











Triad Conference – June 10, 2008

Flux-Based Remedial Design and Assessment Tools

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The Site Managers Dilemma



"Is there some kind of quantitative model to guide these decisions?"

One approach: use complex 3-D numerical CLEMSON models to represent the source and plume







Observation

- If we had large amounts of field data, lots of time, and lots of money, we would probably select the full rigorous 3-D numerical modeling approach
- Many sites do not fit this description these sites could benefit from a more practical and simpler modeling approach
- Such a "screening-level" model should still conserve mass in the source and plume zones, and it should still represent the dominant processes



A much simpler model



SERDP/EPA/Clemson Field Test of DNAPL Removal by Alcohol Flooding, Dover Air Force Base, Delaware

EPA released 92 kg of pure PCE into the test cell at a depth of 35' below the ground surface. A total of 73.5 kg was removed during a 40 day alcohol flood



80% source removal resulted in 81% reduction in groundwater concentration





Source mass reduction leads to discharge reduction



integrated

Power function model [Rao et al., 2001; Parker and Park, 2004; Zhu and Sykes, 2004]







Source conceptual model: Mass is mainly removed by flushing. <u>Remediation is simulated by removing a</u> <u>fraction of the source mass at the time of remediation</u>





Source Zone Solutions

Falta et al., 2005

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General Solution before remediation occurs

$$M(t) = \left\{ -\frac{V_d A C_0}{\lambda_s M_0^{\Gamma}} + \left(M_0^{1-\Gamma} + \frac{V_d A C_0}{\lambda_s M_0^{\Gamma}} \right) e^{(\Gamma-1)\lambda_s t} \right\}^{\overline{1-\Gamma}}$$

If we remove a fraction, **X**, of the DNAPL mass by remediation at time *TR*, then

$$M(t) = \left\{ \frac{-V_d A C_{TR} (1-X)^{\Gamma}}{\lambda_s \left[(1-X) M_{TR} \right]^{\Gamma}} + \left(\left[(1-X) M_{TR} \right]^{1-\Gamma} + \frac{V_d A C_{TR} (1-X)^{\Gamma}}{\lambda_s \left[(1-X) M_{TR} \right]^{\Gamma}} \right) \exp\left[(\Gamma-1) \lambda_s t \right] \right\}^{\frac{1}{1-\Gamma}}$$

and the source discharge is computed from

$$C_{s}(t) = C_{TR} \left(\frac{M(t)}{M_{TR}}\right)^{\Gamma}$$



Source Behavior: Γ =0.5, M₀= 1620 kg, V=20 m/yr, A=10m x 3m, C₀=100 mg/l





Source Behavior: Γ =2.0, M₀= 1620 kg, V=20 m/yr, A=10m x 3m, C₀=100 mg/l





How to estimate Γ from field data using concentration versus time curves



time (linear scale)



Couple the source function to the plume in an analytical model:

Use the source function as the boundary condition in a 3-D advection dispersion differential equation:

$$R\frac{\partial C_i}{\partial t} = -v\frac{\partial C_i}{\partial x} + \alpha_x v\frac{\partial^2 C_i}{\partial x^2} + \alpha_y v\frac{\partial^2 C_i}{\partial y^2} + \alpha_z v\frac{\partial^2 C_i}{\partial z^2} + rxn_i$$

Use a flux-based, mixed boundary condition at x=0:

mass flux of =
$$V_d C_s(t) = \left[V_d C - \phi \alpha_x V \frac{\partial C}{\partial X} \right]_{x=0}$$

Where

$$C_{s}(t) = \frac{(C_{TR}(1-X)^{\Gamma})}{\left[(1-X)M_{TR}\right]^{\Gamma}} \left\{ \frac{-V_{d}AC_{TR}(1-X)^{\Gamma}}{\lambda_{s}\left[(1-X)M_{TR}\right]^{\Gamma}} + \left(\left[(1-X)M_{TR}\right]^{1-\Gamma} + \frac{V_{d}AC_{TR}(1-X)^{\Gamma}}{\lambda_{s}\left[(1-X)M_{TR}\right]^{\Gamma}}\right) \exp\left[(\Gamma-1)\lambda_{s}t\right] \right\}^{\frac{1}{1-\Gamma}}$$



Consider coupled parent-daughter reactions in the plume

For example, we could include reductive dechlorination of PCE to TCE to DCE to vinyl chloride:

 $rxn_{PCE} = -\lambda_{PCE}C_{PCE}$ $rxn_{TCE} = y_{TCE/PCE}\lambda_{PCE}C_{PCE} - \lambda_{TCE}C_{TCE}$ $rxn_{DCE} = y_{DCE/TCE}\lambda_{TCE}C_{TCE} - \lambda_{DCE}C_{DCE}$ $rxn_{VC} = y_{VC/DCE}\lambda_{DCE}C_{DCE} - \lambda_{VC}C_{VC}$

We would like for all of these decay rate constants to be functions of distance and time.

This lets us simulate enhanced plume remediation downgradient from the source



Plume Remediation Model – divide space and time into "reaction zones", solve the coupled parent-daughter reactions for chlorinated solvent degradation in each zone





Solution: method of characteristics with reactions. The residence time in each "reaction zone" is easily calculated. These are treated as batch reactions in each zone.





Scale-dependent longitudinal dispersion is included by assuming that a bundle of streamtubes pass through the source zone





This source/plume remediation model is called REMChlor, and it is available for free from the US EPA: http://www.epa.gov/ada/csmos/models/remchlor.html





REMChlor example: 300 kg release of 1,1,1-TCA in 1975

- DNAPL source has Γ=2.0, C₀=2 mg/l; water flow through source zone is 600 m³ per year
- The TCA is assumed to undergo reductive dechlorination in the plume to 1,1-DCA with a first order rate of 0.8/yr (very low).
- 1,1-DCA degrades to chloroethane with a first order rate of 0.2/yr (very low)







REMChlor simulation of plume remediation





REMChlor simulation of source remediation



More Complex Example Model Application

- Difficult case where natural attenuation will not work
- Long-lived PCE source, high discharge to groundwater
- Low rates of PCE-TCE-DCE-VC decay
- Plume is defined by 1 ppb



Hypothetical 1620 kg Release of PCE in 1975

- DNAPL source has Γ=1.0, C₀=100 mg/l; water flow through source zone is 300 m³ per year
- ► Assume reductive dechlorination from PCE→TCE →DCE →VC
- Assume that only ½ of DCE is converted to vinyl chloride (VC) by reductive dechlorination, the other ½ is destroyed
- Ground water pore velocity is 30 m/yr, R=2, decay rates are low: PCE, 0.4/yr; TCE, 0.15/yr; DCE, 0.1/yr; VC, 0.2/yr



Initial mass discharge to plume is 30 kg/year

Plumes are contoured down to 1 ug/l









Cancer Risk From Drinking Water at a Given Location Over Time (REMChlor also includes the inhalation risk)

Compute chronic daily intake (CDI) of each carcinogen: $CDI_{i} = \frac{q_{w}}{mT_{life}} \int_{\max(0,t-T_{ex})}^{t} C_{w}^{i}(t) dt$

Where q_w is the daily water intake (2 l/d), m is the body mass (70 kg), T_{life} is the 70 year lifetime averaging period, t is the Time, T_{ex} is the length of the exposure period (30 years), and C_w is the concentration of the carcinogen in the well. The CDI is essentially the cumulative dose of carcinogen. With a cancer risk slope factor, SF, the cancer risk is then:

$$Risk_i = CDI_i \times SF_i$$
 $Risk_T = \sum Risk_i$



Lifetime cancer risks in 2075 (exposure from 2045-2075)



Try 2 Different Remediation Schemes, Focusing on Managing the Vinyl Chloride Plume

- 1) Try DNAPL source remediation alone: remove 90% of PCE DNAPL in 2005
- Also include plume remediation: set up an enhanced reductive dechlorination zone from 0 to 400 meters, and an enhance aerobic degradation zone from 400 to 700 meters, in years 2005 to 2025

Source Remediation: Remove 90% of the remaining PCE DNAPL in 2005



Only the vinyl chloride plume is shown



Add Plume Remediation

- A) Set up an enhanced reductive dechlorination zone 0-400 meters from 2005 to 2025
- Increase PCE decay rate from 0.4 to 1.4/yr, TCE from 0.15 to 1.5/yr, and DCE from 0.1 to 0.2/yr. No change in VC decay
- B) Set up an enhanced aerobic degradation zone from 400-700 meters, from 2005 to 2025
- Increase DCE decay rate from 0.1 to 3.5/yr, and VC decay rate from 0.2 to 3.6/yr. PCE and TCE decay rates remain at background levels



Plume Remediation









Compare Remediation Effects on Vinyl Chloride Plume





Compare Remediation Effects on Vinyl Chloride Plume





Lifetime Cancer Risks in 2075 (exposure from 2045-2075)





Observations on PCE Example

- This case was very difficult because of a) the persistent DNAPL source, b) the generation of hazardous daughter products in the plume, and c) the high source concentrations compared to MCLs
- Source remediation alone may not be capable of reducing plume extent, although it greatly reduces plume mass
- A combination of source and plume remediation appears to be capable of reducing the plume extent and longevity



Alternative Source Models

Numerical Source Remediation Models

- Advanced 3-D multiphase flow models such as UTCHEM, T2VOC, STOMP, NUFT
- Models include advanced process simulation capability (surfactants, thermal processes, gravity effects)
- Can handle complex geological heterogeneity
- Can include the DNAPL "architecture", but how well is this really known?



Lagrangian Models of Source Zone

(Enfield et al., 2005; Wood et al., 2005; Jawitz et al., 2005; Basu et al., 2007)

- Based on the concept of streamtubes that pass through the source zone
- Streamtube velocities (travel times) are characterized by a log-normal distribution
- Where NAPL is present, it is distributed in the streamtubes, and can be correlated to travel time
- Mass discharge from individual streamtubes are added to get overall discharge
- NAPL removal from each streamtube depends on water velocity, and initial NAPL mass in streamtube

Comments on Lagrangian Models

- Ideally suited for flushing processes with a flow field that does not change with time.
- Much more practical to parameterize than full 3-D numerical models
- They do not consider buoyancy effects or diffusion into low permeability zones
- They do not model thermal conduction or multiple domain heat and mass transfer processes

Other Useful Tools for Flux-Based Remedial Design

- Mass Flux Toolkit (Farhat, et al., 2006) <u>http://www.gsi-</u> <u>net.com/Software/massfluxtoolkit.asp</u>)
- SourceDK (Farhat, et al., 2004) <u>http://www.gsi-net.com/Software/SourceDK.asp</u>
- Natural Attenuation Software (NAS), (Chapelle et al., 2003)

http://www.nas.cee.vt.edu/index.php