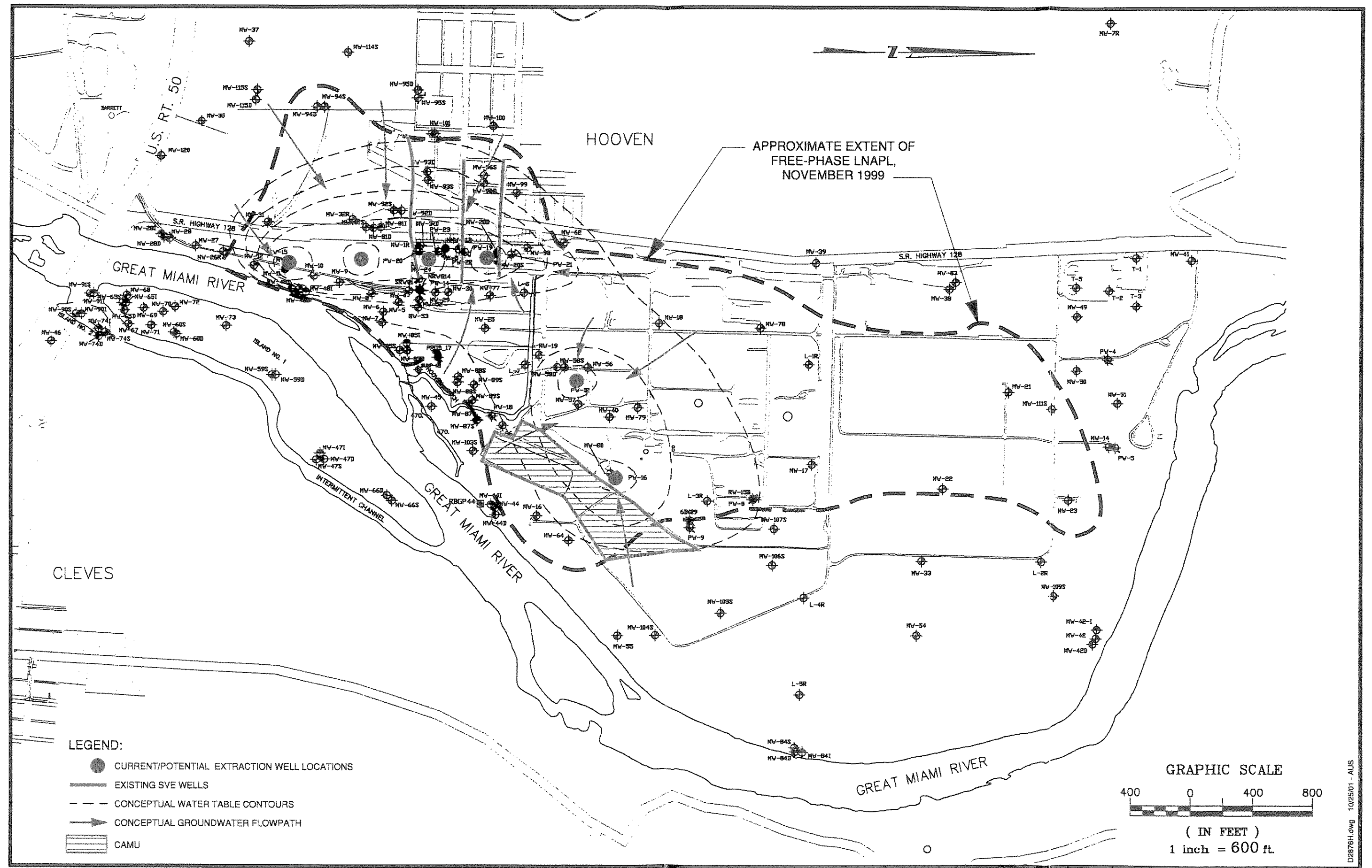


Figure 7-1: Alternative 1: Containment

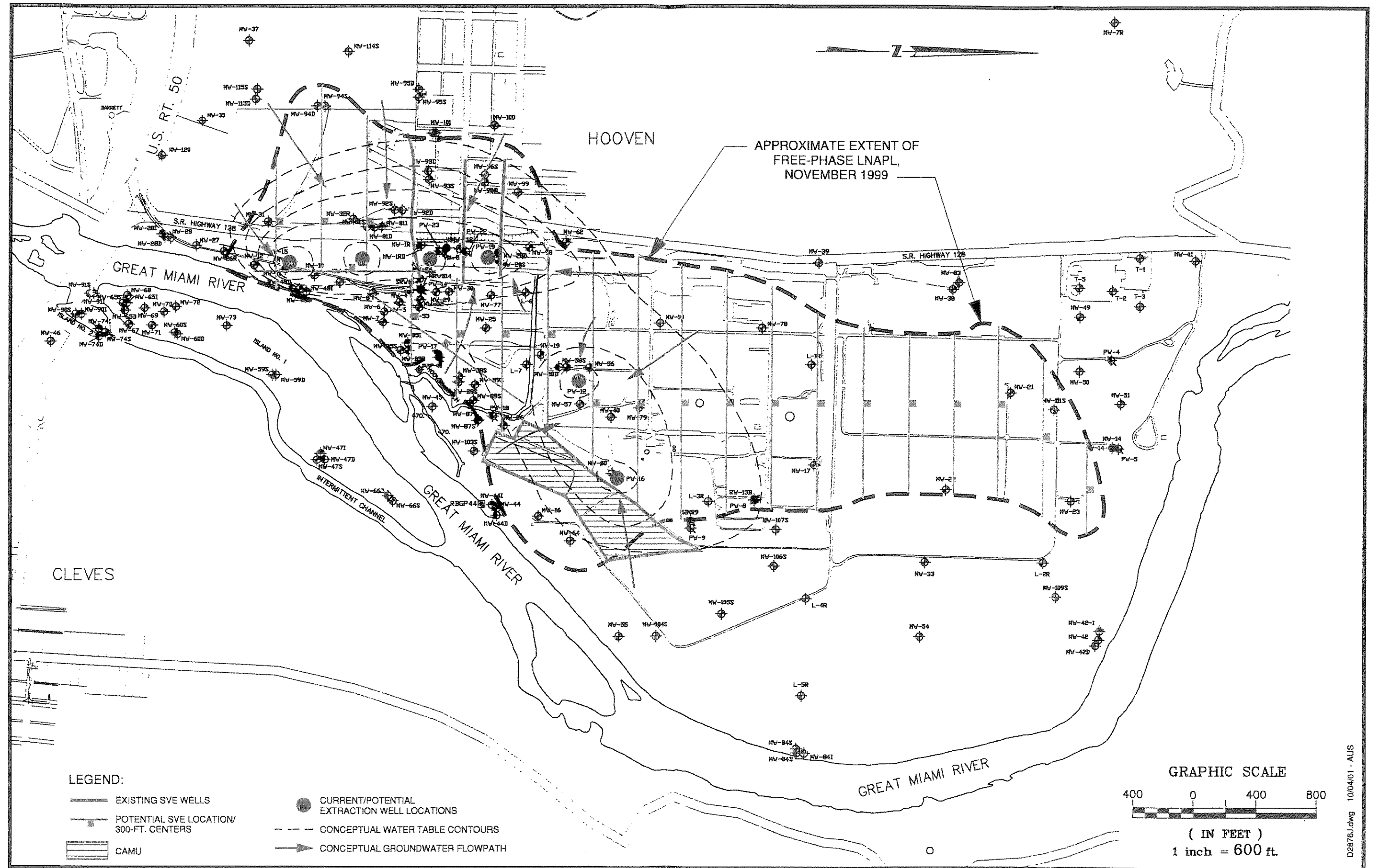


Figure 7-2: Alternative 2: Containment & SVE

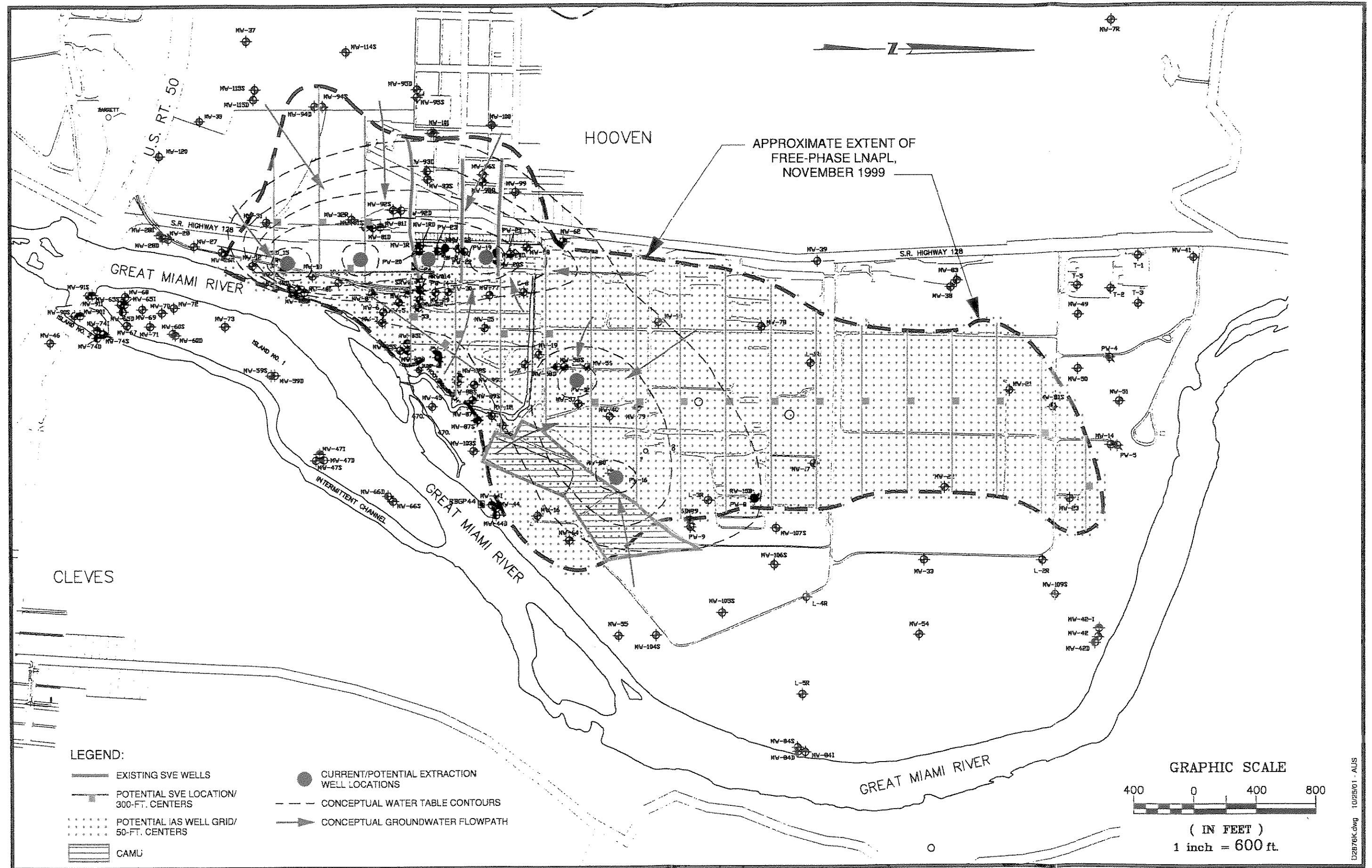


Figure 7-3: Alternative 3: Containment & SVE & IAS

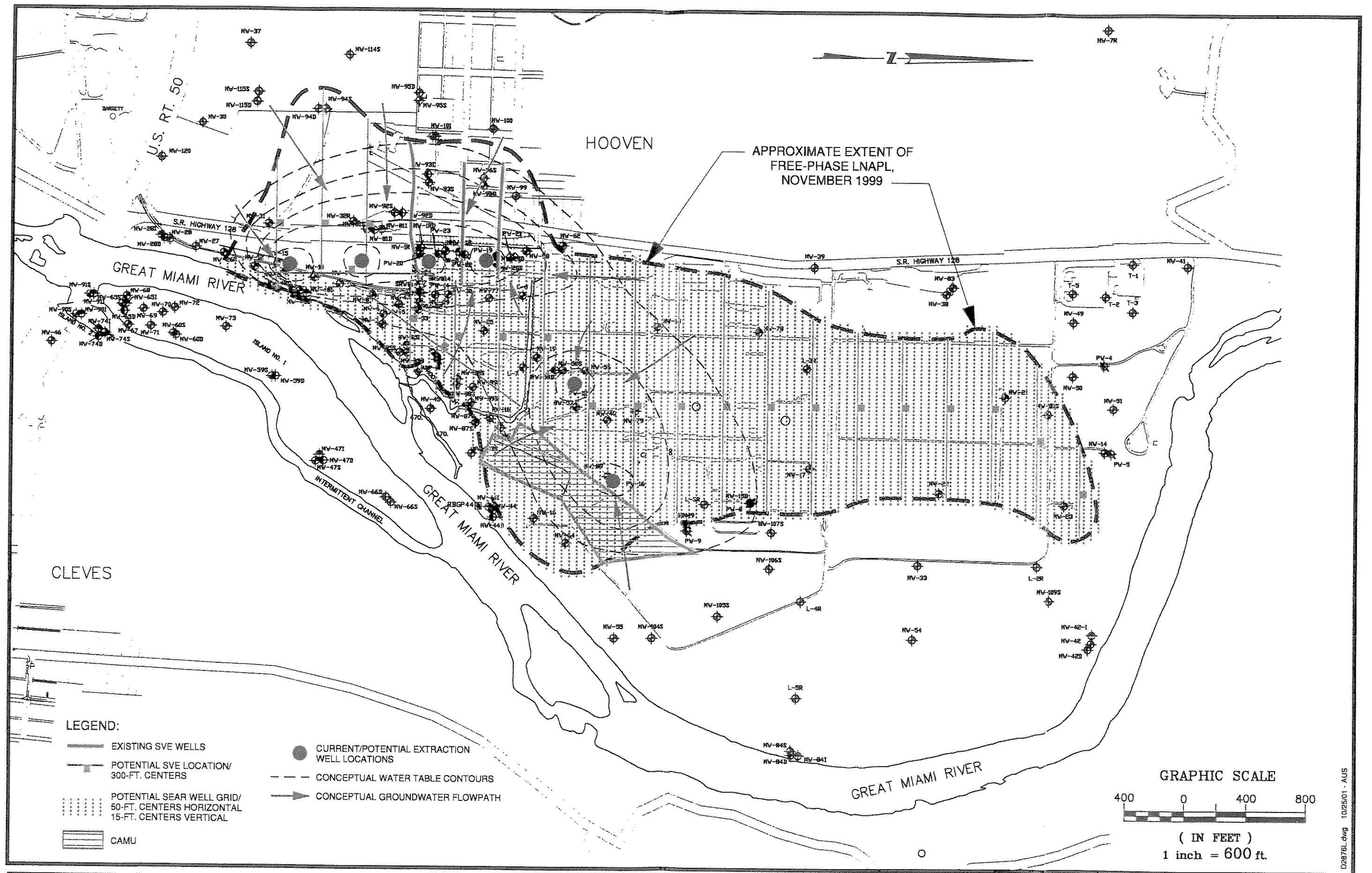


Figure 7-4: Alternative 4: Containment & SVE & SEAR

Table 7-2
Estimated Time from Present Needed for the
Groundwater Benzene Concentration to Drop Below the MCL (5µg/L)

Alternative	Initial Source Removal Technology	Time after Initial Source Removal	Duration of Initial Source Removal	Total Duration
		Years	Years	Years from Present
1	None	458	0	458
2	SVE	294	12	306
3	SVE + IAS	233	10	243
4	SVE + SEAR	93	8	101

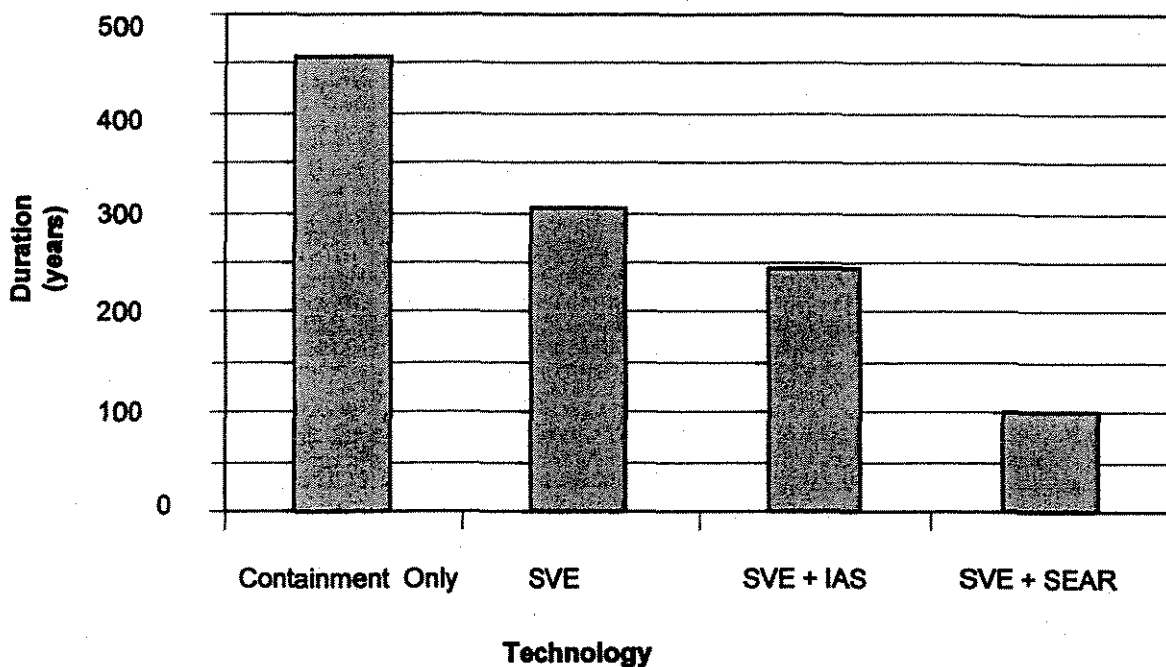


Figure 7-5
Projected Durations from Present to 5 µg/L Benzene, versus Technology

Table 7-4

Present Worth of All Costs Associated with Alternatives 1 through 4

Alternative	Initial Source Removal Technology	Present Worth (\$ millions)			
		Initial Source Removal		Ongoing Site Ops.	Grand Total ¹
		Capital	O&M		
1	None	0.00	0.00	49.20	50.45
2	SVE	18.74	23.77	49.08	92.84
3	SVE + IAS	24.78	32.08	48.64	106.74
4	SVE + SEAR	89.76	16.45	42.22	149.68

¹ Includes \$1.25 million in fixed costs, as discussed in Appendix B.

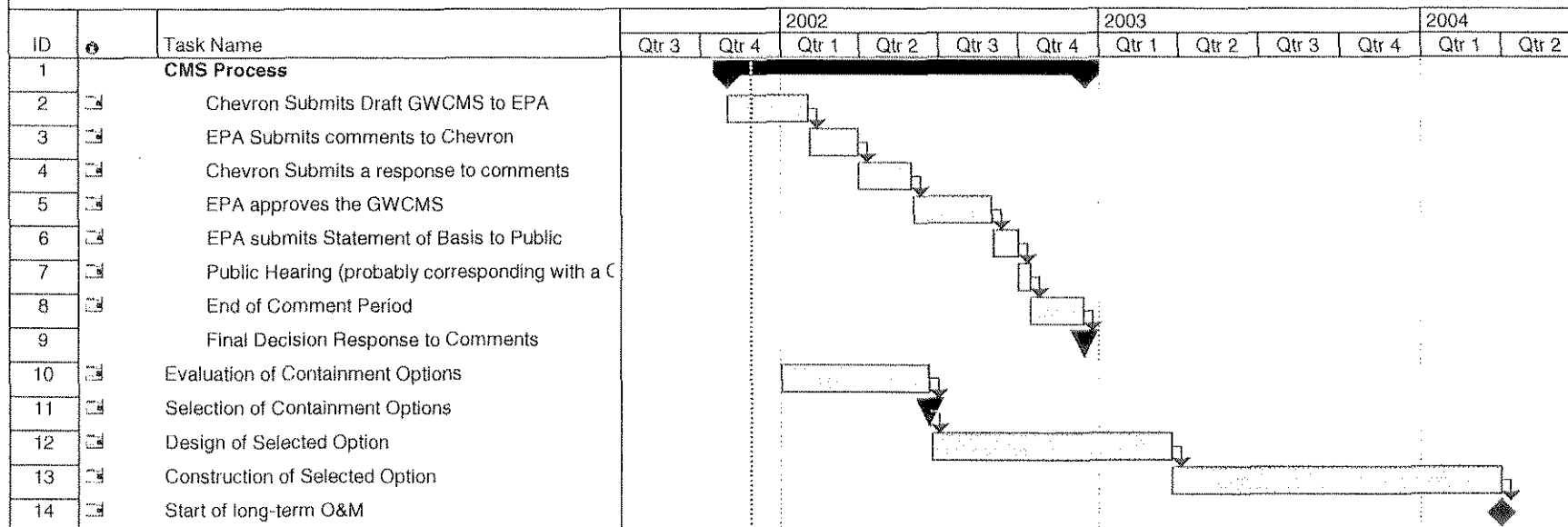


Figure 7-6 Present Worth of Alternatives

The following observations can be made:

- Total present worth costs increase significantly as increasingly aggressive source removal technologies are applied: Alternative 1 (Containment) < Alternative 2 (Containment + SVE) < Alternative 3 (Containment + SVE + IAS) < Alternative 4 (Containment + SVE + SEAR).
- Alternative 4 (Containment + SVE + SEAR) is the fastest alternative, as discussed in Section 7.4.1. It is also the most expensive alternative.

Figure 10-1
Chevron Cincinnati
Groundwater Remedy Implementation Schedule



Task

Split

Progress

Milestone

Summary

Rolled Up Task

Rolled Up Split

Rolled Up Milestone

Rolled Up Progress

External Tasks

Project Summary

External Milestone

Deadline

Note: The actual design and construction times will be dependent upon the complexity of the selected containment option.