US ERA ARCHIVE DOCUMENT

# Table A-1 Plantwide GHG Emission Summary Formosa Plastic Corporation, Texas Olefins Expansion May 2014

		GHG Mass			
		Emissions [1]	CO <sub>2</sub> e [1]		
Name	EPN(s)	ton/yr	ton/yr		
Cracking Furnace Nos. 1 through 14	OL3-FUR1 through OL3- FUR14	1,462,735	1,464,333		
Steam Boiler Nos. 1 through 4	OL3-BOIL1 through OL3-BOIL4	818,869	819,763		
PDH Reactor Nos. 1 through 4	PDH-REAC1 through PDH-REAC4	236,501	236,898		
Olefins 3 Fugitives [4]	OL3-FUG	4.83	114.8		
PDH Fugitives [4]	PDH-FUG	1.17	23.17		
Elevated Flare [2]	OL3-FLRA, OL3-FLRB	84,037	85,450		
Low Pressure Flare 1 [2]	OL3-LPFLR1	9,184	9,857		
Low Pressure Flare 2 [2]	OL3-LPFLR2	9,184	9,857		
Decoking Drum 1 [3]	OL3-DK1	329	329		
Decoking Drum 2 [3]	OL3-DK2	329	329		
MAPD Regenerator Vent [4]	OL3-MAPD	32.8	32.8		
PDH Unit MSS Vessel Opening [4]	PDH-MSSVO	3.12	9.21		
Olefins 3 Plant MSS Vessel Opening [4]	OL3-MSSVO	2.22	54.7		
Olefins 3 Emergency Engine	OL3-GEN	447	449		
PDH Emergency Engine	PDH-GEN	447	449		

total = 2,621,778 2,627,618

# Note:

- [1] Combustion unit emissions (furnace, boiler, reactors) include emissions from both fuel gas and natural gas combustion. CO2e emissions in units of short (English) tons per year.
- [2] Flare emissions include emissions from flare pilot and waste gas combustion.
- MSS emissions associated with flares streams are also included in the elevated flare value.
- [3] Emissions from furnace decoking may occur from either decoking drum 1 or 2.
- [4] FPC TX Requests that No Emission Limit be established for this source.
- Compliance will be assured with the design/work practice standard as specified in the permit.

#### Table A-2

# GHG Emission Calculations - Natural Gas Combustion Formosa Plastic Corporation, Texas Olefins Expansion May 2014

tribution i rom	Natural Gas Fireu C		Emissions	per Unit				
Average Heat Input/Unit	Estimated Hours firing Natural Gas with Remainder Fuel Gas <sup>1</sup>	Annual Avg Heat Input, Each Unit	Pollutant	Emission Factor	GHG Mass Emissions <sup>3</sup>	Global Warming Potential <sup>4</sup>	CO₂e	CO₂e
(MMBtu/hr)	(hrs/yr)	(MMBtu/yr)		(kg/MMBtu) <sup>2</sup>	(metric ton/yr)		(metric ton/yr)	(tpy)
			CO <sub>2</sub>	53.02	29,161	1	29,161	32,150
220	2,500	550,000	CH <sub>4</sub>	1.0E-03	0.55	25	13.75	15.16
			N <sub>2</sub> O	1.0E-04	0.06	298	16.39	18.07
				Totals	29,162		29,191	32,183
			CO <sub>2</sub>	53.02	19,246	1	19,246	21,219
191	1,900	363,000	CH₄	1.0E-03	0.36	25	9.08	10.01
			N <sub>2</sub> O	1.0E-04	0.04	298	10.82	11.93
				Totals	19,247		19,266	21,241
431	2,500	1,078,000	CO <sub>2</sub>	53.02	57,156	1	57,156	63,014
			CH <sub>4</sub>	1.0E-03	1.08	25	26.95	29.71
			N <sub>2</sub> O	1.0E-04	0.11	298	32.12	35.42
1				Totals	57,157		57,215	63,079
			00	50.00	212	4	040	
0.50	8,760	4,000					<b>-</b>	234
						_	+	0.11
			N <sub>2</sub> O			298		0.13
				lotais	212.1		212	234
			CO	53.02	212	1	212	234
						-		
0.40	8,760	4,000	CH <sub>4</sub>	1.0E-03	4.00E-03	25	0.10	0.11
			N <sub>2</sub> O	1.0E-04	4.00E-04	298	0.12	0.13
		·	Totals	212.1		212	234	
	Average Heat Input/Unit (MMBtu/hr)  220  191  431	Average Heat Input/Unit (MMBtu/hr)  220  2,500  191  1,900  431  2,500  8,760	Average Heat Input/Unit (MMBtu/hr) firing Natural Gas with Remainder Fuel Gas¹ (hrs/yr) (MMBtu/yr)  220 2,500 550,000  191 1,900 363,000  431 2,500 1,078,000	CO2	Pollutant	Restimated Hours firing Natural Gaswith Remainder Fuel Gas¹ (hrs/yr)   Fuel Gas² (hrs/yr)	Average Heat Input/Unit (MMBtu/In)   Estimated Hours fitring Natural Gas with Remainder Fuel Gas¹ (hrs/yr)   Each Unit (MMBtu/In)   Each Unit (MBtu/In)   Each Unit (NBtu/In)	Estimated Hours firing Natural Gas with Remainder Fuel Gas¹ (hrs/yr)   Fuel Gas¹ (hrs/yr)   Each Unit (MMBtu/hr)   Each Unit (MBtu/hr)   Each Unit (MMBtu/hr)   Each Unit (MMBtu/hr)   Each Unit (MBtu/hr)   Each Unit (MMBtu/hr)   Each Unit (MMBtu/hr)   Each Unit (MBtu/hr)   Each Unit (MBtu/hr)

## Notes:

- 1. These units have the capability of firing natural gas for up to 8760 hours/yr. For purposes of calculating GHG emissions, the hours of natual gas firing (shown here) with remainder fuel gas firing are used. The hours of natural gas firing are not intended to be permit limitations; FPC TX will comply with the GHG emission limits set forth in the permit.
- 2. CO2 GHG factor from Table C-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting (GHG MRR).

CH4 and N2O GHG factors based on Table C-2 of GHG MRR.

3. CO<sub>2</sub> emissions based on 40 CFR Part 98, Subpart C, Equation C-1.

 $\mathrm{CH}_4$  and  $\mathrm{N}_2\,\mathrm{O}$  emissions based on 40 CFR Part 98, Subpart C, Equation C-8.

4. Global Warming Potential factors based on Table A-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting.

## Sample Calculation: Pvrolvsis Furnaces - CO 2:

GHG Mass Emissions (metric ton/yr) = 0.001 x 550000 (MMBtu/yr) x 53.02 kg/MMBtu = 29161 CO2e (metric ton/yr) = 29161 (metric ton/yr) x 1 = 29161

#### Table A-3

# GHG Emission Calculations - Fuel Gas Combustion Formosa Plastic Corporation, Texas Olefins Expansion May 2014

#### Fuel Gas Data:

	V	alue			
Variable	Olefins 3 Fuel Gas	PDH Unit Fuel Gas	Units	Reference	
HHV	522	391	Btu/scf	design specification	
Carbon Content (Annual Avg)	0.70	0.363	kg C/kg	design specification	
Molecular Weight (Annual Avg)	8.23	6.49	kg/kg-mol	design specification	

G Emissions Contribution From Fuel Gas Fired Combustion:								Emissions per Unit					
Source Type	Fuel Gas Type	Average Heat Input/Unit (MMBtu/hr)	Annual Average Fuel Gas Usage/Unit <sup>1</sup> (MMscf/hr)	Number of Units	Estimated Hours firing Fuel Gas with Remainder Natural Gas <sup>2</sup> (hrs/yr)	Annual Average Fuel Use, Each Unit (scf/yr)	Annual Average Heat Input, Each Unit (MMBtu/yr)	Pollutant	Emission Factor	GHG Mass Emissions <sup>4</sup> (metric ton/yr)	Global Warming Potential <sup>5</sup>	CO₂e (metric ton/yr)	CO₂e (tpy)
								CO <sub>2</sub>		65,604	1	65,604	72,329
Pyrolysis Furnace	Olefins 3	elefins 3 220	0.421	14	6,260	2.64E+09	1.38E+06	CH₄	1.0E-03	1.38	25	34.43	37.96
					•	N <sub>2</sub> O	1.0E-04	0.14	298	41.04	45.25		
									Totals	65,606		65,680	72,412
								CO <sub>2</sub>		128,525	1	128,525	141,699
Steam Boilers	Steam Boilers Olefins 3 431 0	0.826	0.826 4	6,260	5.17E+09	2.70E+06	CH₄	1.0E-03	2.70	25	67.45	74.37	
								N <sub>2</sub> O	1.0E-04	0.27	298	80.40	88.64
									Totals	128,528		128,673	141,862
							CO <sub>2</sub>		34,075	1	34,075	37,568	
PDH Unit reactors	PDH	191	91 0.488 4	4	6,860	3.35E+09	1.31E+06	CH₄	1.0E-03	1.31	25	33	36
								N <sub>2</sub> O	1.0E-04	0.13	298	39	43
									Totals	34,077		34,147	37,647
al, All Fuel Gas Comb	ustion		_	_				_	_	228,210		228,500	251,921

#### Notes.

- 1. Fuel use calculated as: MMscf/hr = Firing rate (MMBtu/hr) / HHV (Btu/scf)
- 2. These units have the capability of firing fuel gas for up to 8760 hours/yr. For purposes of calculating GHG emissions, the hours of fuel gas firing (shown here) with remainder natural gas firing are used.

The hours of fuel gas firing are not intended to be permit limitations; FPC TX will comply with the GHG emission limits set forth in the permit.

- 3. CH<sub>4</sub> and N<sub>2</sub> O GHG factors based on Table C-2 of 40 CFR 98 Mandatory Greenhouse Gas Reporting.
- CH<sub>4</sub> and N<sub>2</sub> O emissions based on 40 CFR Part 98, Subpart C, Equation C-8.
- 4. CO<sub>2</sub> emissions based on 40 CFR Part 98, Subpart C, Equation C-5.
- 5. Global Warming Potential factors based on Table A-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting.

### Sample Calculation: PDH Reactors - CO 2:

GHG Mass Emissions (metric ton/yr) =  $(44/12) \times 3.35E+09$  (scf/yr)  $\times 0.363$  kg C/kg  $\times 6.49$  kg/kg-mol / 849.5 scf/kg-mole @ std cond.  $\times 0.001 = 3.41E+04$  CO2e (metric ton/yr) = 3.41E+04 (metric ton/yr)  $\times 1 = 3.41E+04$