US ERA ARCHIVE DOCUMENT

Regulation 13.7.1 Approved Method

Application: Ships constructed 1 Jan 1990 to 31 Dec 1999

Marine diesel engine power output >5,000 kW

Per cylinder displacement 90 litres

If a method has been approved by Party according to chapter 7 of the NOx Technical Code 2008 then ship is required to fit the "approved method" to enable the engine to meet Tier I limits.

IMO to be notified of approved method

The approved method to be installed at first renewal survey 12 months or more after IMO notified the "method" is approved

Tier	n < 130 rpm	130 ≤ n < 2000 rpm	n ≥ 2000 rpm
I	17.0 g/kWh	45.0*n ^(-0.2) g/kWh	9.8 g/kWh







Technology for meeting IMO III NOx limits Mexico Sept 26th Sept

Joseph Mc Carney

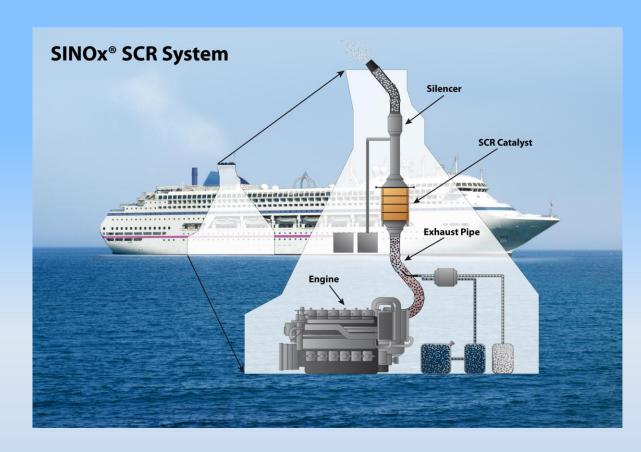
Johnson Matthey







nternational **A**ssociation for Catalytic **C**ontrol of Ship **E**missions to Air

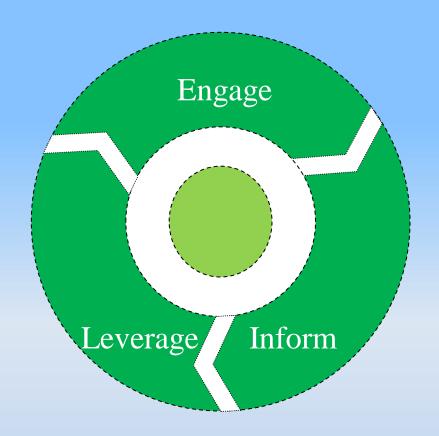








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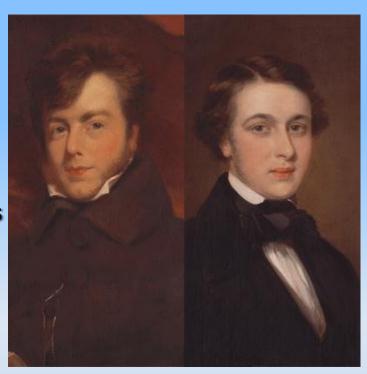




A Major Player



- Speciality chemicals –advanced materials
- 1817 1942 2002 2008 2012
- Core skills in Catalysis, PGMs & Process Tech.
- Invest in R&D and Manufacturing Technology
- Operate in over 30 countries, 10000 employees
- Focus on Growth Opportunities environment
- Technology & Market Leadership
- 160 SCR systems on ships large and small

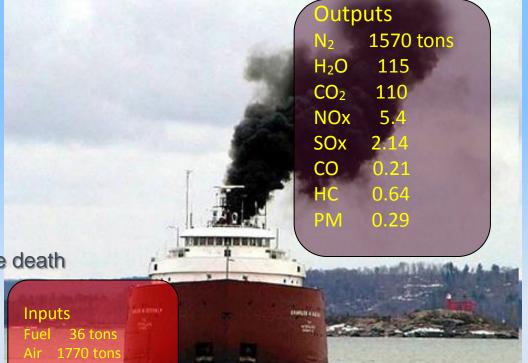




A Major Contribution NOx



- Formed in the heat of the engine
- SMOG & Particulates
- Acidifies the environment
- Lung and heart disease
- Economic costs
 - Medical care
 - Lost Productivity
 - Cost of pain / ill health / premature death



- US EPA ECA application
 - 14000 lives saved p.a
 - 5m experience relief respiratory symptoms



A Major Requirement



"IMO Tier III scripted to force after-treatment in NOx ECAs"





"Beginning in 2012 and completed no later than 2013, the Organization shall review the status of the technological development s to implement the standards set forth in paragraph 5.1.1 of this regulation and shall, if proven necessary, adjust the time periods set forth in that subparagraph." Regulation 13.10 of Annex 13, Resolution MEPC 176 (58):





IMO Review-Terms of Reference Johnson Matthey Catalysts

Exceptions & Exemptions

Range

NOx Review
Of Technology Solutions
To Meet IMO III

Applicability & Suitability

Status / Readiness Technology Trajectory Supply Chain Issues



Contributors



Canada	Japan	BIMCO	ICOMIA
Denmark	Liberia	CLIA	ICS
Estonia	Netherlands	CSC	IMarEST
Finland	Norway	Euromot	INTERTANKO
France	Sweden	IACS	IPIECA
Germany	United Kingdom	IADC	OCIMF
Ireland	United States	IAPH	WSC
European Commission		Integer	IACCSEA

Disclaimer – The views set out in this document reflect the interpretation of the author – and do not necessarily concur with the interpretation of the IMO or other stakeholders



Technology Options



LNG

Fuel Combustion – controlled to Low NOx

SCR

NH3 neutralises NOx on Catalyst

Other

Water Based / Valve Timing / TC Control combustion process in Diesel engine - Low NOx

EGR

Lower O2 content & lower Combustion Temperatures



Technology Options



Meeting IMO III NOx limits

LNG

Fuel Combustion – controlled to Low NOx

SCR

NH3 neutralises NOx on Catalyst

Other

Water Based / Valve Timing / TC Control combustion process in Diesel engine - Low NOx

EGR

Lower O2 content & lower Combustion Temperatures



Technology Options - SCR



State of Technology Readiness
SCR

Issue / Concern

Operating Conditions
e.g. Temperature
Catalyst Fouling – ABS
Low Load Performance

SCR System - design Catalyst Lifetime Ammonia Slip Small Vessels

Supply Chain Concerns
Urea

Response

Flexibility SCR reactor placement
Charge Air, Timing, Burner
Below 25% Load – SCR off

Experience->16000 hours / 2 years Mobile, Stationary, Ships – 500 Compact SCR – Design Phase

Competitive Global Supply Chain AUS 40 Standard US Supply Chain - by 2014

Technology Options - EGR



State of Technology Readiness FGR

Issue / Concern

Technology Readiness
Combined with other technology?
Not available for most engines

H2SO4 / PM Reagent / wash water Response

Capability Demonstrated
High NOx reduction – IMO III
Development Focus Engine OEMs

Low operating costs Mg(OH)2

Scrubber
Developing Experience



Technology Options - LNG



State of Technology Readiness LNG

Issue / Concern

Low emissions – dependent on Engine size / duty cycle / pilot fuel

Energy Density

Response

Experience
100's Gas engines – low emissions
20 Vessels
Meets IMO III
Lower Fuel Costs



Technology Options - Other



State of Technology Readiness – Other VVT, 2Stage TC... Water Based...

Issue / Concern

Not Tier III Compliant 30% - 50% - 65% DWI – HAM – FE

Miller Timing
Decreased Power

Response

Can be used in combination

Loss over come with 2-stage TC



Technology Options - summary



LNG

Fuel Combustion – controlled to Low NOx

Practical

SCR

NH3 neutralises NOx on Catalyst

Panacea

Other

Water Based / Valve Timing / TC Control combustion process in Diesel engine - Low NOx

Partial

EGR

Lower O2 content & lower Combustion Temperatures

Potential



Conclusion / Insight



Technology to meet IMO III limits is available There are a number of options / combinations

Greater collaboration between Engine OEMs and other technology providers will deliver efficient, economical, environmental solutions, for cleaner shipping

IACCSEA

Greater collaboration between technology providers and regulators will maximise the gain to society at an "efficient" cost

IACCSEA



SCR installation – Alice Austen



Engines: 2 x CAT 3516 A **Temperature:** 752°F **NOx Reduction:** < 3 g/kWh (~ 70%) **SCR** installed: 2004 Staten Island Ferry (US)

SCR installation – MS Timbus



SINOx® Installed: 1999 MaK 8M32 (Main)/ MAN 6L16/24 (Aux.) Type **Power** 3,840kW / 540 kW (Aux.) 21,000 / 3,000 Nm³/h **Exhaust Gas Flow** HFO / MDO Fuel 320 / 336° C **Temperature Urea Consumption:** 97 / 8 l/h (@40%) SODRA Catalyst Type SW 30 Honeycomb Catalyst Volume 3 m³/engine (Main) 0.4 m³/engine (Aux.) 2g/kWh **Exhaust NOx:**

SCR installation – Kleven



Project: Supply Vessel/Work ship Kleven

Exhaust gas flow: 8.790 m³/h

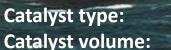
Engine type: 2 x MAN 6L 32/40, 2 x MAN 8L 21/31

Fuel: MGO

Temperature:

335° C

SINOx® Installed: 2007



SW 40 3.8 m³

NOx Reduction: 86%









SCR installation – LNG Carriers



Project: 2 x LNG Carrier, Exmar Excellence/Excelerate

SINOx[®] Installed: 2007

Exhaust Gas Flow: 2 x 70.100 Nm³/h

Application: 2 x 70t/h Regas Boiler

Fuel: HFO/MDO

Temperature: 380°C





Catalyst Type: SW 30 Honeycomb

Catalyst Volume: 10,62 m³

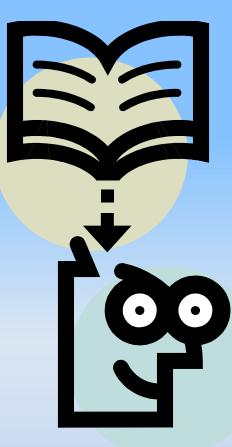
Exhaust NOx: 30 mg/Nm³

Reduction Rate: 93%



De-NOx - Selective Catalytic Reduction

- 1. Combustion → pollution inc. the acidic pollutants NOx &SOx
- 2. NOx is dangerous, & increasingly its emission is regulated.
- 3. NOx can be controlled in the engine or neutralised in the tailpipe via catalytic after treatment such as SCR
- 4. SCR is a proven technology (power-plants ,HDD and auto)
- 5. The SCR process produces Nitrogen as its end product
- 6. Marine SCR >500 Case studies yachts to container ships
- 7 SCR needs a reducing agent Urea / Ammonia
- 8 The catalyst is robust but requires the correct conditions for optimum operation
- 9. Sulphur is not a poison to Marine SCR Catalysts but its effects need to be considered e.g. limiting temperature.
- 10. After-treatment can allow an increase in efficiency (fuel
- 11. SCR on its own can meet IMO III or as a top up technology





Technology for IMO III Mexico Sept 26th Sept

For Further information please contact

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